

1

Business

- This is class 17 of 36 before the case study!
- Next exam given out on Monday, Oct. 17
 - Due Friday, Oct 21

2

Review – Non-ideal Gases

- **Equations of State**

- ✓ Van der Waals
- ✓ SRK
- ✓ Use P_c , T_c , and ω which are species-specific

- **Corresponding States (Compressibility Factor)**

- ✓ Use P_r and T_r to get z
- ✓ $PV = znRT$ or $P\dot{V} = znRT$
- ✓ Kay's rule for mixtures
 - $P'_c = \sum y_i P_{c,i}$ and $T'_c = \sum y_i T_{c,i}$

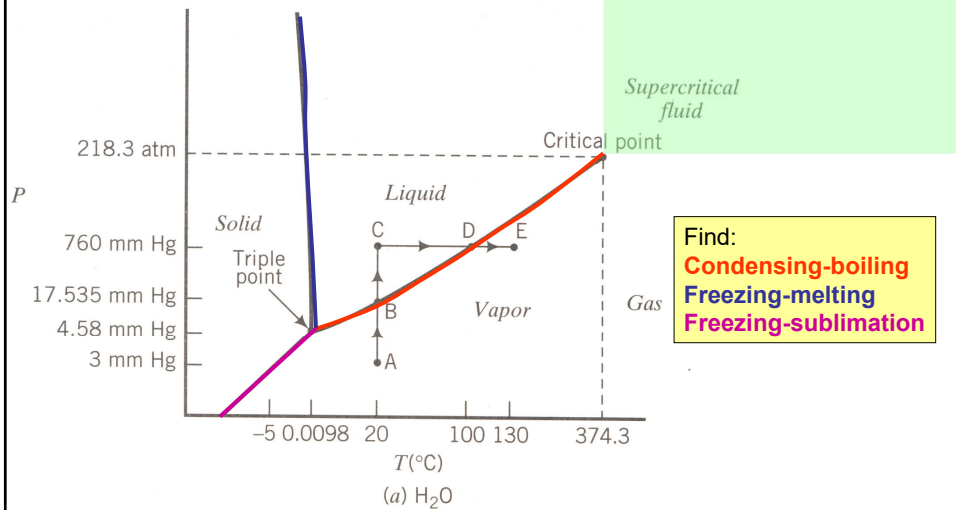
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Multiphase Systems Ch. 6



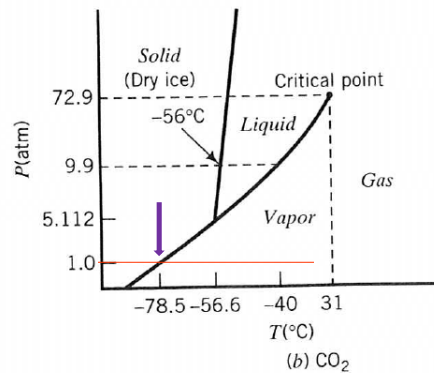
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P vs T Diagram: Water (pure component)



5

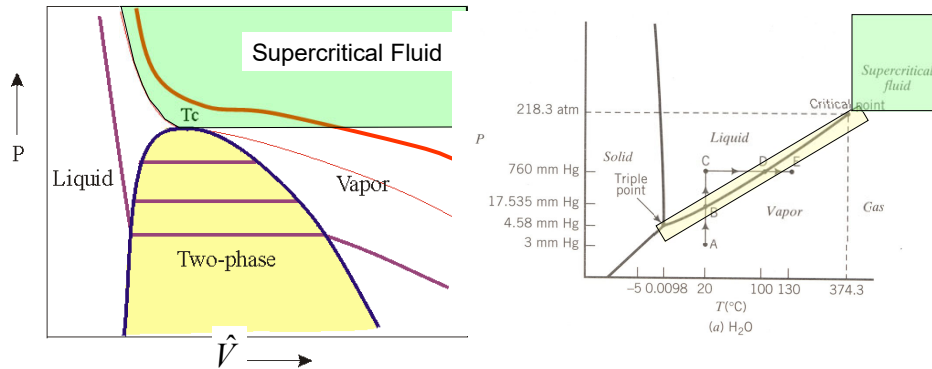
P vs T Diagram: CO₂



At atmospheric pressure, CO₂ sublimates at -78°C (Table B.1)
 At 9.9 atm, melting at -56°C, vaporization at about -40°C

6

P vs V and P vs T Phase Diagrams for H₂O



Note big changes in density ($1/\hat{V}$) in 2-phase region

7

Two Phases: Vapor & Liquid

- All charts above were for a PURE component
 - Pure H₂O or pure CO₂
- Wanted:
 - If at phase boundary, how much vapor and how much liquid at equilibrium?
 - If not at phase boundary (pure component), we only have vapor or liquid, not both!
- Also, what if we have more than one component?
 - What is the equilibrium composition of the liquid and the vapor?

8

Definitions

- Boiling point
 - Temperature at which pure liquid changes to vapor
 - Is a function of P
- Normal boiling point
 - Boiling point at 1 atm
- Freezing point
 - Temperature at which liquid changes to solid
 - Is a function of P
- Sublimation point (you get the idea!)

9

Vapor Pressure

note that these examples have more than one species (air + liquid)

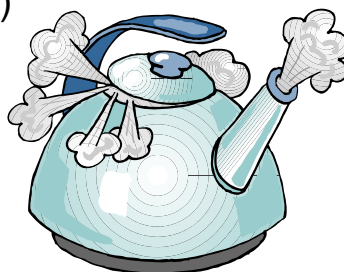
- Why does a wet sidewalk become dry on a cold day if water boils at 212°F?
- Why does a 2-liter bottle of Sprite stay fizzy until you open it for the first time?
- Why is humid air so uncomfortable in the summer?
- Why do swamp coolers work in the desert but not in the swamp?
- Why does a wet finger dry faster when I blow on it?
- What happens to the steam plume from a power plant?
- How do raindrops evaporate before hitting the ground sometimes?



10

So What Is Vapor Pressure?

- P_i^*
- Measure of the volatility of a species
- **For pure component:**
 - The pressure of the vapor above a pure liquid at equilibrium (2-phase line)
- Redefine boiling point
 - T when $P_i^* = P_{\text{tot}}$
(pure substance)



11

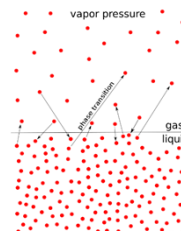
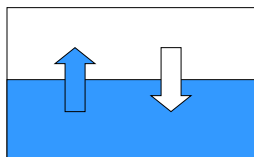
Class Answers

- | | |
|---|---|
| <ul style="list-style-type: none">• Name some compounds with high vapor pressures (i.e., evaporate quickly) | <ul style="list-style-type: none">• Name some compounds with low vapor pressures (i.e., evaporate slowly) |
|---|---|

12

Molecular Level

- As $T \uparrow$, molecules are more excited
- Some molecules exit the liquid phase
- Some molecules condense
- Equilibrium is steady-state condition when the same # of molecules condense and vaporize
- So.... P_i^* is related to the number of moles that evaporate at a given temperature



13

Properties of Vapor Pressure

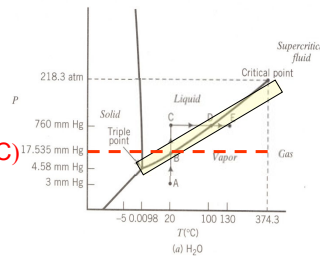
- P_i^* is a function of T
 - If you raise the T , more of the substance wants to be vapor
 - Related to volatility, or tendency to evaporate at a given T
- P_i^* is different for each species
 - Related to MW_i
 - Related to chemical structure (aromatic, paraffinic, etc.)

14

For A Pure Component

- If $P_{\text{tot}} < P^*$ (point A)
 - All vapor (i.e., gas)
- If $P_{\text{tot}} > P^*$ (point C) $P^*(20^\circ\text{C})$
 - All liquid
- If $P_{\text{tot}} = P^*$ (point B)
 - 2-phase (vapor and liquid)

(more complicated with multiple species)



15

Example: Non-ideal gas n-butane at 12 atm and 300 K

- Valerie and I got $P_r = .32$ and $T_r = .71$, then a $z = .76$
 - This was from the dotted region on the compressibility chart
- The SRK equation would not converge using the \hat{V} from the ideal gas equation!
- $P^*_{\text{n-butane}} = 2.5463 \text{ atm}$
- Since $P > P^*$, this was a liquid!!!

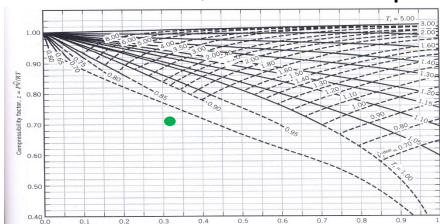
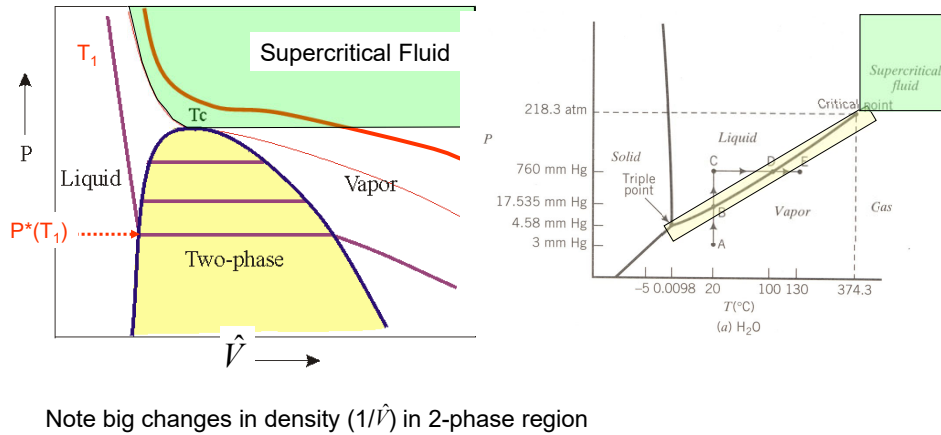


Figure 5.4-2 Generalized compressibility chart, low pressures. (From D. M. Himmelblau, *Basic Principles and Calculations in Chemical Engineering*, 3rd Edition, copyright © 1974, p.175. Reprinted by permission of Prentice Hall, Inc., Englewood Cliffs, NJ.)



16

P vs V and P vs T Phase Diagrams for H₂O



17

P* is a function of T

Consider a pure water system (i.e., no air present)

- What is $P^*_{\text{H}_2\text{O}}$ at 100°C and $P_{\text{tot}} = 1 \text{ atm}$?

$P^*_{\text{H}_2\text{O}} = 1 \text{ atm}$, and since $P_{\text{tot}} = P^*_{\text{H}_2\text{O}}$, 2-phase

- What is $P^*_{\text{H}_2\text{O}}$ at 100°C and $P_{\text{tot}} = 10 \text{ atm}$?

$P^*_{\text{H}_2\text{O}} = 1 \text{ atm}$, and since $P_{\text{tot}} > P^*_{\text{H}_2\text{O}}$, 1-phase, liquid

- What is $P^*_{\text{H}_2\text{O}}$ at 100°C and $P_{\text{tot}} = 0.01 \text{ atm}$?

$P^*_{\text{H}_2\text{O}} = 1 \text{ atm}$, and since $P_{\text{tot}} < P^*_{\text{H}_2\text{O}}$, 1-phase, gas

Vapor pressure depends on T, not P_{tot} !

18

Relationship to ΔH_{vap}

- From thermodynamics:

$$\frac{dP^*}{dT} = \frac{\Delta H_{\text{vap}}}{T(\hat{V}_{\text{gas}} - \hat{V}_{\text{liq}})}$$

- Assuming \hat{V}_{liq} is negligible and that ΔH_{vap} is constant with T, and ideal gas,

$$\ln P^* = \frac{-\Delta H_{\text{vap}}}{RT} + B$$

- This is the Clausius-Clapeyron equation

19

So how do you know
what P_i^* is at a given T?



20

Vapor Pressure Chart

(which compounds have highest vapor pressure?)

- [Figure 6.1-4](#)

21

Vapor Pressures of Water

- [Table B.3](#) in Textbook
 - P^*_{ice} from $T = -14.0$ to 0.0°C
 - P^*_{water} from $T = 0.0^\circ\text{C}$ to 101.9°C

22

Antoine Equation

- [Table B.4](#)

Table B.4 Antoine Equation Constants^a

$$\log_{10} p^* = A - \frac{B}{T + C} \quad p^* \text{ in mm Hg, } T \text{ in } ^\circ\text{C}$$

Example: The vapor pressure of acetaldehyde at 25°C is determined as follows:

$$\begin{aligned} \log_{10} p_{\text{C}_2\text{H}_4\text{O}}^*(25^\circ\text{C}) &= 8.00552 - \frac{1600.017}{25 + 291.809} = 2.9551 \\ \Rightarrow p_{\text{C}_2\text{H}_4\text{O}}^*(25^\circ\text{C}) &= 10^{2.9551} = 902 \text{ mm Hg} \end{aligned}$$

23

DIPPR Database

$$\ln P^* = A + \frac{B}{T} + C \ln T + DT^E$$

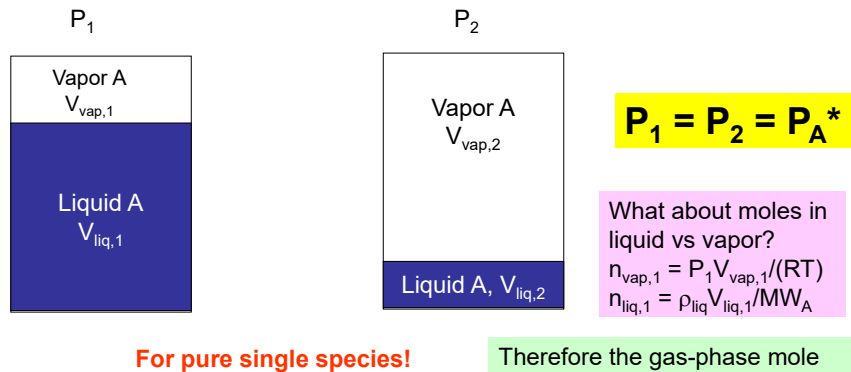
Access the DIPPR database by:

1. Being on a campus server or college/university VPN
2. Navigating to <https://dippr.aiche.org/> or dippr.byu.edu
3. Clicking the button “Log in to DIPPR® Website”

24

P_i^* is **NOT** dependent on volume!

Example: pure component A, both at same T

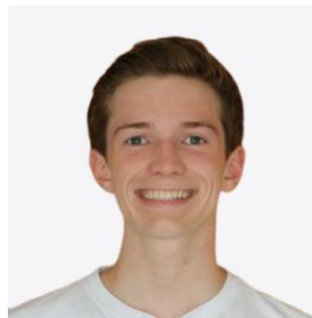


For pure single species!

Therefore the gas-phase mole fraction in each vessel is the same, but the number of moles is proportional to volume

25

What about mixtures?



26

Liquid Mixtures: Raoult's Law (simplified)

- Multiple species in liquid and gas phases

Memorize!

$$P_i = y_i P_{\text{tot}} = x_i P_i^*$$

- x_i is mole fraction in liquid phase
- P_i is the partial pressure ($= y_i P_{\text{tot}}$)
- y_i is mole fraction in gas phase

Special cases:

- 1 species with both liquid and vapor present

$$P_{\text{tot}} = P_i^*$$

- Because $x_i = 1$ and $y_i = 1$ ($i = 1$ in both phases)

- 1 species in liquid, 2 or more species in gas phase

$$y_i P_{\text{tot}} = P_i = P_i^*$$

- Because $x_i = 1$ but not y_i ($i = 1$ in liq and 2+ in gas)

- 2 or more species in liquid... coming up later



Yikes! Another definition for x_i

27

Gibb's Phase Rule

$$DF = 2 + c - \Pi$$

- DF - Degrees of freedom for phase rule
- c – # of components (i.e., species)
- Π - # of phases (“Pi” starts with a “p”)
- Single species, 2 phases
 - $DF = 2 + 1 - 2 = 1$ (need to specify T or P)
- 2 species, 2 phases
 - $DF = 2 + 2 - 2 = 2$ (need to specify both T and P)

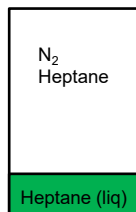
This is different than the degrees of freedom in material balances

28

Example

1 liquid species, 2 gas species

Goal: Find the equilibrium mole fraction of *n*-heptane in the gas phase



Gibbs Phase Rule

DF = 2 + 2 species – 2 phases = 2
(must specify T & P)

P_{tot} = 1 atm

T = 25°C

Find: y_{heptane} in gas phase

Procedure:

Find P*_{heptane} at 25°C

$y_{\text{heptane}} P_{\text{tot}} = x_{\text{heptane}} P^*_{\text{heptane}}$
but $x_{\text{heptane}} = 1.0$, so

$y_{\text{heptane}} = P^*_{\text{heptane}} / P_{\text{tot}}$

Look up Antoine eq constants

$$P^* = 10^{\left(A - \frac{B}{T+C}\right)} = 10^{\left(6.87689 - \frac{1238.122}{25+216.823}\right)}$$

P* = 45.68 mm Hg

$$y_{\text{heptane}} = P^*_{\text{heptane}} / P_{\text{tot}} = 45.68 \text{ mm Hg} / 760 \text{ mm Hg} = 0.0601$$

29

Homework

- **16.1** – T, P*, and V given
 - P_{tot} (easy!)
 - Wanted m_{tot}
 - calculate m_{liq} from density and volume
 - calculate m_{vapor} from ideal gas law & MW
- **16.2** – from manometer, get P* vs T
 - Check with Clausius Clapeyron eqn.
- **16.3** – (a) Gibbs phase rule; (b) find P*
 - Please use both Antoine and DIPPR to find P*
 - $y_i = P_i^* / P_{\text{tot}}$
- **16.4** – Explain vapor pressure to a non-engineer

30