

Reflection



After Action Report

What did I learn from this HW assignment?



1



Class 27



Enthalpies,
Heat Capacities
Heats of Formation,
Oh My!



2

Review of Energy Balances

$$\Delta \dot{H} + \Delta \dot{E}_K + \Delta \dot{E}_P = \dot{Q} + \dot{W}_s$$

- Enthalpies needed to calculate heat or work terms
- Methods to calculate enthalpy (so far):
 - Steam tables
 - Graph (P-H diagram)
 - Interpolation from 2 given values
- Needed: Method to get enthalpies for any species as a function of T & P

3

We Can't Measure Enthalpy!

Things we can measure:

- T, y_i , P, Q, W_s
- Last HW assignment had you fit H vs T
$$\hat{H} = mT + b$$
- Today we will find a way to get $\hat{H}$ for any species at any temperature.
- Idea: Measure Q, find $\Delta \hat{H}$

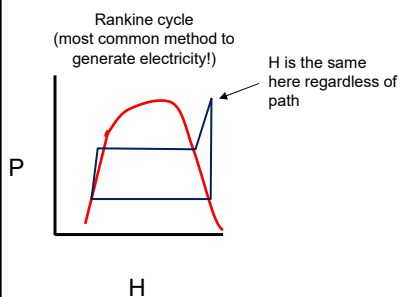
4

Concepts

1. Enthalpy is a state function
2. Heat Capacities
3. Latent Heats (phase change)
4. Heat of Formation
5. Calculating ΔH as $f(T,P)$

5

Concept 1. Enthalpy Is A State Function



- Enthalpy is independent of path
- Always talk about ΔH from some reference condition
 - Steam tables:
 $\hat{H} = 0$ at triple point
 - Other tables are different
(e.g., in Table B.1, $\Delta \hat{H}_f^o$ for $H_2 = 0$ at 25°C)
 - Don't mix and match tables!!!

6

Concept 2. Heat Capacities

- $\hat{H} = f(T, P)$ $d\hat{H} = \left(\frac{\partial \hat{H}}{\partial T}\right)_P dT + \left(\frac{\partial \hat{H}}{\partial P}\right)_T dP$ Generally small
- $\hat{U} = f(T, \hat{V})$ $d\hat{U} = \left(\frac{\partial \hat{U}}{\partial T}\right)_V dT + \left(\frac{\partial \hat{U}}{\partial \hat{V}}\right)_T d\hat{V}$
- Now define heat capacities:

$$C_P = \left(\frac{\partial \hat{H}}{\partial T}\right)_P, \quad C_V = \left(\frac{\partial \hat{U}}{\partial T}\right)_V$$
- For **ideal gases**:

$$d\hat{H} \equiv C_P dT, \quad d\hat{U} \equiv C_V dT$$
- For **solids and liquids**:

$$d\hat{H} = C_P dT + \hat{V} dP$$
- For **non-ideal gases**:

$$d\hat{H} = C_P dT + \left[\hat{V} - T \left(\frac{d\hat{V}}{dT} \right)_P \right] dP$$
 Not small

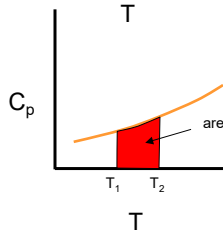
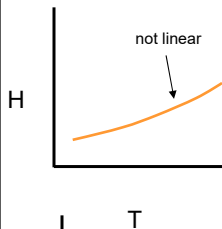
7

Concept 2. Heat Capacities (cont.)

- $C_P = \left(\frac{\partial \hat{H}}{\partial T}\right)_P$ (like slope of H vs T curve, prob 7.55)
- $\Delta \hat{H} = \int_{T_1}^{T_2} C_P dT$
- $C_P = a + bT + cT^2 + dT^3 + \dots$
- so

$$\Delta \hat{H}_{T_1 \rightarrow T_2} = \int_{T_1}^{T_2} (a + bT + cT^2 + dT^3) dT$$

$$= a(T_2 - T_1) + \frac{b}{2}(T_2^2 - T_1^2) + \frac{c}{3}(T_2^3 - T_1^3) + \frac{d}{4}(T_2^4 - T_1^4)$$
- For ideal gases: $C_P = C_V + R$
- For solids and liquids, $C_P \cong C_V$

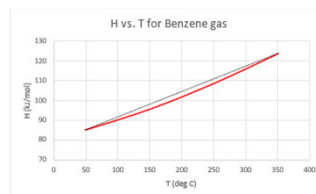


8

A Practical View

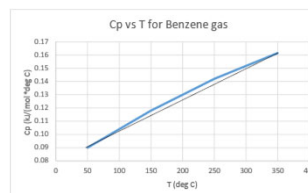
- Wouldn't it be nice to have a polynomial equation for H !

- $H = a + bT + cT^2$



- This would not work for different reference enthalpies!

- Solution: Polynomial for C_p
 - $C_p = a + bT + cT^2 + dT^3$ ($= dH/dT$)
 - Fit to thermodynamic data



- $\Delta \hat{H}_{T_1 \rightarrow T_2} = \int_{T_1}^{T_2} (a + bT + cT^2 + dT^3) dT$

9

Form 1: $C_p[\text{kJ}/(\text{mol}\cdot^\circ\text{C})]$ or $[\text{kJ}/(\text{mol}\cdot\text{K})] = a + bT + cT^2 + dT^3$ Form 2: $C_p[\text{kJ}/(\text{mol}\cdot^\circ\text{C})]$ or $[\text{kJ}/(\text{mol}\cdot\text{K})] = a + bT + cT^{-2}$										
Example: $(C_p)_{\text{acetone(g)}} = 0.07196 + (20.10 \times 10^{-5})T - (12.78 \times 10^{-8})T^2 + (34.76 \times 10^{-12})T^3$, where T is in $^\circ\text{C}$.										
Note: The formulas for gases are strictly applicable at pressures low enough for the ideal gas equation of state to apply.										
Compound	Formula	Mol. Wt.	State	Form	Temp. Unit	$a \times 10^3$	$b \times 10^5$	$c \times 10^8$	$d \times 10^{12}$	Range (Units of T)
Acetone	CH_3COCH_3	58.08	l	1	$^\circ\text{C}$	123.0	18.6			–30–60
			g	1	$^\circ\text{C}$	71.96	20.10	–12.78	34.76	0–1200
Acetylene	C_2H_2	26.04	g	1	$^\circ\text{C}$	42.43	6.053	–5.033	18.20	0–1200
Air		29.0	g	1	$^\circ\text{C}$	28.94	0.4147	0.3191	–1.965	0–1500
			g	1	K	28.09	0.1965	0.4799	–1.965	273–1800
Ammonia	NH_3	17.03	g	1	$^\circ\text{C}$	35.15	2.954	0.4421	–6.686	0–1200
Ammonium sulfate	$(\text{NH}_4)_2\text{SO}_4$	132.15	c	1	K	215.9				275–328
Benzene	C_6H_6	78.11	l	1	$^\circ\text{C}$	126.5	23.4			6–67
			g	1	$^\circ\text{C}$	74.06	32.95	–25.20	77.57	0–1200
Isobutane	C_4H_{10}	58.12	g	1	$^\circ\text{C}$	89.46	30.13	–18.91	49.87	0–1200
n-Butane	C_4H_{10}	58.12	g	1	$^\circ\text{C}$	92.30	27.88	–15.47	34.98	0–1200
Isobutene	C_4H_8	56.10	g	1	$^\circ\text{C}$	82.88	25.64	–17.27	50.50	0–1200
Calcium carbide	CaC_2	64.10	c	2	K	68.62	1.19	-8.66×10^{10}	—	298–720
Calcium carbonate	CaCO_3	100.09	c	2	K	82.34	4.975	-12.87×10^{10}	—	273–1033
Calcium hydroxide	$\text{Ca}(\text{OH})_2$	74.10	c	1	K	89.5				276–373
Calcium oxide	CaO	56.08	c	2	K	41.84	2.03	-4.52×10^{10}		273–1173
Carbon	C	12.01	c	2	K	11.18	1.095	-4.891×10^{10}		273–1373
Carbon dioxide	CO_2	44.01	g	1	$^\circ\text{C}$	36.11	4.233	–2.887	7.464	0–1500
Carbon monoxide	CO	28.01	g	1	$^\circ\text{C}$	28.95	0.4110	0.3548	–2.220	0–1500
Carbon tetrachloride	CCl_4	153.84	l	1	K	93.39	12.98			273–343
Chlorine	Cl_2	70.91	g	1	$^\circ\text{C}$	33.60	1.367	–1.607	6.473	0–1200
Copper	Cu	63.54	c	1	K	22.76	0.6117			273–1357

^aAdapted in part from D. M. Himmelblau, *Basic Principles and Calculations in Chemical Engineering*, 3rd Edition, © 1974, Table E.1. Adapted by permission of Prentice-Hall, Inc., Englewood Cliffs, NJ.

^aAdapted in part from D. M. Himmelblau, *Basic Principles and Calculations in Chemical Engineering*, 3rd Edition, © 1974, Table E.1. Adapted by permission of Prentice-Hall, Inc., Englewood Cliffs, NJ.

10

Caution!



- When getting a heat capacity coefficient from Table B.2, use the multiplier at the top of the column
- Example: Acetone
 - $a = 123$
 - multiplier = 10^3
(i.e., the actual number was multiplied by 10^3 to make it look nicer in the table)
 - Therefore, **$a = 123 \times 10^{-3} \text{ kJ/(gmol}\cdot\text{K)}$**

11

DIPPR Format

$$C_p = A + B \left[\frac{C/T}{\sinh(C/T)} \right]^2 + D \left[\frac{E/T}{\cosh(E/T)} \right]^2$$

Integrated form:

$$\int_{T_1}^{T_2} C_p dT = A[T_2 - T_1] + BC \left[\coth\left(\frac{C}{T_2}\right) - \coth\left(\frac{C}{T_1}\right) \right] - DE \left[\tanh\left(\frac{E}{T_2}\right) - \tanh\left(\frac{E}{T_1}\right) \right]$$

12

Heat Capacity Example

Student volunteer needed!

13

Heat Capacity Example

Example: Enthalpy Change Using Heat Capacity						
CO2 is heated from 20C to 600 C			T1=	20 C		
CO + 1/2 O2 ==> CO2			T2=	600 C		
Heat capacity polynomial						
	a	b	c	d	T	form
CO2	3.61E-02	4.23E-05	-2.89E-08	7.46E-12	C	1
$\Delta \hat{H} = \int_{T_1}^{T_2} C_p dT = a(T_2 - T_1) + \frac{b}{2}(T_2^2 - T_1^2) + \frac{c}{3}(T_2^3 - T_1^3) + \frac{d}{4}(T_2^4 - T_1^4)$						
Basis: 1 gmol of CO						
Integrate heat capacities for products						
CO2	2.67E+01 kJ/mol					
Delta H = 2.67E+01 kJ/mol						

14

I put an excel sheet with the heat capacity coefficients on the class web page

Heat Capacity Table (collected from different problems and examples)										
Cp coefficients										
		a	b	c	d	T	Form	DelH_f	DelH_vap	T_boil (C)
acetone (gas)	CH ₃ COCH ₃	7.20E-02	2.01E-04	-1.28E-07	3.48E-11	C	1.00E+00	-216.7		
acetone (liquid)	CH ₃ COCH ₃	1.23E-01	1.86E-04			C	1	-248.2	3.02E+01	5.60E+01
acetylene	C ₂ H ₂	4.24E-02	6.05E-05	-5.03E-08	1.82E-11	C	1	226.75		
Air	Air	2.89E-02	4.15E-06	3.19E-09	-1.97E-12	C	1.00E+00			
ammonia	NH ₃ (g)	3.52E-02	2.95E-05	4.42E-09	-6.69E-12	C	1	-46.19		
benzene	C ₆ H ₆ (g)	7.41E-02	3.30E-04	-2.52E-07	7.76E-11	C	1	8.29E+01	3.08E+01	8.01E+01
benzene	C ₆ H ₆ (l)	1.27E-01	2.34E-04					48.66		
calcium carbonate	CaCO ₃ (s)	8.23E-02	4.98E-05	-1.29E+03		K	2	-1.21E+03		
calcium oxide	CaO(s)	4.18E-02	2.03E-05	-4.52E+02		K	2			
carbon	C(s)	1.12E-02	1.10E-05	-4.89E+02		K	2	0		
carbon dioxide	CO ₂	3.61E-02	4.23E-05	-2.89E-08	7.46E-12	C	1	-393.5		
carbon monoxide	CO	2.90E-02	4.11E-06	3.55E-09	-2.22E-12	C	1	-110.52		
chlorine	Cl ₂	3.36E-02	1.37E-05	-1.61E-08	6.47E-12	C	1	0	20.4	-34.06
ethane	C ₂ H ₆	4.94E-02	1.39E-04	-5.82E-08	7.28E-12	C	1	-84.67		
ethylene	C ₂ H ₄	4.08E-02	1.15E-04	-6.89E-08	1.77E-11	C	1	52.28		
hydrogen	H ₂	2.88E-02	7.65E-08	3.29E-09	-8.70E-13	C	1	0		
methane	CH ₄	3.43E-02	5.47E-05	3.66E-09	-1.10E-11	C	1	-74.85		
methanol (gas)	CH ₃ OH (g)	4.29E-02	8.30E-05	-1.87E-08	-8.03E-12	C	1	-201.2	35.27	
methanol (liquid)	CH ₃ OH (liq)	7.59E-02	1.68E-04			C	1	-238.6		64.7
nitric oxide	NO	2.95E-02	8.19E-06	-2.93E-09	3.65E-13	C	1	90.37		
nitrogen	N ₂	2.90E-02	2.20E-06	5.72E-09	-2.87E-12	C	1	0		
n-pentane (gas)	C ₅ H ₁₂ (g)	1.15E-01	3.41E-04	-1.90E-07	4.23E-11	C	1	-146.4		
n-pentane (liq)	C ₅ H ₁₂ (liq)	1.55E-01	4.37E-04			C	1	-173		
oxygen	O ₂	2.91E-02	1.16E-05	-6.08E-09	1.31E-12	C	1	0		
propane	C ₃ H ₈ (g)	6.80E-02	2.26E-04	-1.31E-07	3.17E-11	C	1	-103.8		
sulfur dioxide	SO ₂	3.89E-02	3.90E-05	-3.10E-08	8.61E-12	C	1	-296.6		
toluene (gas)	C ₇ H ₈ (g)	9.42E-02	3.80E-04	-2.79E-07	8.03E-11	C	1	50		
toluene (liquid)	C ₇ H ₈ (l)	1.49E-01	3.24E-04			C	1	12		
water	H ₂ O(l)	7.54E-02				C	1	-285.84		
water (steam)	H ₂ O(g)	3.35E-02	6.88E-06	7.60E-09	-3.59E-12	C	1	-241.83		

15

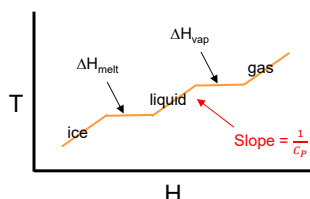
Concepts

1. Enthalpy is a state function
2. Heat Capacities
3. Latent Heats (phase change)
4. Heat of Formation
5. Calculating ΔH as $f(T,P)$

16

Concept 3.

Phase Changes (pure substances)



$$\Delta \hat{H}_{melt} = \hat{H}_{liq} - \hat{H}_{solid} \quad (\text{tabulated})$$

$$\Delta \hat{H}_{vap} = \hat{H}_{gas} - \hat{H}_{liq} \quad (\text{tabulated})$$

$$\Delta \hat{H}_{freezing} = -\Delta \hat{H}_{melt}$$

$$\Delta \hat{H}_{condens} = -\Delta \hat{H}_{vap}$$

Also we could find $\Delta \hat{H}_{sub}$

Remember that for a pure substance, T is constant during a phase change

- The heat of phase change is called **latent heat**, which comes from the fact that the temperature does not change during phase change
- The heat required to merely change the temperature of a substance is called the **sensible heat**

17

Table B.1 Selected Physical Property Data^a

Compound	Formula	Mol. Wt.	SG (20°/4°)	$T_m(^{\circ}\text{C})^b$	$\Delta \hat{H}_m(T_m)^c$ kJ/mol	$T_b(^{\circ}\text{C})^c$	$\Delta \hat{H}_v(T_b)^c$ kJ/mol	$T_c(\text{K})^f$	$P_c(\text{atm})^g$	$(\Delta \hat{H}_c)^{e,h,i}$ kJ/mol	$(\Delta \hat{H}_c)^{e,j}$ kJ/mol
Acetaldehyde	CH ₃ CHO	44.05	0.783 ¹⁸	-123.7	—	20.2	25.1	461.0	—	-166.2(g)	-1192.4(g)
Acetic acid	CH ₃ COOH	60.05	1.049	16.6	12.09	118.2	24.39	594.8	57.1	-486.18(l)	-871.69(l)
Acetone	C ₃ H ₆ O	58.08	0.791	-95.0	5.69	56.0	30.2	508.0	47.0	-438.15(g)	-919.73(g)
Acetylene	C ₂ H ₂	26.04	—	—	—	-81.5	17.6	309.5	61.6	-248.2(l)	-1785.7(l)
Ammonia	NH ₃	17.03	—	-77.8	5.653	-33.43	23.351	405.5	111.3	-216.7(g)	-1821.4(g)
Ammonium hydroxide	NH ₄ OH	35.03	—	—	—	—	—	—	—	+226.75(g)	-1299.6(g)
Ammonium nitrate	NH ₄ NO ₃	80.05	1.725 ²⁵	169.6	5.4	—	—	Decomposes at 210°C	—	-67.20(l)	-382.58(g)
Ammonium sulfate	(NH ₄) ₂ SO ₄	132.14	1.769	513	—	—	—	Decomposes at 513°C after melting	—	-46.19(g)	—
Aniline	C ₆ H ₅ N	93.12	1.022	-6.3	—	184.2	—	699	52.4	-366.48(aq)	—
Benzaldehyde	C ₆ H ₅ CHO	106.12	1.046	-26.0	—	179.0	38.40	—	—	-365.14(c)	—
Benzene	C ₆ H ₆	78.11	0.879	5.53	9.837	80.10	30.765	562.6	48.6	-399.36(aq)	—
Benzoic acid	C ₇ H ₆ O ₂	122.12	1.266 ¹⁵	122.2	—	249.8	—	—	—	-1179.3(c)	—
Benzyl alcohol	C ₇ H ₈ O	108.13	1.045	-15.4	—	205.2	—	—	—	-1173.1(aq)	—
Bromine	Br ₂	159.83	3.119	-7.4	10.8	58.6	31.0	584	102	—	—
1,2-Butadiene	C ₄ H ₆	54.09	—	-136.5	—	10.1	—	446	—	-88.83(l)	-3520.0(l)
1,3-Butadiene	C ₄ H ₆	54.09	—	-109.1	—	-4.6	—	425	42.7	-40.04(g)	—
n-Butane	C ₄ H ₁₀	58.12	—	-138.3	4.661	-0.6	22.305	425.17	37.47	+48.66(l)	-3267.6(l)
Isobutane	C ₄ H ₁₀	58.12	—	-159.6	4.540	-11.73	21.292	408.1	36.0	+82.93(g)	-3301.5(g)
1-Butene	C ₄ H ₈	56.10	—	-185.3	3.8480	-6.25	21.916	419.6	39.7	-3226.7(g)	-3741.8(l)
Calcium carbide	CaC ₂	64.10	2.22 ¹⁸	2300	—	—	—	—	—	—	—
Calcium carbonate	CaCO ₃	100.09	2.93	—	—	—	—	Decomposes at 825°C	—	0(l)	—
Calcium chloride	CaCl ₂	110.99	2.152 ¹⁵	782	28.37	>1600	—	—	—	-147.0(l)	-2855.6(l)
										-124.7(g)	-2878.5(g)
										-158.4(l)	-2849.0(l)
										-134.5(g)	-2868.8(g)
										+1.17(g)	-2718.6(g)
										-62.76(c)	—

18

Calcium hydroxide	Ca(OH) ₂	74.10	2.24						(-H ₂ O at 580°C)	-986.59(c)	—
Calcium oxide	CaO	56.08	3.32	2570	50	2850	—	—	—	-635.6(c)	—
Calcium phosphate	Ca ₃ (PO ₄) ₂	310.19	3.14	1670	—	—	—	—	—	-4138(c)	—
Calcium silicate	CaSiO ₃	116.17	2.915	1530	48.62	—	—	—	—	-1584(c)	—
Calcium sulfate	CaSO ₄	136.15	2.96	—	—	—	—	—	—	-1432.7(c)	—
Calcium sulfate (gypsum)	CaSO ₄ ·2H ₂ O	172.18	2.32						(-1.5 H ₂ O at 128°C)	-1450.4(aq)	—
Carbon (graphite)	C	12.010	2.26	3600	46.0	4200	—	—	—	0(c)	-393.51(c)
Carbon dioxide	CO ₂	44.01	—	-56.6 at 5.2 atm	8.33	(Sublimes at -78°C)	304.2	72.9	—	-412.9(l)	—
Carbon disulfide	CS ₂	76.14	1.261 ^{22*/20*}	-112.1	4.39	46.25	26.8	552.0	78.0	-393.5(g)	—
Carbon monoxide	CO	28.01	—	-205.1	0.837	-191.5	6.042	133.0	34.5	+87.9(l)	-1075.2(l)
Carbon tetrachloride	CCl ₄	153.84	1.595	-22.9	2.51	76.7	30.0	556.4	45.0	+115.3(g)	1102.6(g)
Chlorine	Cl ₂	70.91	—	-101.00	6.406	-34.06	20.4	417.0	76.1	-110.52(g)	-282.99(g)
Chlorobenzene	C ₆ H ₅ Cl	112.56	1.107	-45	—	132.10	36.5	632.4	44.6	-139.5(l)	-352.2(l)
Chloroethane	C ₂ H ₅ Cl	See ethyl chloride								-106.7(g)	-385.0(g)

Adapted in part from D. M. Himmelblau, *Principles and Calculations in Chemical Engineering*, 3rd Edition, ©1974, Tables D.1 and F.1. Adapted by permission of Prentice-Hall, Inc., Englewood Cliffs, NJ.

*Melting point at 1 atm.
 †Heat of fusion at T_m and 1 atm.
 ‡Boiling point at 1 atm.
 §Heat of vaporization at T_b and 1 atm.
 ¶Critical temperature.
 ¶Critical pressure.
 ¶Heat of formation at 25°C and 1 atm.
 ††Heat of combustion at 25°C and 1 atm. Standard states of products are CO₂(g), H₂O(l), SO₂(g), HCl(aq), and N₂(g). To calculate ΔH_c° with H₂O(g) as a product, add 44.01 n_w to the tabulated value, where n_w = moles H₂O formed/mole fuel burned.
 †††To convert ΔH to kcal/mol, divide given value by 4.184; to convert to Btu/lb-mole, multiply by 430.28.

19

Table B.10 Atomic Heat Capacities for Kopp's Rule^a

Element	C_{pa} [J/(g-atom·°C)]	
	Solids	Liquids
C	7.5	12
H	9.6	18
B	11	20
Si	16	24
O	17	25
F	21	29
P	23	31
S	26	31
All Others	26	33

^aD. M. Himmelblau, *Basic Principles and Calculations in Chemical Engineering*, 3rd Edition, Prentice-Hall, Englewood Cliffs, NJ, 1974, p. 270.

Kopp's Rule:

$$C_p = \sum_{k=\text{element}} v_k C_{p,k}$$

where v_k = moles of element k in molecule

So for solid phenol, C₆H₅OH,

$$v_C = 6$$

$$v_H = 6$$

$$v_O = 1$$

$$C_p = 6 \cdot 7.5 + 6 \cdot 9.6 + 17 = 119.6 \text{ J/(mol·°C)}$$

(Dippr = 129 J/(mol·°C) at 25°C)

Only use this out of desperation!

20

Other Estimation Formulas

- Trouton's rule (8.4-3)

$$\Delta H_v = f(T_b)$$

- Chen's equation (8.4-4)

$$\Delta H_v = f(T_b, T_c, P_c)$$

- Clapeyron equation (8.4-7)

$$\Delta H_v = f(P^*)$$

- Watson's correlation (8.4-8)

$$\Delta H_v \text{ vs. } T \text{ using } T_c$$

Only use these equations out of desperation!

21

Simplifications

- Sometimes we get lazy and assume an average heat capacity for some temperature range

$$\hat{H}_2 - \hat{H}_1 = \bar{C}_p(T_2 - T_1)$$

- **We will use this on exams!**
 - I am not testing you on integration skills

22

Concepts

1. Enthalpy is a state function
2. Heat Capacities
3. Latent Heats (phase change)
4. Heat of Formation
5. Calculating ΔH as $f(T,P)$

23

Concept 4. Heat of Formation

- **Wanted: Common reference state for all species!**
- Can use $\Delta \hat{H}_f^o$ as a reference at 25°C, 1 atm
- Good for reaction chemistry
- $\Delta \hat{H}_f^o = 0$ for species whose natural state is 25°C, 1 atm
 - N₂, O₂, H₂, C(graphite)

$$\hat{H}_i = \Delta \hat{H}_{f,i}^o + \int_{25^\circ\text{C}}^{T_2} C_{P,i} dT$$

Tabulated in Table B.1

24

This equation is the “magic bullet”
to solve all energy balances

$$\hat{H}_i = \Delta \hat{H}_{f,i}^o + \int_{25^\circ\text{C}}^{T_2} C_{P,i} dT$$

25

Python Example (Find $\hat{H}_{NH_3}$ at 700°C)

```
[2]: # %Load http://che.byu.edu/imports.py
import numpy as np
import matplotlib.pyplot as plt
%matplotlib inline
from scipy.optimize import fsolve, curve_fit
from scipy.integrate import odeint, quad
from scipy.interpolate import interp1d
from scipy.misc import import derivative
import scipy.constants as const
import sympy as sp
sp.init_printing()
import glob
import time
#import pint; u = pint.UnitRegistry()

[3]: delHF0_NH3 = -46.19 #heat of formation of NH3 in kJ/mol
Tfinal = 700 #temperature in C
CPNH3a = np.array([3.52e-2, 2.95e-5, 4.42e-9, -6.69e-12])
# note that np.array is a function, hence the parentheses, and the argument of the function is a list, which you do by square brackets
def CPMH3(T):
    return CPMH3a[0] + CPMH3a[1]*T + CPMH3a[2]*(T**2) + CPMH3a[3]*(T**3)
def h(T):
    integral = quad(CPMH3, 25, 700)
    return integral[0]
# Use the square brackets here because the integrate function returns an array with the integrated value and the error, so the square brackets
H_NH3 = h(700) + delHF0_NH3
print("H_NH3 = ", H_NH3)

H_NH3 = -15.107955034179685
```

26

Python Example

(Find $\hat{H}_{NH_3}$ at 700°C)

```

3]: delHf0_NH3 = -46.19          #heat of formation of NH3 in kJ/mol
    Tfinal = 700                #temperature in C
    CPNH3a = np.array([3.52e-2,2.95e-5,4.42e-9,-6.69e-12])
    # note that np.array is a function, hence the parentheses, and the argument of
    def CPNH3(T) :
        return CPNH3a[0] + CPNH3a[1]*T + CPNH3a[2]*(T**2) + CPNH3a[3]*(T**3)
    def h(T) :
        integral = quad(CPNH3,25,700)
        return integral[0]
    # Use the square brackets here because the integrate function returns an array
    H_NH3 = h(700) + delHf0_NH3
    print("H_NH3 = ",H_NH3)

H_NH3 = -15.107955034179685

```

27

Compound	Formula	Mol. Wt.	SG (20°/4°)	$T_m(^{\circ}\text{C})^b$	$\Delta\hat{H}_m(T_m)^{c,j}$ kJ/mol	$T_b(^{\circ}\text{C})^d$	$\Delta\hat{H}_b(T_b)^{c,j}$ kJ/mol	$T_c(\text{K})^f$	$P_c(\text{atm})^g$	$(\Delta\hat{H}_c^{\circ})^{c,h}$ kJ/mol	$(\Delta\hat{H}_c^{\circ})^{c,i}$ kJ/mol
Acetaldehyde	CH ₃ CHO	44.05	0.783 ¹⁸	-123.7	—	20.2	25.1	461.0	—	-166.2(g)	-1192.4(g)
Acetic acid	CH ₃ COOH	60.05	1.049	16.6	12.09	118.2	24.39	594.8	57.1	-486.18(l)	-871.69(l)
										-438.15(g)	-919.73(g)
Acetone	C ₃ H ₆ O	58.08	0.791	-95.0	5.69	56.0	30.2	508.0	47.0	-248.2(l)	-1785.7(l)
										-216.7(g)	-1821.4(g)
Acetylene	C ₂ H ₂	26.04	—	—	—	-81.5	17.6	309.5	61.6	+226.75(g)	-1299.6(g)
Ammonia	NH ₃	17.03	—	-77.8	5.653	-33.43	23.351	405.5	111.3	-67.20(l)	-382.58(g)
										-46.19(g)	—
Ammonium hydroxide	NH ₄ OH	35.03	—	—	—	—	—	—	—	-366.48(aq)	—
Ammonium nitrate	NH ₄ NO ₃	80.05	1.725 ²⁵	169.6	5.4	—	Decomposes at 210°C	—	—	-365.14(c)	—
										-399.36(aq)	—
Ammonium sulfate	(NH ₄) ₂ SO ₄	132.14	1.769	513	—	—	Decomposes at 513°C after melting	—	—	-1179.3(c)	—
										-1173.1(aq)	—
Aniline	C ₆ H ₅ N	93.12	1.022	-6.3	—	184.2	—	699	52.4	—	—
Benzaldehyde	C ₆ H ₅ CHO	106.12	1.046	-26.0	—	179.0	38.40	—	—	-88.83(l)	-3520.0(l)
										-40.04(g)	—
Benzene	C ₆ H ₆	78.11	0.879	5.53	9.837	80.10	30.765	562.6	48.6	+48.66(l)	-3267.6(l)
										+82.93(g)	-3301.5(g)
Benzoic acid	C ₇ H ₆ O ₂	122.12	1.266 ¹⁵	122.2	—	249.8	—	—	—	—	-3226.7(g)
Benzyl alcohol	C ₇ H ₈ O	108.13	1.045	-15.4	—	205.2	—	—	—	—	-3741.8(l)
Bromine	Br ₂	159.83	3.119	-7.4	10.8	58.6	31.0	584	102	0(l)	—
1,2-Butadiene	C ₄ H ₆	54.09	—	-136.5	—	10.1	—	446	—	—	—
1,3-Butadiene	C ₄ H ₆	54.09	—	-109.1	—	-4.6	—	425	42.7	—	—
n-Butane	C ₄ H ₁₀	58.12	—	-138.3	4.661	-0.6	22.305	425.17	37.47	-147.0(l)	-2855.6(l)
										-124.7(g)	-2878.5(g)
Isobutane	C ₄ H ₁₀	58.12	—	-159.6	4.540	-11.73	21.292	408.1	36.0	-158.4(l)	-2849.0(l)
										-134.5(g)	-2868.8(g)
1-Butene	C ₄ H ₈	56.10	—	-185.3	3.8480	-6.25	21.916	419.6	39.7	+1.17(g)	-2718.6(g)
Calcium carbide	CaC ₂	64.10	2.22 ¹⁸	2300	—	—	—	—	—	-62.76(c)	—
Calcium carbonate	CaCO ₃	100.09	2.93	—	—	Decomposes at 825°C	—	—	—	-1206.9(c)	—
Calcium chloride	CaCl ₂	110.99	2.152 ¹⁵	782	28.37	>1600	—	—	—	-794.96(c)	—

28

Balances

$$\Delta H_{sys} = H_{out} - H_{in} = \left(\sum n_i \hat{H}_i \right)_{out} - \left(\sum n_i \hat{H}_i \right)_{in}$$

$$\hat{H}_i = \Delta \hat{H}_{f,i}^o + \int_{25^\circ\text{C}}^{T_2} C_{P,i} dT$$

$$\sum n_i \hat{H}_i = \sum n_i \Delta \hat{H}_{f,i}^o + \left(\sum n_i [a_i(T - 298)] \right) + \left(\sum n_i \left[b_i \frac{T^2 - 298^2}{2} \right] \right) + \left(\sum n_i [c_i] \frac{T^3 - 298^3}{3} \right) + \dots$$

$$\sum n_i \hat{H}_i = \sum n_i \Delta \hat{H}_{f,i}^o + \left(\sum n_i a_i \right) (T - 298) + \left(\sum n_i b_i \right) \frac{T^2 - 298^2}{2} + \left(\sum n_i c_i \right) \frac{T^3 - 298^3}{3} + \dots$$

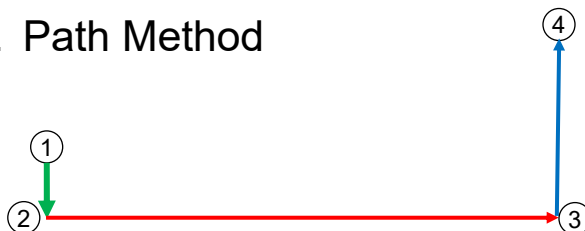
where a_i , b_i , and c_i are the heat capacity coefficients for species i

Note that for a chemical reaction, the number of moles of each species (n_i) changes

29

Two Methods to Get ΔH

1. Path Method



$$H_4 - H_1 = (H_2 - H_1) + (H_3 - H_2) + (H_4 - H_3)$$

2. ΔH_f^o method

$$\hat{H}_i = \Delta \hat{H}_{f,i}^o + \int_{25^\circ\text{C}}^{T_2} C_{P,i} dT$$

So compute H_4 and H_1 and subtract

30

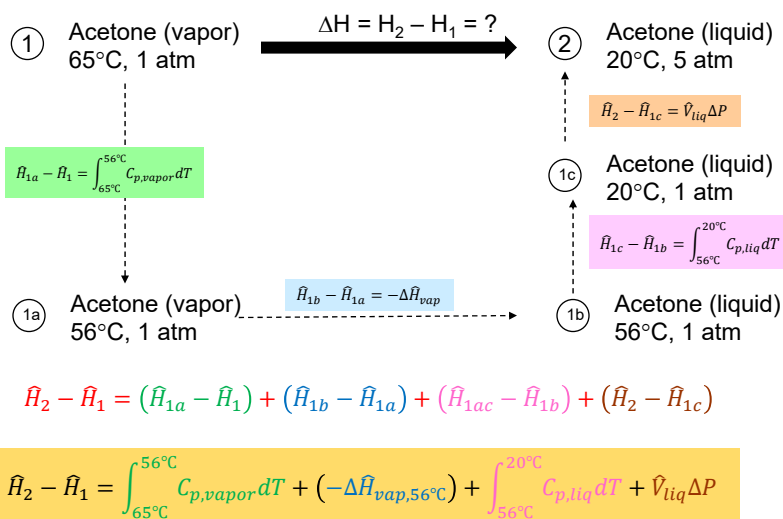
Example

Calculate the enthalpy change for acetone going from a vapor at 65°C and 1 atm to a liquid at 20 °C and 5 atm

- A. Path method using ΔH_{vap} at 1 atm and T_{boiling}
- B. Heat of formation method

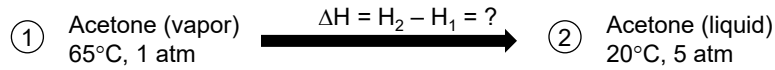
31

Example: Find ΔH for acetone vapor at 65°C forming a liquid at 20 °C and 5 atm (Path method)



32

Example: Find ΔH for acetone vapor at 65°C forming a liquid at 20 °C and 5 atm (ΔH_f° method)



$$\hat{H}_1 = \Delta H_{f,vapor}^\circ + \int_{25^\circ\text{C}}^{65^\circ\text{C}} C_{p,vapor} dT$$

$$\hat{H}_2 = \Delta H_{f,liq}^\circ + \int_{25^\circ\text{C}}^{20^\circ\text{C}} C_{p,liq} dT + \hat{V}_{liq} \Delta P$$

$$\hat{H}_2 - \hat{H}_1 = \left(\Delta H_{f,liq}^\circ + \int_{25^\circ\text{C}}^{20^\circ\text{C}} C_{p,liq} dT + \hat{V}_{liq} \Delta P \right) - \left(\Delta H_{f,vapor}^\circ + \int_{25^\circ\text{C}}^{65^\circ\text{C}} C_{p,vapor} dT \right)$$

$$\hat{H}_2 - \hat{H}_1 = \underbrace{\Delta H_{f,liq}^\circ - \Delta H_{f,vapor}^\circ}_{-\Delta H_{\text{vaporization at } 25^\circ\text{C}}} + \int_{25^\circ\text{C}}^{20^\circ\text{C}} C_{p,liq} dT + \hat{V}_{liq} \Delta P - \int_{25^\circ\text{C}}^{65^\circ\text{C}} C_{p,vapor} dT$$

33

See Excel Sheet

Path vs ΔH_f° method

34

Bottom Line

You Should Know Both Methods to Get ΔH

1. Path Method
2. ΔH_f° method



Remember that ΔH is just part of energy balance

$$\Delta \dot{H} + \Delta \dot{E}_K + \Delta \dot{E}_P = \dot{Q} + \dot{W}_s$$

35

Table B.8 Specific Enthalpies of Selected Gases: SI Units

	$\hat{H}(\text{kJ/mol})$					
	Reference state: Gas, $P_{\text{ref}} = 1 \text{ atm}$, $T_{\text{ref}} = 25^\circ\text{C}$					
	O ₂	N ₂	H ₂	CO	CO ₂	H ₂ O
0	-0.72	0.73	-0.72	-0.73	-0.80	-84.4
25	0.00	0.00	0.00	0.00	0.00	0.00
100	2.19	2.24	2.19	2.19	2.19	2.34
200	5.15	5.31	5.15	5.15	5.15	6.01
300	8.17	8.47	8.17	8.17	8.17	9.57
400	11.24	11.72	11.24	11.24	11.24	13.23
500	14.37	15.00	14.37	14.37	14.37	17.01
600	17.56	18.33	17.56	17.56	17.56	20.91
700	20.81	21.59	20.81	20.81	20.81	24.92
800	24.13	24.85	24.13	24.13	24.13	29.05
900	27.46	28.89	27.19	27.49	42.94	33.32
1000	30.86	32.47	30.56	29.04	48.60	37.69
1100	34.31	36.07	33.99	32.19	54.33	42.18
1200	37.81	39.70	37.46	35.39	60.14	46.78
1300	41.34	43.38	40.97	38.62	65.98	51.47
1400	44.89	47.07	44.51	41.90	71.89	56.25
1500	48.45	50.77	48.06	45.22	77.84	61.09

This reference does not follow Table B.1

Stronger memo to follow!

36

Table B.9 Specific Enthalpies of Selected Gases:
American Engineering Units

H (Btu/lb-mole)

Reference state: Gas, $P_{\text{ref}} = 1 \text{ atm}$, $T_{\text{ref}} = 77^\circ\text{F}$

T	Ar	O ₂	N ₂	H ₂	CO	CO ₂	H ₂ O
32		-315	-312	-310	-312	-394	-361
77		0	0	0	0	0	0
100	160		160	159	160	206	
200	858	858	858	848	858	1092	1092
300	1563	1602	1563	1539	1563	1992	1992
400	2275	2342	2275	2225	2275	2792	2792
500	2993	3094	2993	2925	2993	3592	3592
600	3719	3858	3719	3639	3719	4392	4392
700	4451						5233
800	5188						6122
900	5930						7059
1000	6677						8045
1100	7429	7826	7399	7145	7467	11263	8880
1200	8186	8645	8151	7861	8233	12533	9831
1300	8947	9471	8922	8581	9021	13820	10799
1400	9712	10304	9699	9306	9809	15122	11783
1500	10481	11142	10485	10035	10606	16436	12783
1600	11254	11988	11278	10769	11409	17773	13798
1700	12031	12836	12080	11509	12220	19119	14831
1800	12811	13691	12888	12254	13036	20469	15877
1900	13594	14551	13702	13003	13858	21840	16941
2000	14381	15415	14524	13759	14688	23211	18019

37

Taboo Equations

3rd Edition

- Page 451: 9.5-1a and 9.5-1b
- 1st Eqn. on page 457
- Page 463: last equation (under section 5)

4th Edition

- Page 506: 9.5-1a and 9.5-1b
- 1st Eqn. on page 511
- Page 519: last equation (under section 5)

38

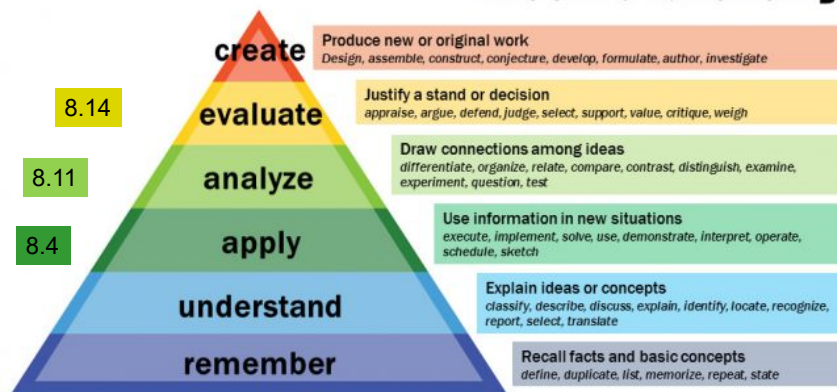
Problem Solving (pp. 361-362)

1. Solve material balances (mass or moles)
2. Write energy balance (drop appropriate terms)
3. Choose reference state(s)
4. Table of n_i & H_i in and out (or m_i , U_i , etc.)
5. Find ΔH_{sys} or ΔU_{sys}
6. Find W , W_s , ΔE_k , ΔE_p as needed
7. Solve energy balance

39

Homework Problems

Bloom's Taxonomy



Vanderbilt University Center for Teaching

<https://cft.vanderbilt.edu/guides-sub-pages/blooms-taxonomy/>

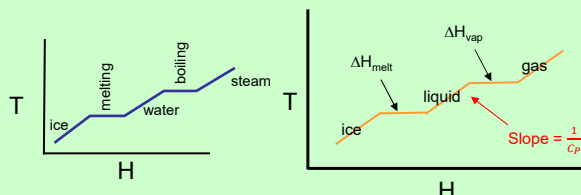
40

QUIZ

1. What is meant by the statement that “enthalpy is a state function?”
2. What is a heat capacity?
3. For water, draw a graph with temperature on the y axis and enthalpy on the x axis, starting from ice and proceeding to steam, labeling the different portions of the line.
4. How do you use the heat of formation to calculate enthalpy? (eqn. needed)

41

1. What is meant by the statement that “enthalpy is a state function?”
 - H is not dependent on T & P path
2. What is a heat capacity?
 - Change in enthalpy with temperature
3. For water, draw a graph with temperature on the y axis and enthalpy on the x axis, starting from ice and proceeding to steam, labeling the different portions of the line.



4. How do you use the heat of formation to calculate enthalpy?

$$H(\text{at } T_2) = \Delta H_f^0 + \int_{T_1=25^\circ\text{C}}^{T_2} C_p dT$$

42