

Mechanical Energy Balance

- Special Case
- No temperature change, no chemical rxn
($\Delta u \approx 0$, $\Delta H \approx 0$)
- Velocity, pressure, friction are important

$\Rightarrow$ magic (energy; momentum equations)

$$\frac{\Delta P}{\rho} + \frac{\Delta u^2}{2} + g \Delta z + \hat{F} = - \frac{W_s}{\dot{m}}$$

$\uparrow$ change in pressure $\uparrow$ velocity $\uparrow$ height $\uparrow$ friction $\uparrow$ shaft work done by system

If $\hat{F} = 0$
 $W_s = 0$

$\Rightarrow$ Bernoulli's Equ.

$$\frac{\Delta P}{\rho} + \frac{\Delta u^2}{2} + g \Delta z = 0$$

or

$$\frac{P_2 - P_1}{\rho} + \frac{u_2^2 - u_1^2}{2} + g(z_2 - z_1) = 0$$

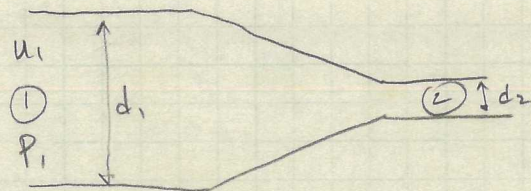
Other Relationships

$$\dot{V} = u A$$

$\frac{m^3}{s}$ $\frac{m}{s}$ m^2

$$\dot{m} = \rho u A$$

$\frac{g}{s}$ $\frac{g}{m^3}$ $\frac{m}{s}$ m^2

Examples

Find A. $P_2 - P_1$
B. u_2

Mass Balance

$$\dot{m} = \text{constant} = \rho A_1 u_1 = \rho A_2 u_2$$

$$A_1 = \pi \frac{d_1^2}{4}$$

$$A_2 = \pi \frac{d_2^2}{4}$$

$$\rho \pi \frac{d_1^2}{4} u_1 = \rho \pi \frac{d_2^2}{4} u_2$$

(if densities are equal)

$$\text{so } \boxed{u_2 = u_1 \left(\frac{d_1}{d_2} \right)^2}$$

what about pressure?

Bernoulli's Eqn.

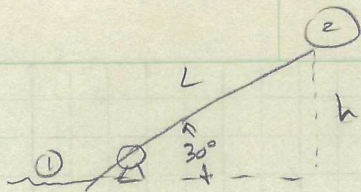
$$\frac{P_2 - P_1}{\rho} + \frac{u_2^2 - u_1^2}{2} + g(z_2 - z_1) = 0$$

$$P_2 = P_1 - \frac{\rho}{2} (u_2^2 - u_1^2)$$

$$= P_1 - \frac{\rho}{2} \left(\left[u_1 \left(\frac{d_1}{d_2} \right)^2 \right]^2 - u_1^2 \right)$$

$$\boxed{P_2 = P_1 - \frac{\rho}{2} (u_1^2) \left(\left[\frac{d_1}{d_2} \right]^4 - 1 \right)}$$

7.55



$$\sin 30^\circ = \frac{h}{L} = 0.5 \Rightarrow L = 2h$$

$$\frac{\Delta P}{\rho} + \frac{\Delta u^2}{2} + g \Delta z + \hat{F} = -\frac{W_s}{\dot{m}}$$

$$F = 0.041 L \frac{\text{ft} \cdot \text{lb}_f}{\text{lb}_m}$$

① → surface of lake $u_1 = 0$

② → atmospheric discharge $P_2 = P_1$

$$\frac{u_2^2}{2} + gh + \underbrace{(0.041)(2h)}_{\substack{\text{ft} \cdot \text{lb}_f \\ \text{lb}_m}} = -\frac{W_s}{\dot{m}}$$

$\frac{u_2^2}{2} = ?$ need u_2

$$\dot{V} = (95 \text{ gal/min}) \left(\frac{\text{ft}^3}{7.4805 \text{ gal}} \right) \left(\frac{\text{min}}{60 \text{ s}} \right) = 0.212 \frac{\text{ft}^3}{\text{s}}$$

$$uA = \dot{V}$$

$$A = \pi \frac{d^2}{4} = \left(\pi \left(\frac{1.049 \text{ in}}{4} \right)^2 \right) \left(\frac{\text{ft}}{12 \text{ in}} \right)^2 = 6 \times 10^{-3} \text{ ft}^2$$

$$u_2 = \frac{0.212 \text{ ft}^3/\text{s}}{6 \times 10^{-3} \text{ ft}^2} = 35.3 \text{ ft/s}$$

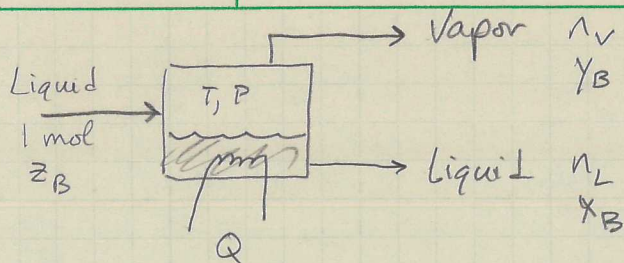
$$\dot{m} = \rho A u_2 = \left(62.4 \frac{\text{lb}_m}{\text{ft}^3} \right) \left(6 \times 10^{-3} \text{ ft}^2 \right) \left(35.3 \text{ ft/s} \right) = 13.2 \frac{\text{lb}_m}{\text{s}}$$

$$\frac{(35.3 \text{ ft/s})^2}{2} + \left(32.2 \frac{\text{ft}}{\text{s}^2} \right) h + \left(0.082 h \frac{\text{ft} \cdot \text{lb}_f}{\text{lb}_m} \right) \left(32.2 \frac{\text{ft} \cdot \text{lb}_m}{\text{lb}_f \cdot \text{s}^2} \right) = \left(\frac{-8 \text{ hp}}{13.2 \frac{\text{lb}_m}{\text{s}}} \right) \left(\frac{1.7376 \frac{\text{ft} \cdot \text{lb}_f}{\text{s}}}{1.34 \times 10^{-3} \text{ hp}} \right)$$

$$623 + 32.2 h + 2.64 h = 10,742$$

$$h = 290 \text{ ft!}$$

7.51



(a) unknowns $n_v, n_L, y_B, x_B, Q, T, P = 7$

species balances (benz, tol) $= 2$

Other Equations

(1) Raoult's Law

$$x_B P_B^* = y_B P_{tot} \quad 1$$

$$x_T P_T^* = y_T P_{tot} \quad 2$$

(2) Energy Balance $3 \Rightarrow 3$

2 DoF

But if T, P are known, DoF = 0

(b) $T = 90^\circ\text{C}, P_{tot} = 652 \text{ mm Hg}$

$$P_{tot} = P_B + P_T = x_B P_B^* + x_T P_T^*$$

$$\text{So } P_{tot} = x_B P_B^* + (1 - x_B) P_T^*$$

$$\text{rearranging, } P_{tot} = x_B (P_B^* - P_T^*) + P_T^*$$

$$\text{So } x_B = \frac{P_{tot} - P_T^*}{P_B^* - P_T^*}$$

$$\text{Then, } y_B = \frac{x_B P_B^*}{P_{tot}}$$

Total mole balance

$$1 = n_v + n_L$$

Benzene balance

$$\begin{aligned} 0.5 &= x_B n_L + y_B n_v = x_B n_L + y_B (1 - n_L) \\ &= y_B + n_L (x_B - y_B) \end{aligned}$$

$$\text{So } n_L = \frac{0.5 - y_B}{x_B - y_B}$$

Energy Balance

$$Q = \sum n_i \hat{H}_{i, \text{out}} - \sum n_i \hat{H}_{i, \text{in}}$$

See spreadsheet

7.51 (cont.)

make a linear correlation for $\hat{H}$ for each species in each phase

$$y = mx + b$$

$$m = \frac{y_2 - y_1}{x_2 - x_1}$$

then use one data point to get $b = y_1 - mx_1$

$$Q = n_1(y_B \hat{H}_{B,v} + y_T \hat{H}_{T,v}) + n_2(x_B \hat{H}_{B,L} + x_T \hat{H}_{T,L}) - n_f(z_B \hat{H}_{B,F} + z_T \hat{H}_{T,F}) \Rightarrow n_f = 1$$

(b) See spreadsheet

(c) If P is too low, all vapor

If P is too high, all liquid

(d) See spreadsheet as $P \uparrow, n_L \uparrow$, so less energy req'd to produce vapor

(e) See spreadsheet