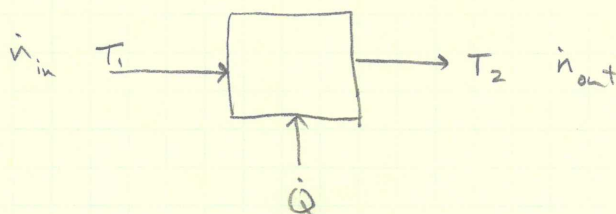
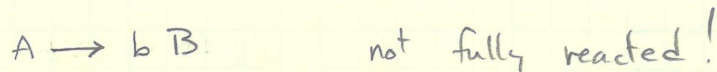


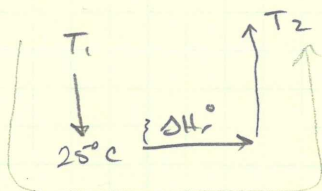
Energy Balances with Reaction

- Goals:
- ① Energy balances w/ ΔH_r° (single rxns.)
 - ② Energy balances w/ ΔH_f° (multiple rxns.)

A. Energy balances with ΔH_r° Material Balance

$$\dot{n}_A = \dot{n}_{A,0} - \dot{\xi}$$

$$\dot{n}_B = 0 + b\dot{\xi}$$

Energy Balance

follow the path!

$$\Delta \dot{H} = \dot{n}_{A,0} \int_{T_1}^{25^\circ\text{C}} C_{p,A} dT + \dot{\xi} \Delta H_r^\circ + \dot{n}_B \int_{25^\circ\text{C}}^{T_2} C_{p,B} dT + \dot{n}_A \int_{25^\circ\text{C}}^{T_2} C_{p,A} dT$$

where $\Delta H_r^\circ = \Delta H_{f,B}^\circ - \Delta H_{f,A}^\circ$
 $b\dot{\xi}$
 $\dot{n}_{A,0} - \dot{\xi}$

- This method only works well with one reactant species
- For multiple species and/or merts, use different method

Caution

Enthalpy tables are self consistent,
but often not consistent with heat of
formation tables

What?

Example: Find $\hat{H}_{H_2O,l}$ (sat'd liquid) at 25°C and 1 atm

ppt { (a) use steam Tables

$$\text{Table B.5} \Rightarrow \hat{H} = \left(104.8 \frac{\text{kJ}}{\text{kg}}\right) \left(\frac{\text{kg}}{1000 \text{ g}}\right) \left(\frac{18 \text{ g}}{\text{mol}}\right) = 188.6 \frac{\text{kJ}}{\text{gmol}}$$

(b) use ΔH_f°

$$+ \hat{V} \Delta P = \left(0.00101 \frac{\text{m}^3}{\text{kg}}\right) (1 \text{ atm} - 0.0317 \text{ bar})$$

$$= 1.78 \times 10^{-3} \text{ kJ/mol more}$$

Table B.1 $\Rightarrow \Delta H_f^\circ = -285.84 \frac{\text{kJ}}{\text{gmol}}$

$$\hat{H} = \Delta H_f^\circ + \int_{25}^{25} C_p dT = \Delta H_f^\circ$$

Why? Ref for steam tables $\Rightarrow \hat{H}_{H_2O}$ at triple pt. = 0
(0.01°C , 0.00611 bar)

Ref for ΔH_f° is $\Delta H_{f,H_2}^\circ = 0$ } at 25°C , 1 bar
 $\Delta H_{f,O_2}^\circ = 0$



By the way, Section 9.5 is off limits

Tables B.8 ; B.9 are off limits $\Rightarrow \hat{H}_{25^\circ\text{C},i}^{\text{ref}} = 0$
(unless entire problem is from Table)

$$\begin{aligned}
 \hat{V} \Delta P &= \left(.00101 \frac{\text{m}^3}{\text{kg}} \right) \left[1 \text{ atm} - .0317 \text{ bar} \left(\frac{\text{atm}}{1.01325 \text{ bar}} \right) \right] \left[\frac{1.01325 \times 10^5 \text{ N/m}^2}{\text{atm}} \right] \\
 &= \left(99.1 \frac{\text{N-m}}{\text{kg}} \right) \left(\frac{\text{kg}}{1000 \text{ g}} \right) \left(\frac{18 \text{ g}}{\text{mol}} \right) \left(\frac{\text{J}}{\text{N-m}} \right) \left(\frac{\text{kJ}}{1000 \text{ J}} \right) \\
 &= 1.78 \times 10^{-3} \frac{\text{kJ}}{\text{mol}}
 \end{aligned}$$

{ look at Table B.7, liquid at 50°C, see how $\hat{H}$ changes with pressure
 (ppx)

0.5 bar	→	209.3
1.0 bar	→	209.3
5.0 bar	→	209.7

pretty small change!

B. Energy balances with ΔH_f° & C_p 's

$$\Delta \dot{H}_{sys} + \Delta \dot{E}_p + \Delta \dot{E}_k = \dot{Q} - \dot{W}_s$$

$$\Delta \dot{H}_{sys} = (\sum \dot{n}_i \hat{H}_i)_{out} - (\sum \dot{n}_i \hat{H}_i)_{in}$$

$$\hat{H}_i = \Delta \hat{H}_{f,i}^\circ + \int_{25^\circ C}^T \hat{C}_{p,i} dT$$

Construct Table

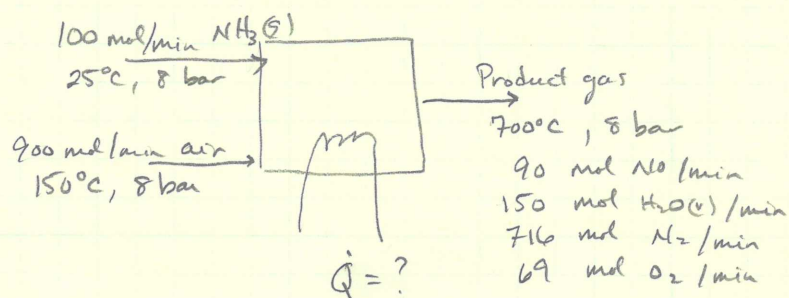
<u>IN</u>					<u>Out</u>				
species	$\dot{n}_i$	T	$\hat{H}_i$	$\underline{H}_i$	species	$\dot{n}_i$	T	$\hat{H}_i$	$\underline{H}_i$
A	✓	✓	✓	✓	A	✓	✓	✓	✓
B	✓	✓	✓	✓	B	✓	✓	✓	✓
C	✓	✓	✓	✓	C	✓	✓	✓	✓
R	0	-	-	-	R	✓	✓	✓	✓
Q	0	-	-	-	Q	✓	✓	✓	✓
S	0	-	-	-	S	✓	✓	✓	✓

Products {

- This method does not calculate ΔH_{rxn}

- Much better for multiple reactions

Example: 9.20



(a) make enthalpy chart

IN				
	$\dot{n}$	$T(^{\circ}\text{C})$	$\hat{H}$	H
NH_3	100	25	0	
O_2	189	150	0	
N_2	711	150	0	
NO	0	-	-	-
$\text{H}_2\text{O}(l)$	0	-	-	-

OUT				
	$\dot{n}$	$T(^{\circ}\text{C})$	$\hat{H}$	H
	0	-	-	-
	69	700	0	
	716	700	0	
	90	700	0	

$$\hat{H} = \Delta H_{f,i}^{\circ} + \int_{25}^{700} C_{p,i} dT$$

$$\dot{Q} = (\sum \dot{n}_i \hat{H}_i)_{\text{out}} - (\sum \dot{n}_i \hat{H}_i)_{\text{in}}$$

see spreadsheet