

Outline

Date		Class #		Comb. Lecture	Problem Due
Nov	11	19 ✓	Concepts, Candle, Fireplace, Premixed, Diffusion	1	
			Heats of Formation, Heats of Reaction, Heat Capacities,		
	13	20 ✓	Enthalpies	2	#1
	18	21 ✓	Stoichiometry, Equilibrium Constants	3	#2,#3
			Adiabatic Flame Temperature, Multi-Component		
	20	22 ✓	Equilibrium, NASA-Lewis Code	4	#4
	27		BYU Friday, NO Class		
	29		Thanksgiving		
Dec	2	25 ✓	Heterogeneous Combustion	5	#5
	4	26 ✓	NO _x Mechanisms, Soot	6	#6
	9	27 ✓	Flame Speeds, Turbulence, Explosions	7	#7
	11	28 ✓	Flameless Combustion	8	#8

Only one more lecture class after today!

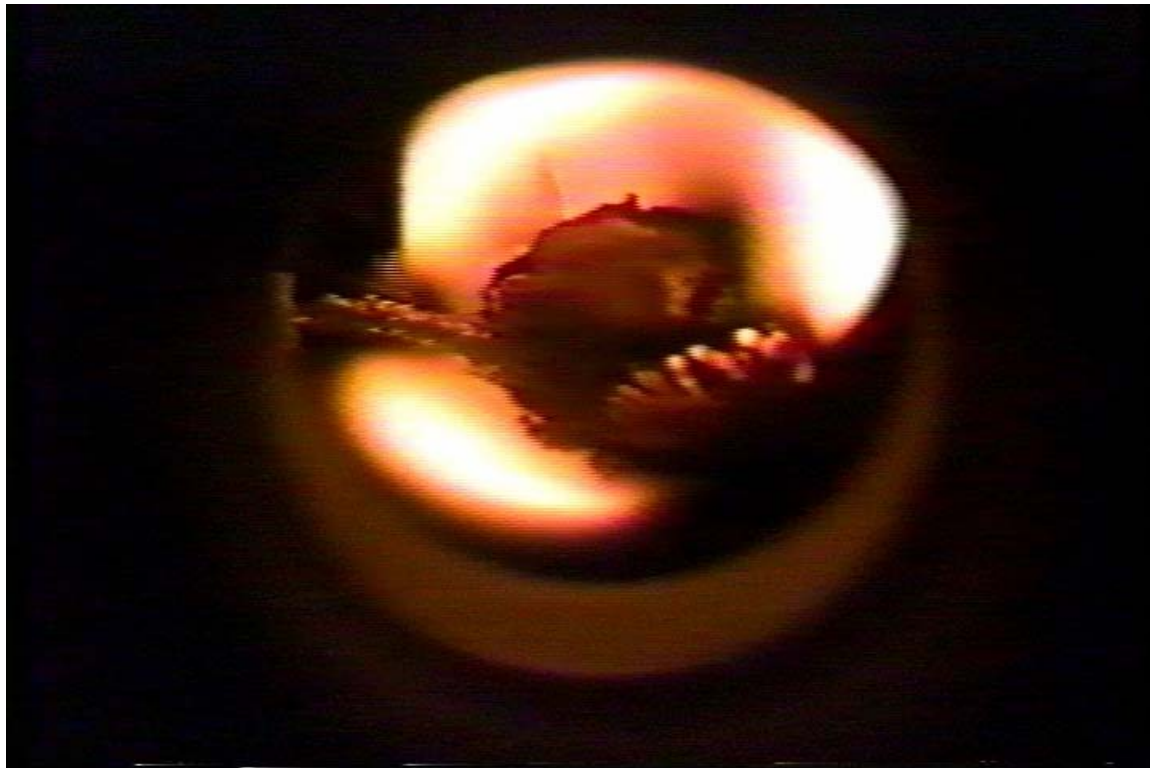
Combustion Kinetics

Combustion Class 6

- Heterogeneous kinetics
 - Chemical reaction rate
 - Mass transfer rate
- Homogeneous kinetics
 - Importance of radicals
 - Examples
 - NO_x

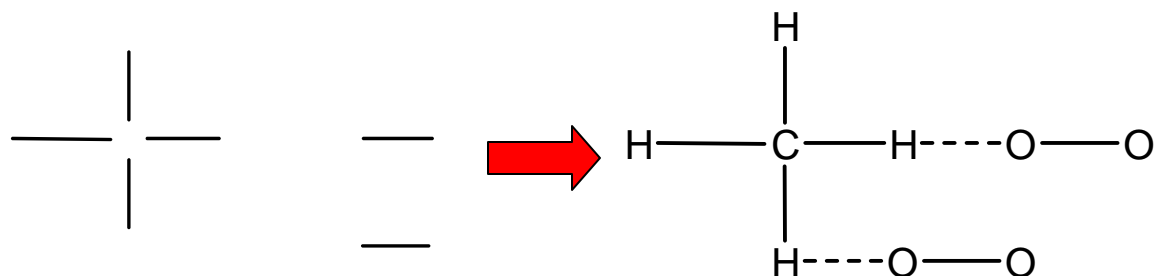
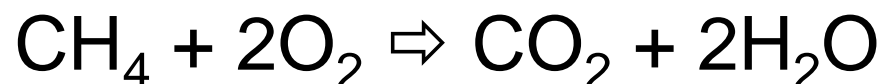
Heterogeneous Kinetics

Board Discussion



Elementary Step Reactions

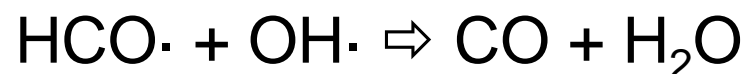
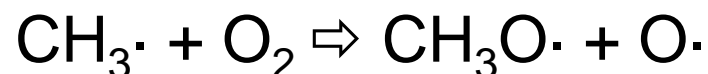
- How does the chemistry really happen?



??? Very unlikely!



More Realistic Chemistry



etc.....



Bottom Line:

- These are elementary steps
 - Chemistry happens!
- Lots of radical chemistry in flames
- High temperatures necessary to maintain radical pool
- This is why flames go out when cooled!

TABLE 2. The Westbrook and Dryer Comprehensive Mechanism for Methanol Oxidation

Reaction	Rate ^a			
	log A	n	E _a	Reference ^b
2.1 CH ₃ OH + M → CH ₃ + OH + M	18.5	0	80.0	This study
2.2 CH ₃ OH + O ₂ → CH ₂ OH + HO ₂	13.6	0	50.9	Aronowitz et al. (1978)
2.3 CH ₃ OH + OH → CH ₂ OH + H ₂ O	12.6	0	2.0	This study
2.4 CH ₃ OH + O → CH ₂ OH + OH	12.2	0	2.3	LeFevre et al. (1972)
2.5 CH ₃ OH + H → CH ₂ OH + H ₂	13.5	0	7.0	This study
2.6 CH ₃ OH + H → CH ₃ + H ₂ O	12.7	0	5.3	This study
2.7 CH ₃ OH + CH ₃ → CH ₂ OH + CH ₄	11.3	0	9.8	Gray and Herod (1968)
2.8 CH ₃ OH + HO ₂ → CH ₂ OH + H ₂ O ₂	12.8	0	19.4	Aronowitz et al. (1978)
2.9 CH ₂ OH + M → CH ₂ O + H + M	13.4	0	29.0	This study
2.10 CH ₂ OH + O ₂ → CH ₂ O + HO ₂	12.0	0	6.0	Aronowitz et al. (1978)
2.11 CH ₄ + M → CH ₃ + H + M	17.1	0	88.4	Hartig et al. (1971)
2.12 CH ₄ + H → CH ₃ + H ₂	14.1	0	11.9	Baldwin et al. (1970a)
2.13 CH ₄ + OH → CH ₃ + H ₂ O	3.5	3.08	2.0	Zellner and Steinert (1976)
2.14 CH ₄ + O → CH ₃ + OH	13.2	0	9.2	Herron (1969)
2.15 CH ₄ + HO ₂ → CH ₃ + H ₂ O ₂	13.3	0	18.0	Skinner et al. (1972)
2.16 CH ₃ + HO ₂ → CH ₃ O + OH	13.2	0	0.0	Colket (1975)
2.17 CH ₃ + OH → CH ₂ O + H ₂	12.6	0	0.0	Fenimore (1969)
2.18 CH ₃ + O → CH ₂ O + H	14.1	0	2.0	Peeters and Mahnen (1973)
2.19 CH ₃ + O ₂ → CH ₂ O + O	13.4	0	29.0	Brabbs and Brokaw (1975)
2.20 CH ₂ O + CH ₃ → C ₂ H ₄ + HCO	10.0	0.5	6.0	Tunder et al.
2.21 CH ₃ + HCO → CH ₄ + CO	11.5	0.5	0.0	Tunder et al.
2.22 CH ₃ + HO ₂ → CH ₄ + O ₂	12.0	0	0.4	Skinner et al. (1972)
2.23 CH ₂ O + M → CH ₂ O + H + M	13.7	0	21.0	Brabbs and Brokaw (1975)
2.24 CH ₂ O + O ₂ → CH ₂ O + HO ₂	12.0	0	6.0	Engleman (1976)
2.25 CH ₂ O + M → HCO + H + M	16.7	0	72.0	Schecker and Jost (1969)
2.26 CH ₂ O + OH → HCO + H ₂ O	14.7	0	6.3	Bowman (1975)
2.27 CH ₂ O + H → HCO + H ₂	12.6	0	3.8	Westenberg and deHaas (1972a)
2.28 CH ₂ O + O → HCO + OH	13.7	0	4.6	Bowman (1975)
2.29 CH ₂ O + HO ₂ → HCO + H ₂ O ₂	12.0	0	8.0	Lloyd (1974)
2.30 HCO + OH → CO + H ₂ O	14.0	0	0.0	Bowman (1970)
2.31 HCO + M → H + CO + M	14.2	0	19.0	Westbrook et al. (1977)
2.32 HCO + H → CO + H ₂	14.3	0	0.0	Niki et al. (1969)
2.33 HCO + O → CO + OH	14.0	0	0.0	Westenberg and deHaas (1972b)
2.34 HCO + HO ₂ → CH ₂ O + O ₂	14.0	0	3.0	Baldwin and Walker (1973)
2.35 HCO + O ₂ → CO + HO ₂	12.5	0	7.0	Westbrook et al. (1977)
2.36 CO + OH → CO ₂ + H	7.1	1.3	-0.8	Baulch and Drysdale (1974)
2.37 CO + HO ₂ → CO ₂ + OH	14.0	0	23.0	Baldwin et al. (1970b)
2.38 CO + O + M → CO ₂ + M	15.8	0	4.1	Simonaitis and Hecklen (1972)
2.39 CO ₂ + O → CO + O ₂	12.4	0	43.8	Gardiner et al. (1971)
2.40 H + O ₂ → O + OH	14.3	0	16.8	Baulch et al. (1973a)
2.41 H ₂ + O → H + OH	10.3	1	8.9	Baulch et al. (1973b)
2.42 H ₂ O + O → OH + OH	13.5	0	18.4	Baulch et al. (1973b)
2.43 H ₂ O + H → H ₂ + OH	14.0	0	20.3	Baulch et al. (1973b)

TABLE 2. (Continued)

Reaction	Rate ^a			
	log A	n	E _a	Reference ^b
2.44 H ₂ O ₂ + OH → H ₂ O + HO ₂	13.0	0	1.8	Baulch et al. (1973b)
2.45 H ₂ O + M → H + OH + M	16.3	0	105.1	Baulch et al. (1973b)
2.46 H + O ₂ + M → HO ₂ + M	15.2	0	-1.0	Baulch et al. (1973b)
2.47 HO ₂ + O → OH + O ₂	13.7	0	1.0	Lloyd (1974)
2.48 HO ₂ + H → OH + OH	14.4	0	1.9	Baulch et al. (1973b)
2.49 HO ₂ + H → H ₂ + O ₂	13.4	0	0.7	Baulch et al. (1973b)
2.50 HO ₂ + OH → H ₂ O + O ₂	13.7	0	1.0	Lloyd (1974)
2.51 H ₂ O ₂ + O ₂ → HO ₂ + HO ₂	13.6	0	42.6	Lloyd (1974)
2.52 H ₂ O ₂ + M → OH + OH + M	17.1	0	45.5	Baulch et al. (1973b)
2.53 H ₂ O ₂ + H → HO ₂ + H ₂	12.2	0	3.8	Baulch et al. (1973b)
2.54 O + H + M → OH + M	16.0	0	0.0	Moretti (1965)
2.55 O ₂ + M → O + O + M	15.7	0	115.0	Jenkins et al. (1967)
2.56 H ₂ + M → H + H + M	14.3	0	96.0	Baulch et al. (1973b)
2.57 C ₂ H ₆ → CH ₃ + CH ₃	19.4	-1	88.3	Pacey (1973)
2.58 C ₂ H ₆ + CH ₃ → C ₂ H ₅ + CH ₄	-0.3	4	8.3	Clark and Dove (1973)
2.59 C ₂ H ₆ + H → C ₂ H ₅ + H ₂	2.7	3.5	5.2	Clark and Dove (1973)
2.60 C ₂ H ₆ + OH → C ₂ H ₅ + H ₂ O	13.8	0	2.4	Greiner (1970)
2.61 C ₂ H ₆ + O → C ₂ H ₅ + OH	13.4	0	6.4	Herron and Huie (1973)
2.62 C ₂ H ₅ → C ₂ H ₄ + H	13.6	0	38.0	Lin and Back (1966)
2.63 C ₂ H ₅ + O ₂ → C ₂ H ₄ + HO ₂	12.0	0	5.0	Cooke and Williams (1971)
2.64 C ₂ H ₅ + C ₂ H ₃ → C ₂ H ₄ + C ₂ H ₄	17.5	0	35.6	Benson and Haugen (1967)
2.65 C ₂ H ₄ + O → CH ₃ + HCO	13.0	0	1.1	David et al. (1972)
2.66 C ₂ H ₄ + M → C ₂ H ₃ + H + M	17.6	0	98.2	Just et al. (1977)
2.67 C ₂ H ₄ + H → C ₂ H ₃ + H ₂	13.8	0	6.0	Benson and Haugen (1967)
2.68 C ₂ H ₄ + OH → C ₂ H ₃ + H ₂ O	14.0	0	3.5	Baldwin et al. (1966)
2.69 C ₂ H ₄ + O → CH ₂ O + CH ₂	13.4	0	5.0	Peeters and Mahnen (1973)
2.70 C ₂ H ₃ + M → C ₂ H ₂ + H + M	16.5	0	40.5	Benson and Haugen (1967)
2.71 C ₂ H ₂ + M → C ₂ H + H + M	14.0	0	114.0	Jachimowski (1977)
2.72 C ₂ H ₂ + O ₂ → HCO + HCO	12.6	0	28.0	Gardiner and Walker (1968)
2.73 C ₂ H ₂ + H → C ₂ H + H ₂	14.3	0	19.0	Browne et al. (1969)
2.74 C ₂ H ₂ + OH → C ₂ H + H ₂ O	12.8	0	7.0	Vandooren and Van Tiggelen (1977)
2.75 C ₂ H ₂ + O → C ₂ H + OH	15.5	-0.6	17.0	Browne et al. (1969)
2.76 C ₂ H ₂ + O → CH ₂ + CO	13.8	0	4.0	Vandooren and Van Tiggelen (1977)
2.77 C ₂ H + O ₂ → HCO + CO	13.0	0	7.0	Browne et al. (1969)
2.78 C ₂ H + O → CO + CH	13.7	0	0.0	Browne et al. (1969)
2.79 CH ₂ + O ₂ → HCO + OH	14.0	0	3.7	Benson and Haugen (1967)
2.80 CH ₂ + O → CH + OH	11.3	0.68	25.0	Mayer et al. (1967)
2.81 CH ₂ + H → CH + H ₂	11.4	0.67	25.7	Mayer et al. (1967)
2.82 CH ₂ + OH → CH + H ₂ O	11.4	0.67	25.7	Peeters and Vinckier (1975)
2.83 CH + O ₂ → CO + OH	11.1	0.67	25.7	Peeters and Vinckier (1975)
2.84 CH + O ₂ → HCO + O	13.0	0	0.0	Jachimowski (1977)

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^aUnits are cm-mol-s-kcal. $k = AT^n \exp(-E_a/RT)$ ^bReferences refer to sources noted in the original article.

Detailed Premixed Flame Measurements

A. Propane/Air

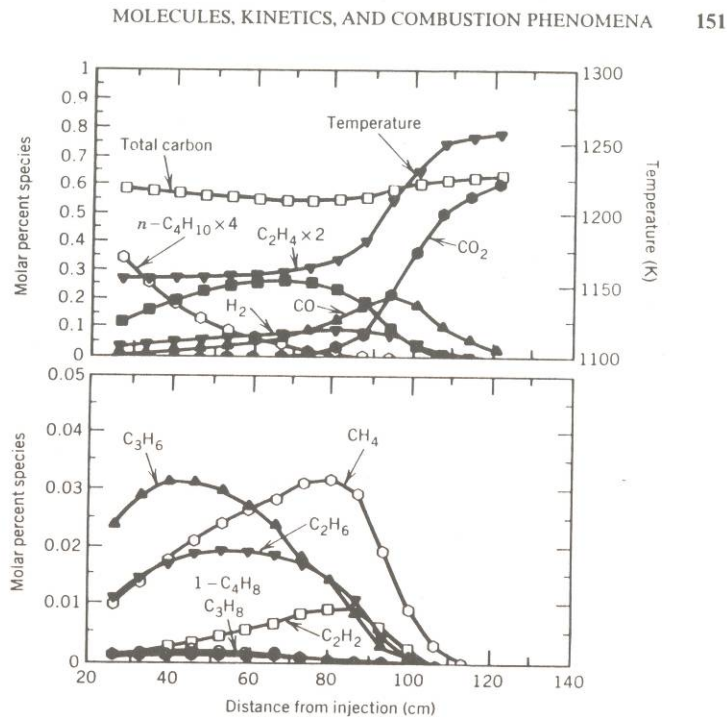


FIGURE 11. Species evolution for the reaction of *n*-butane and oxygen as a function of reaction distance. Data are from the Princeton Flow Reactor, for an initial equivalence ratio of 0.80, an initial reaction temperature of 1155 K, and atmospheric pressure. A distance of 1.0 cm corresponds to approximately 0.67 msec of reaction time. Figure from Ref. 54.

B. Butane/Air

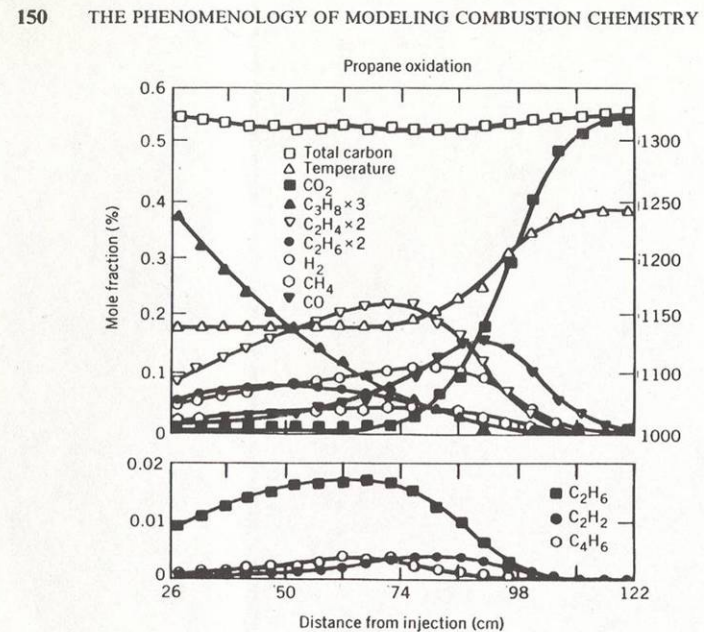


FIGURE 10. Species evolution for the reaction of propane and oxygen as a function of reaction distance. Data are from the Princeton Flow Reactor, for an initial equivalence ratio of 0.82, an initial reaction temperature of 1138 K, and atmospheric pressure. A distance of 1.0 cm corresponds to approximately 0.90 msec of reaction time. Figure from Ref. 53.

From F. L. Dryer, "The Phenomenology of Modeling Combustion Chemistry," in *Fossil Fuel Combustion: A Source Book*, edited by W. Bartok and A. F. Sarofim, John Wiley & Sons, New York (1991).

Global & Simplified Kinetic Expressions

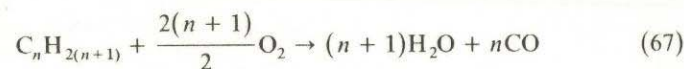


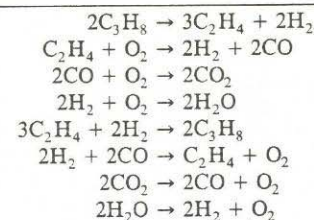
TABLE 7. Parameters for Two-Step Reaction Mechanism, Giving Best Agreement between Experimental and Computed Flammability Limits^a

Fuel	A	E _a	a	b
CH ₄	2.8 × 10 ⁹	48.4	-0.3	1.3
CH ₄	1.5 × 10 ⁷	30.0	-0.3	1.3
C ₂ H ₆	1.3 × 10 ¹²	30.0	0.1	1.65
C ₃ H ₈	1.0 × 10 ¹²	30.0	0.1	1.65
C ₄ H ₁₀	8.8 × 10 ¹¹	30.0	0.15	1.6
C ₅ H ₁₂	7.8 × 10 ¹¹	30.0	0.25	1.5
C ₆ H ₁₄	7.0 × 10 ¹¹	30.0	0.25	1.5
C ₇ H ₁₆	6.3 × 10 ¹¹	30.0	0.25	1.5
C ₈ H ₁₈	5.7 × 10 ¹¹	30.0	0.25	1.5
C ₈ H ₁₈	9.6 × 10 ¹²	40.0	0.25	1.5
C ₉ H ₂₀	5.2 × 10 ¹¹	30.0	0.25	1.5
C ₁₀ H ₂₂	4.7 × 10 ¹¹	30.0	0.25	1.5
CH ₃ OH	3.7 × 10 ¹²	30.0	0.25	1.5
C ₂ H ₅ OH	1.8 × 10 ¹²	30.0	0.15	1.6
C ₆ H ₆	2.4 × 10 ¹¹	30.0	-0.1	1.85
C ₇ H ₈	1.9 × 10 ¹¹	30.0	-0.1	1.85

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^aSame units as in Table 6.

TABLE 8. Summary of the Modified Four-Step, Reversible Mechanism for Laminar Flames of Propane and Air



With rate expressions:

$$\begin{aligned} R_1 &= f_1(P) 2.089 \times 10^{17} \exp(-49,600/RT) [C_3H_8]^{0.50} [O_2]^{1.07} [C_2H_4]^{0.40} \\ R_2 &= f_2(P) 2 \times 10^{13} \exp(-50,000/RT) [C_2H_4]^{0.90} [O_2]^{1.18} [C_3H_8]^{-0.37} \\ R_3 &= S(\phi) 1.5 \times 10^{13} \exp(-40,000/RT) [CO]^{1.0} [O_2]^{0.25} [H_2O]^{0.50} \\ R_4 &= 3.311 \times 10^{13} \exp(-38,100/RT) [H_2]^{0.85} [O_2]^{1.42} [C_2H_4]^{-0.56} \\ R_5 &= 4.920 \times 10^8 \exp(-49,600/RT) [C_3H_8]^{0.127} [O_2]^{1.07} [C_2H_4]^{0.40} \\ R_6 &= 2.25 \times 10^9 \exp(-50,000/RT) [C_2H_4]^{0.528} [O_2]^{1.18} [C_3H_8]^{-0.37} \\ R_7 &= 4.16 \times 10^{16} T^{-1/2} \exp(-106,950/RT) [CO_2]^{1.0} [O_2]^{-0.25} [H_2O]^{0.50} \\ R_8 &= 6.12 \times 10^{15} T^{-1/2} \exp(-100,586/RT) [H_2]^{-0.153} [O_2]^{0.916} [C_2H_4]^{-0.563} [H_2O]^{1.0}, \end{aligned}$$

where

$$\begin{aligned} f_1(P) &= 6.434 P^{-0.8116} \\ f_2(P) &= 1.115 - 1.125 e^{-0.251} \\ S(\phi) &= \min[1.0, 16.0 \exp(-2.48\phi)] \end{aligned}$$

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From F. L. Dryer, "The Phenomenology of Modeling Combustion Chemistry," in *Fossil Fuel Combustion: A Source Book*, edited by W. Bartok and A. F. Sarofim, John Wiley & Sons, New York (1991).

NO_x (Nitrogen Oxides from Combustion)

A. Thermal NO_x

- $\text{N}_2 + \text{O}_2 \rightarrow 2\text{NO}$ (involves N, O, and OH radicals)
- Nitrogen and oxygen only, no other major species
- Dominant source of NO_x in gaseous hydrocarbon combustion (methane, etc.)

B. Fuel NO_x

- Nitrogen in fuel \rightarrow NO, NO₂ and N₂O
- Example: pyridine combustion (), coal combustion
- Dominant source of NO_x in coal combustion

C. Prompt NO_x

- CH or $\text{CH}_2 + \text{N}_2 \rightarrow \text{HCN} \rightarrow \text{NO}$, etc.
- Hard to quantify because radical concentrations are generally unknown
- Not usually a dominant source of NO_x in combustion

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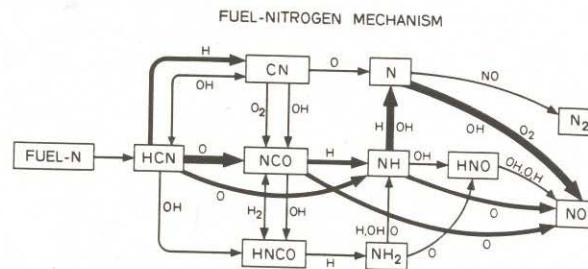


FIGURE 12. Schematic diagram of the principal reaction paths in the fuel nitrogen conversion process in flames.

TABLE 10. Rate Coefficients for Thermal NO Formation Reactions^a

Reaction Number	Reaction	A	B	C (K)
18	$O + N_2 \rightarrow NO + N$	1.8(11)	0	38.4(3)
-19	$O + NO \rightarrow N + O_2$	3.8(6)	1.0	20.8(3)
-20	$H + NO \rightarrow OH + N$	2.6(11)	0	25.4(3)

^aFrom Hanson and Salimian.²⁶ Units: kgmol, m³, K, sec; $k = AT^B \exp(-C/T)$.

3.1. Thermal NO Formation

The three principal reactions that comprise the thermal NO formation mechanism are



The rate coefficients for both the forward and reverse reactions have been measured over a wide temperature range (Table 10).²⁶

Invoking a steady-state approximation for the N-atom concentration* and assuming that reaction (9) is partially equilibrated, the NO formation rate due to the thermal mechanism may be expressed,

$$\frac{d(NO)}{dt} = 2k_{18}(O)(N_2) \frac{1 - (NO)^2/K(O_2)(N_2)}{1 + k_{-18}(NO)/[k_{19}(O_2) + k_{20}(OH)]} \quad (21)$$

where $K = (k_{18}/k_{-18})(k_{19}/k_{-19})$ = equilibrium constant for the reaction $N_2 + O_2 \rightleftharpoons 2NO$. Calculation of the NO formation rate requires values of the local temperature and the local concentrations of O_2 , N_2 , O , and OH .

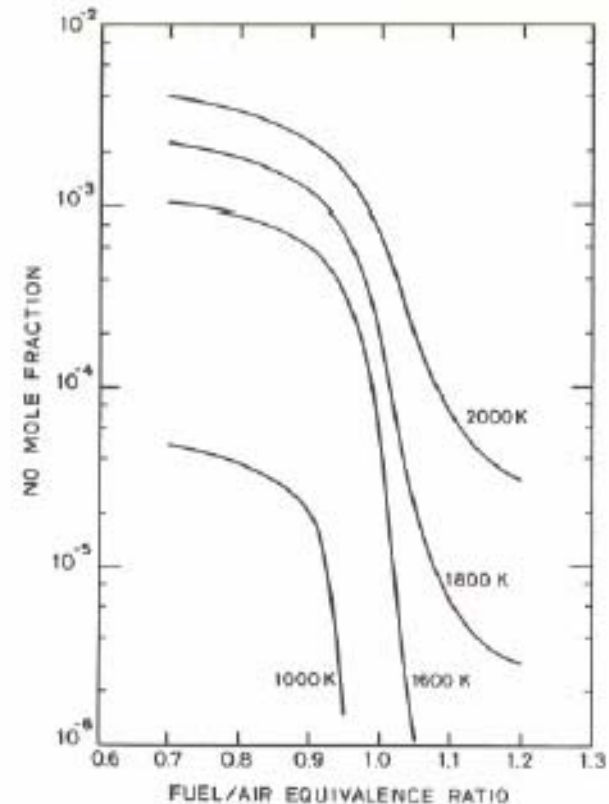


FIGURE 5. Equilibrium NO mole fractions for premixed methane-air combustion at a pressure of 1 atm.

From F. L. Dryer, "The Phenomenology of Modeling Combustion Chemistry," in *Fossil Fuel Combustion: A Source Book*, edited by W. Bartok and A. F. Sarofim, John Wiley & Sons, New York (1991).

FATE OF NITROGEN OXIDES IN THE ATMOSPHERE

