

# Final Exam

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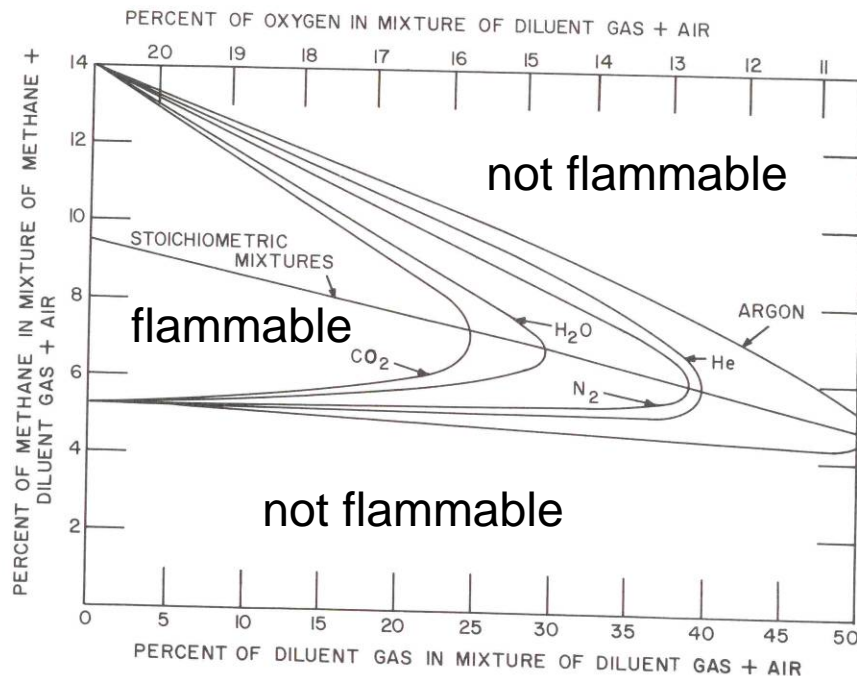
- **Wednesday, Dec. 17, 7 am to 10 am**
- Closed Book, Closed Notes
- Combustion Terms
  - From the sheet on the “pre-test”
- Short Answers
  - Describe this, how does this work, etc.
- Problems
  - Like the homework
  - Basis for solid fuels (daf?), oxygen demand, etc.
  - Bring a calculator!!
- I am aiming for 1-2 hours (not 3!)
  - Come at 7 am anyway

# Outline

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1. Flammability Limits
2. Flame Speeds
  - Flashback
  - Laminar vs. Turbulent
3. Explosions
  - Deflagration vs. Detonation
4. Pepcon video
5. Lab demos

# 1. Flammability Limits



(from Lewis and von Elbe, 1987)

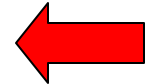
- Measured in premixed gases
- Fuel Rich limit
- Fuel Lean limit
- Effects of diluents (see figure at left)
- Also functions of pressure
- Must be measured

# Flammability Limits

(in air at 1 atm total pressure)

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Species	Lean ( $\phi$ )	Rich ( $\phi$ )
Acetylene	0.19	$\infty$
Carbon Monoxide	0.34	6.76
Methane	0.46	1.64
Methanol	0.48	4.08
Ethane	0.50	2.72
Ethylene	0.41	6.1
Hydrogen	0.14	2.54
Propane	0.51	2.83
n-Decane	0.36	3.92
n-Octane	0.51	4.25



(from Turns, p. 236)

(from The John Zink Combustion Handbook, 2001, p. 45)

TABLE 2.4 Combustion Data for Hydrocarbons

Hydrocarbon	Formula	Higher Heating Value (vapor), Btu lb <sub>m</sub> <sup>-1</sup>	Theor. Air/fuel Ratio, by mass	Max Flame Speed, (ft s <sup>-1</sup> )	Adiabatic Flame Temp (in air) (°F)	Ignition Temp (in air) (°F)	Flash Point (°F)	Flammability Limits (in air) (% by volume)	
Paraffins or Alkanes									
Methane	CH <sub>4</sub>	23875	17.195	1.1	3484	1301	Gas	5.0	15.0
Ethane	C <sub>2</sub> H <sub>6</sub>	22323	15.899	1.3	3540	968–1166	Gas	3.0	12.5
Propane	C <sub>3</sub> H <sub>8</sub>	21669	15.246	1.3	3573	871	Gas	2.1	10.1
<i>n</i> -Butane	C <sub>4</sub> H <sub>10</sub>	21321	14.984	1.2	3583	761	-76	1.86	8.41
<i>iso</i> -Butane	C <sub>4</sub> H <sub>10</sub>	21271	14.984	1.2	3583	864	-117	1.80	8.44
<i>n</i> -Pentane	C <sub>5</sub> H <sub>12</sub>	21095	15.323	1.3	4050	588	< -40	1.40	7.80
<i>iso</i> -Pentane	C <sub>5</sub> H <sub>12</sub>	21047	15.323	1.2	4055	788	< -60	1.32	9.16
Neopentane	C <sub>5</sub> H <sub>12</sub>	20978	15.323	1.1	4060	842	Gas	1.38	7.22
<i>n</i> -Hexane	C <sub>6</sub> H <sub>14</sub>	20966	15.238	1.3	4030	478	-7	1.25	7.0
Neohexane	C <sub>6</sub> H <sub>14</sub>	20931	15.238	1.2	4055	797	-54	1.19	7.58
<i>n</i> -Heptane	C <sub>7</sub> H <sub>16</sub>	20854	15.141	1.3	3985	433	25	1.00	6.00
Triptane	C <sub>7</sub> H <sub>16</sub>	20824	15.151	1.2	4035	849	—	1.08	6.69
<i>n</i> -Octane	C <sub>8</sub> H <sub>18</sub>	20796	15.093	—	—	428	56	0.95	3.20
<i>iso</i> -Octane	C <sub>8</sub> H <sub>18</sub>	20770	15.093	1.1	—	837	10	0.79	5.94
Olefins or Alkenes									
Ethylene	C <sub>2</sub> H <sub>4</sub>	21636	14.807	2.2	4250	914	Gas	2.75	28.6
Propylene	C <sub>3</sub> H <sub>6</sub>	21048	14.807	1.4	4090	856	Gas	2.00	11.1
Butylene	C <sub>4</sub> H <sub>8</sub>	20854	14.807	1.4	4030	829	Gas	1.98	9.65
<i>iso</i> -Butene	C <sub>4</sub> H <sub>8</sub>	20737	14.807	1.2	—	869	Gas	1.8	9.0
<i>n</i> -Pentene	C <sub>5</sub> H <sub>10</sub>	20720	14.807	1.4	4165	569	—	1.65	7.70
Aromatics									
Benzene	C <sub>6</sub> H <sub>6</sub>	18184	13.297	1.3	4110	1044	12	1.35	6.65
Toluene	C <sub>7</sub> H <sub>8</sub>	18501	13.503	1.2	4050	997	40	1.27	6.75
<i>p</i> -Xylene	C <sub>8</sub> H <sub>10</sub>	18663	13.663	—	4010	867	63	1.00	6.00
Other Hydrocarbons									
Acetylene	C <sub>2</sub> H <sub>2</sub>	21502	13.297	4.6	4770	763–824	Gas	2.50	81
Naphthalene	C <sub>10</sub> H <sub>8</sub>	17303	12.932	—	4100	959	174	0.90	5.9

These adiabatic flame temperatures are a little bit off!

Note: Based largely on: "Gas Engineers' Handbook", American Gas Association, Inc., Industrial Press, 1967. For heating value in J kg<sup>-1</sup>, multiply the value in Btu lb<sub>m</sub><sup>-1</sup> by 2324. For flame speed in m s<sup>-1</sup>, multiply the value in ft s<sup>-1</sup> by 0.3048.

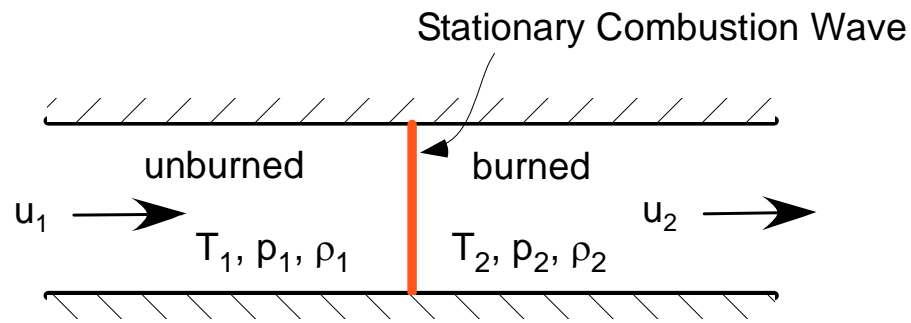
#### REFERENCES

*American Institute of Physics Handbook*, 2nd ed., D.E. Gray, Ed., McGraw-Hill Book Company, 1955.  
*Chemical Engineers' Handbook*, 4th ed., R.H. Perry, C.H. Chilton, and S.D. Kirkpatrick, Eds., McGraw-Hill Book Company, 1963.  
*Handbook of Chemistry and Physics*, 53rd ed., R.C. Weast, Ed., The Chemical Rubber Company, 1972.  
*Handbook of Laboratory Safety*, 2nd ed., N.V. Steere, Ed., The Chemical Rubber Company, 1971.  
*Physical Measurements in Gas Dynamics and Combustion*, Princeton University Press, 1954.

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## 2. Flame Speeds

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- Usually measured at stoichiometric conditions ( $\phi = 1.0$ )
- Premixed gases
- Refers to velocity of unburned gas ( $u_1$ )
- Must be measured

(from **In Air** Zink Combustion Handbook, 2001, p. 45)

**TABLE 2.4** Combustion Data for Hydrocarbons

Hydrocarbon	Formula	Higher Heating Value (vapor), Btu lb <sub>m</sub> <sup>-1</sup>	Theor. Air/fuel Ratio, by mass	Max Flame Speed, (ft s <sup>-1</sup> )	Adiabatic Flame Temp (in air) (°F)	Ignition Temp (in air) (°F)	Flash Point (°F)	Flammability Limits (in air) (% by volume)	
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All the same!

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Note: Based largely on: "Gas Engineers' Handbook", American Gas Association, Inc., Industrial Properties of Gases, 1967. For heating value in J kg<sup>-1</sup>, multiply the value in Btu lb<sub>m</sub><sup>-1</sup> by 2324. For flame speed in m s<sup>-1</sup>, multiply the value in ft s<sup>-1</sup> by 0.3048.

#### REFERENCES

American Institute of Physics Handbook, 1963.  
 Chemical Engineers' Handbook, 6th ed., McGraw-Hill Book Company, 1963.  
 Handbook of Chemistry and Physics, 54th ed., CRC Press, 1972.  
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All the same!

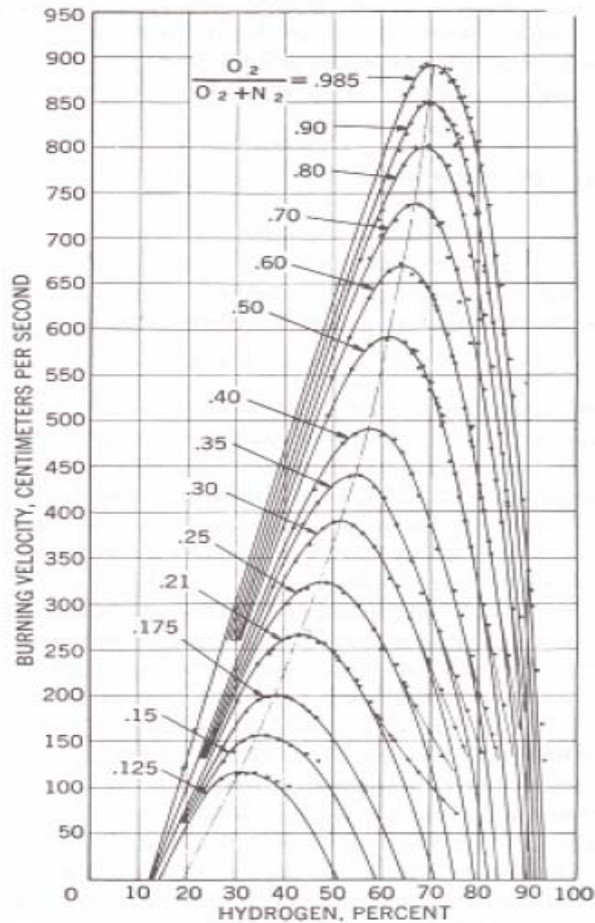
1.1 ft/s = 33 cm/s = 0.3 m/s

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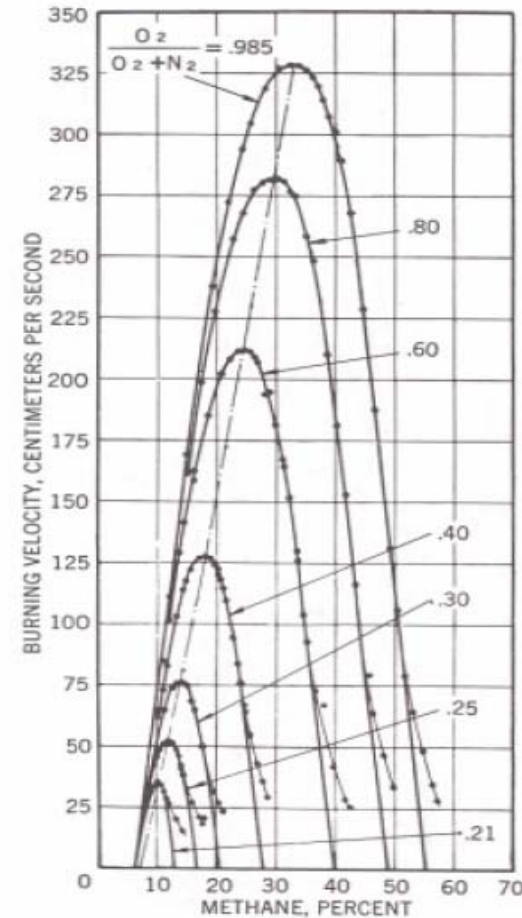


# Laminar Premixed Flame Speeds

(from Lewis and von Elbe, 1987, pp. 396, 401)



H<sub>2</sub>, O<sub>2</sub>, and N<sub>2</sub> at room T  
and atmospheric pressure

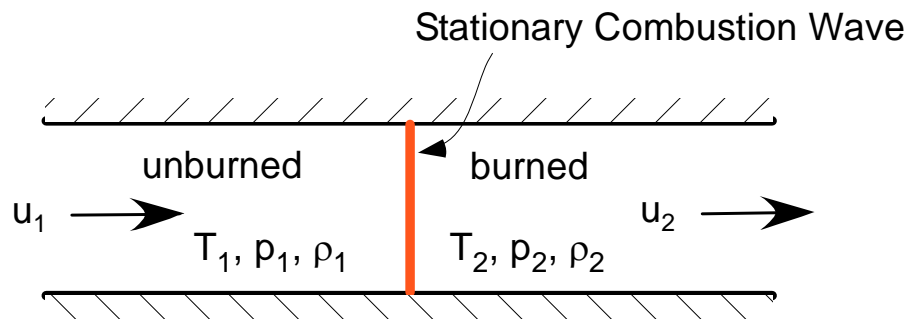


CH<sub>4</sub>, O<sub>2</sub>, and N<sub>2</sub> at room T  
and atmospheric pressure



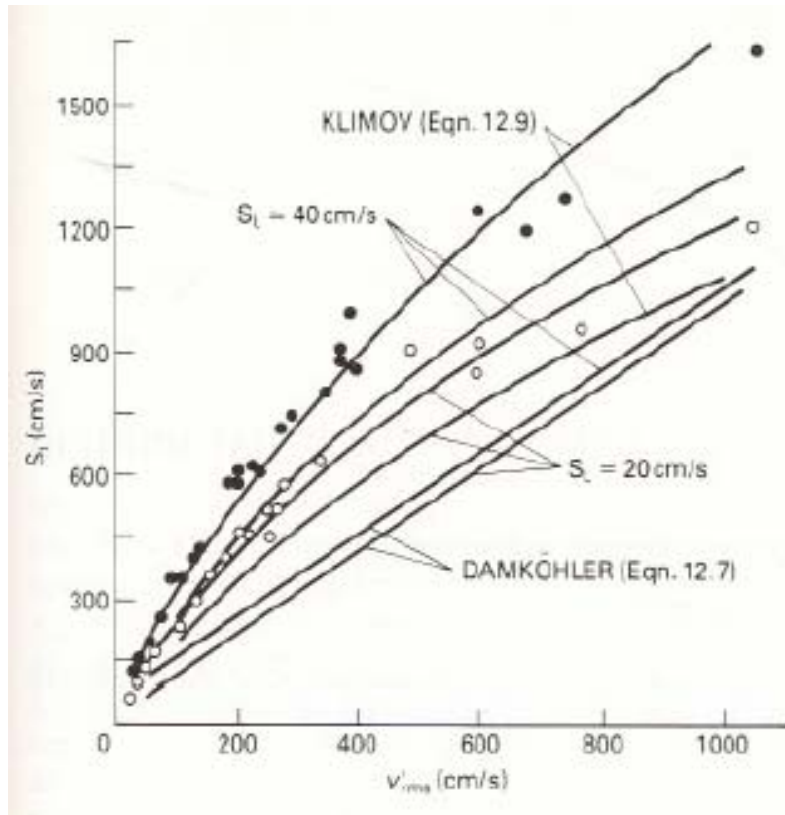
# Flame Speeds (cont.)

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- Flashback:  
when  $u_1 < S_L$   
(flame travels upstream)
- If  $u_1 > S_L$ , flashback is not possible!
- Refers to unburned gas velocity ( $u_1$ )
- Must get correct  $S_L$   
(correct concentrations, pressure, temperature, etc.)
- Most fuels similar, except  $C_2H_2$ ,  $C_2H_4$ , and  $H_2$

# Turbulent Flame Speeds ( $S_t$ )

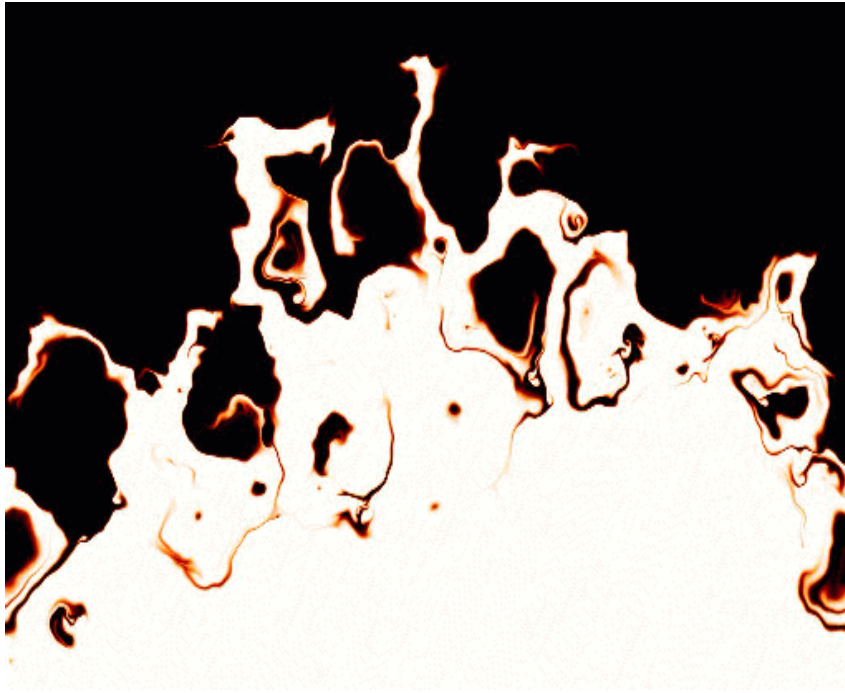


- Dependent on the turbulent fluctuation velocity ( $v'_{rms}$ )
- Depends on strength of recirculation, geometry, etc.
- Can be much higher than laminar flame speed ( $S_L$ )

So for  $S_L = 0.4$  m/s,  $S_t$  can be 15 m/s!!

# Why is $S_t > S_L$ ?

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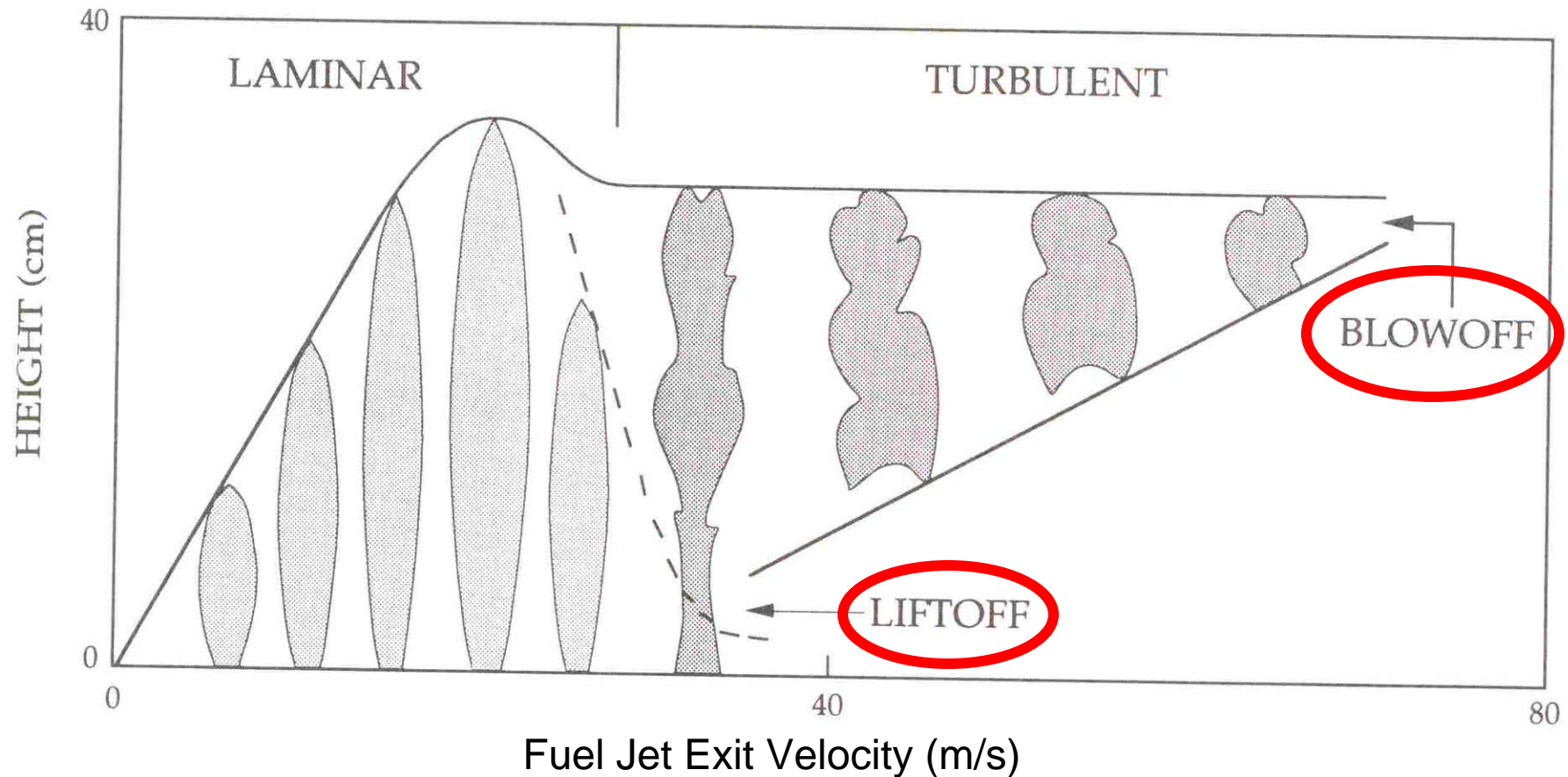


Movies:

<http://flash.uchicago.edu/~nata/combustion/>

- $S_L$  depends on molecular diffusion of heat and radicals
  - relatively slow
- $S_t$  depends on turbulent mixing of heat and radicals
  - can be much faster than molecular diffusion
- Greater surface area between burned and unburned in turbulent eddies

# Effects of Turbulence on a Gaseous Diffusion Flame



(from Glassman, Combustion, 1977, p. 285)

# Effects of Turbulence on Flames

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## A. Turbulent diffusion flames

- Enhanced mixing rate of oxidizer and fuel
- Enhanced surface area of flame (wrinkled)
- Higher heat release per unit volume

## B. Premixed flames

- Enhanced mixing rate of combustion products with reactants
  - Heat
  - Radical species

# 3. Explosions

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<b>Explosion</b>	Rapid expansion due to reaction (something blew up). Not really a technical term
<b>Deflagration</b>	Combustion at subsonic speeds
<b>Conflagration</b>	Large disastrous fire (may also mean a conflict or war)
<b>Detonation</b>	Combustion at supersonic speeds (includes shock wave)



# Examples:

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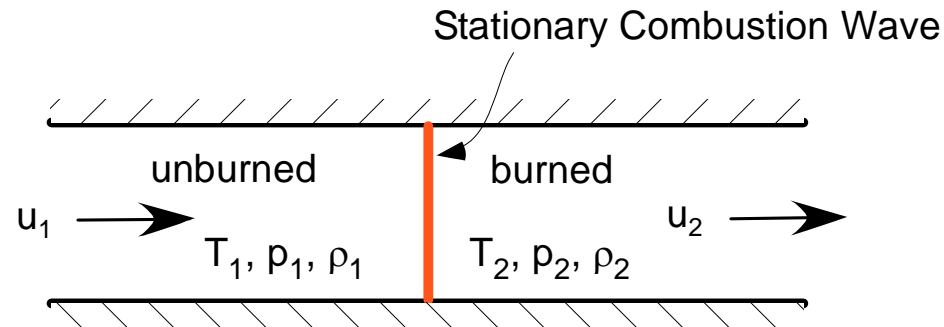
- Combustion of mixture in a tube with one or both ends open leads to deflagration.
- Combustion of mixture in closed vessel may lead to a detonation if the flame speed is high enough. The combustion wave follows the shock (pressure) wave.

# How Do You Get A Detonation?

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- Enormous energy release per unit volume
  - Short time
  - Small space
- A firecracker does not detonate
- Most bombs do not cause detonations

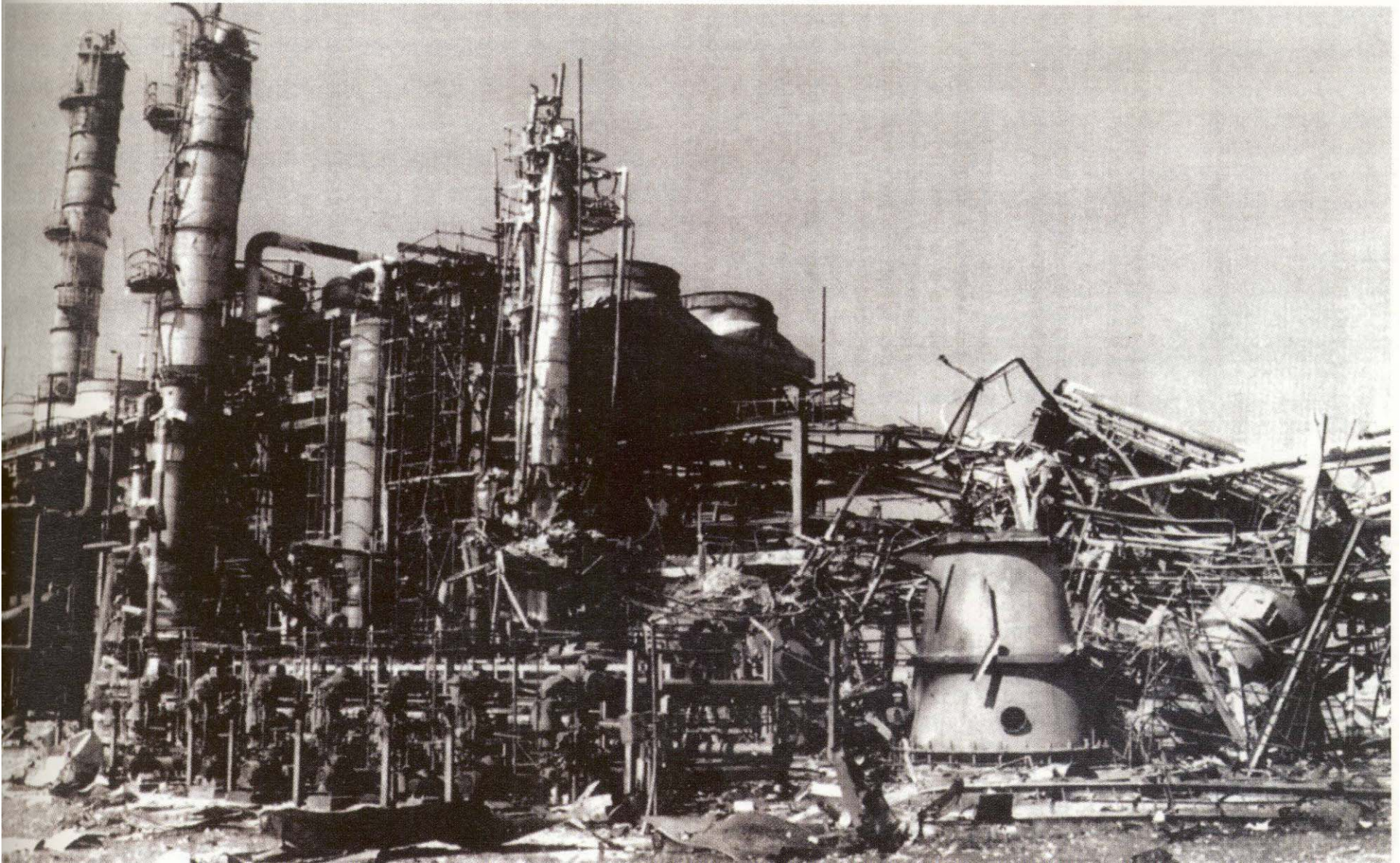
# Detonation vs. Deflagration in Gases



	<b>Detonation</b>	<b>Deflagration</b>
$u_1/c_1$	5 to 10	0.0001 to 0.03
$u_2/u_1$	0.4 to 0.7 (deceleration)	4 to 6 (acceleration)
$p_2/p_1$	13 to 55 (compression)	$\sim 0.98$ (slight expansion)
$T_2/T_1$	8 to 21 (heat addition)	4 to 16 (heat addition)
$\rho_2/\rho_1$	1.7 to 2.6	0.06 to 0.25



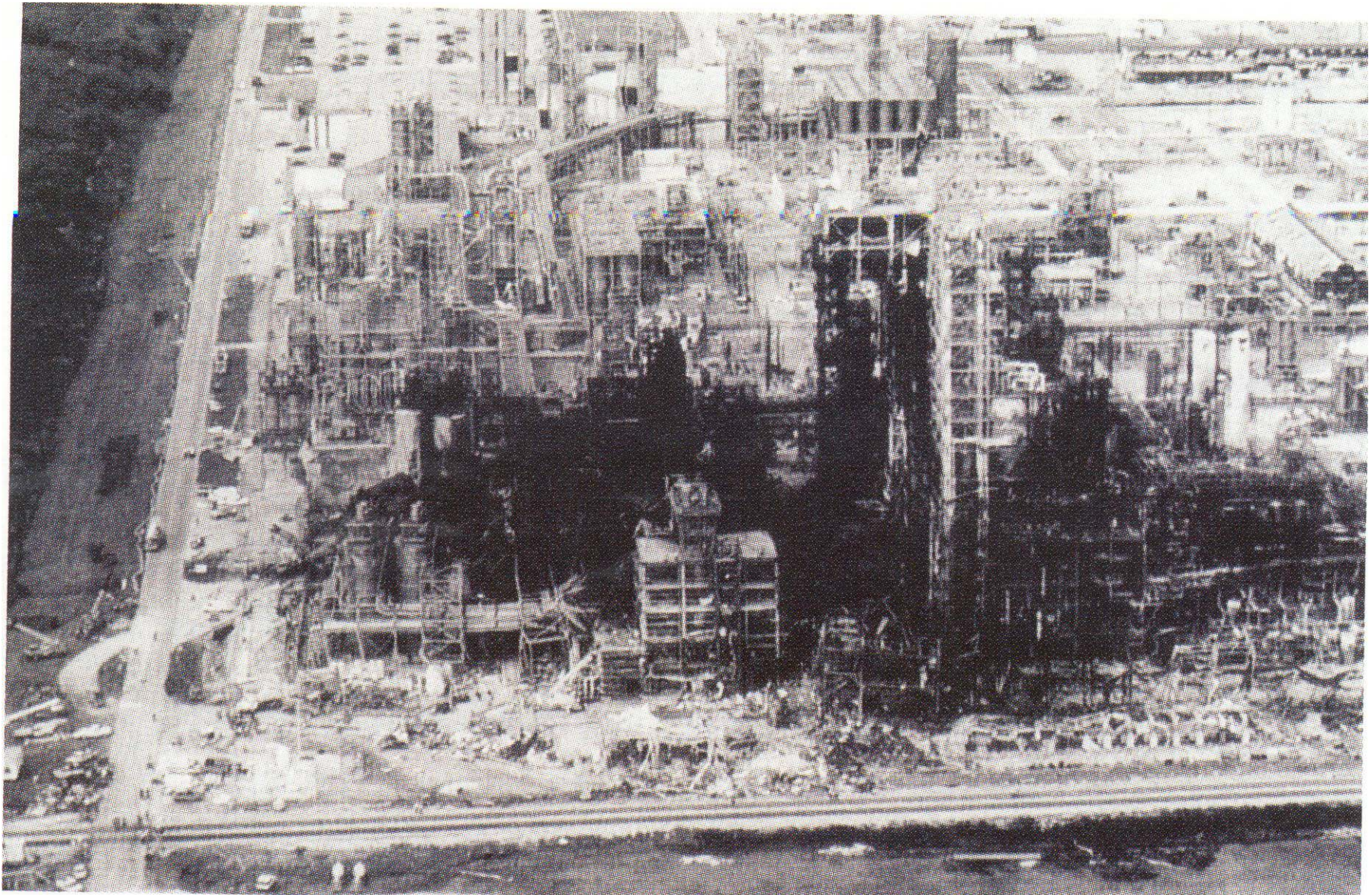
## Ethylene oxide plant explosion caused by autoignition



From John Zink Combustion Handbook



## Refinery damage due to improper maintenance procedures



From John Zink Combustion Handbook