

# Mathematical Modeling

ChE 436

Class 13

# 1. Types of mathematical models

- a) First principles  $\frac{V}{F_{A,0}} = \int \frac{dX_A}{-r_A}$
- b) Empirical FOPDT for everything
- c) Mixture of the two Semi-empirical

We will focus on mathematical models based on first principles in this chapter (Chapter 2)

## 2. Basic equations

- General conservation principle

$$\frac{\left[ \begin{array}{c} \text{accumulation of } S \\ \text{within a system} \end{array} \right]}{\text{time period}} = \frac{\left[ \begin{array}{c} \text{flow of } S \\ \text{into the system} \end{array} \right]}{\text{time period}} - \frac{\left[ \begin{array}{c} \text{flow of } S \\ \text{out of the system} \end{array} \right]}{\text{time period}} + \frac{\left[ \begin{array}{c} \text{amount of } S \\ \text{generated within} \\ \text{the system} \end{array} \right]}{\text{time period}} - \frac{\left[ \begin{array}{c} \text{amount of } S \\ \text{consumed within} \\ \text{the system} \end{array} \right]}{\text{time period}}$$

$$\text{Accumulation} = \text{In} - \text{Out} + \text{Generation} - \text{Consumption}$$

- where S can be:
  - total mass
  - mass of individual species
  - energy
  - momentum

# 3. Balances

- **Total Mass Balance:**

$$\frac{dm}{dt} = \frac{d(\rho V)}{dt} = \sum_{i=\text{inlet}} w_i - \sum_{j=\text{outlet}} w_j$$

$w_i$  = mass flow rate of stream i

- **Species Mole Balance:**

$$\frac{dn_A}{dt} = \frac{d(c_A V)}{dt} = \sum_{i=\text{inlet}} c_{Ai} q_i - \sum_{j=\text{outlet}} c_{Aj} q_j + r_A V$$

$C_A$  = moles A / volume  
 $q_i$  = volumetric flow rate of stream i

- **Total Energy Balance:**

$$\frac{dE}{dt} = \frac{d(U + K + P)}{dt} = \sum_{i=\text{inlet}} w_i \left[ h_i + \frac{z_i g_i}{g_c} + \frac{V_i^2}{2g_c} \right] - \sum_{j=\text{outlet}} w_j \left[ h_j + \frac{z_j g_j}{g_c} + \frac{V_j^2}{2g_c} \right] + Q + W_s$$

$h_i$  = enthalpy per unit mass of stream i

## 4. Forms of energy balance

- Neglecting potential and kinetic energy terms:

$$\frac{dE}{dt} = \frac{dU}{dt} = \sum_{i=\text{inlet}} w_i h_i - \sum_{j=\text{outlet}} w_j h_j + Q + W_s$$

- Note also that for liquid systems:

$$\frac{dU}{dt} \approx \frac{dH}{dt}$$

- In terms of temperature, the equation becomes (approximately):

$$\frac{d[\rho C_p V (T - T_{ref})]}{dt} = \sum_{i:\text{inlet}} w_i C_p (T_i - T_{ref}) - \sum_{j:\text{outlet}} w_j C_p (T_j - T_{ref}) + Q + W_s$$

- We will not be using a momentum equation in this class.



- What assumption does this book make about heat capacities?

# How to Develop a Transient Model

## (Table 2.1)

1. Identify objective
2. Draw a schematic diagram, labeling process variables
3. List all assumptions
4. Determine spatial dependence
  - yes = PDE
  - no = ODE
5. Write dynamic balances (mass, species, energy)
6. Other relations (thermo, reactions, geometry, etc.)
7. Degrees of freedom
  - Does # of eqns = # of unknowns?
8. Simplify (outputs on LHS, inputs on RHS)
9. Classify inputs as
  - Disturbances
  - Manipulated variables