

## Business

- Today: Exam Review
- Tues-Thurs: Exam 3
- Then
  - 5 Class Periods
  - 2 days for Lab (before & after Thanksgiving)
  - Review for Final
  - Final Exam on Dec. 16 (7-10 am)

## Chapter 12

How to get tuning parameters



## 1. ITAE

- Integrated time-weighted absolute error
- Graph at right is IAE
  - Needs time weighting

$$ITAE = \int_0^{\infty} t \cdot |e(t)| dt$$

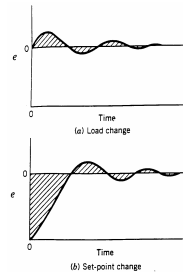


Figure 12.9. Graphical interpretation of IAE. The shaded area is the IAE value.

Table 12.3 Controller Design Relations Based on the ITAE Performance Index and a First-Order-plus-Time-Delay Model (Smith and Corripio, 1997)<sup>a</sup>

Type of Input	Type of Controller	Mode	A	B
Disturbance	PI	P	0.859	-0.977
		I	0.674	-0.680
		D	0.842	-0.738
Disturbance	PID	P	1.357	-0.947
		I	0.381	0.995
		D	0.586	-0.916
Set point	PI	P	1.03 <sup>b</sup>	-0.165 <sup>b</sup>
		I	0.965	-0.85
		D	0.796 <sup>b</sup>	-0.1465 <sup>b</sup>
Set point	PID	P	0.308	0.929
		I		
		D		

<sup>a</sup> Design relation:  $Y = A(\theta/\tau)^B$  where  $Y = KK_c$  for the proportional mode,  $\tau/\tau_I$  for the integral mode, and  $\tau/\tau_D$  for the derivative mode.

<sup>b</sup> For set-point changes, the design relation for the integral mode is  $\tau/\tau_I = A + B(\theta/\tau)$ .

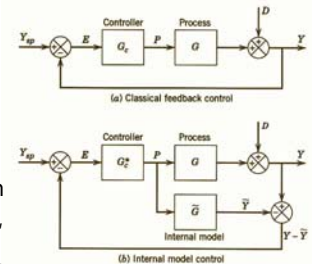
So for a PI controller  
 $K_p K_c = A (\theta/\tau_p)^B$  from P Mode  
 $\tau_p/\tau_I = A + B (\theta/\tau_p)$  from I Mode

## 2. Direct Synthesis

- Pick out form desired for  $Y/Y_{sp}$ 
  - FOPDT
  - Second order
- Adjust  $G_c$  to make this happen
  - May or may not look like PID controller
- Gives some values for  $K_c$ ,  $\tau_I$ , and  $\tau_D$  in special cases

## 3. Internal Model Control

- Use a model of the process
  - May use a time delay
- Compare process response to model response
- Change block diagram
- Gives values for  $K_c$ ,  $\tau_I$ , and  $\tau_D$ 
  - Table 12.1 and Control Station





## Other Stuff in Ch. 12

- On-line controller tuning
  - In closed loop mode
- Recommendations for different systems
  - PI vs PID, etc.
- Troubleshooting
  - Equipment problems
    - Sticky valve stem
    - Fouled heat exchanger
  - Change in feed rate conditions
  - Cavitation in pumps

