

Practical Combustion

Class 3

1

1a. Comparison of Combustors

Modified from Table 5.2 in Smoot & Smith, 1985

	Fixed Bed	Fluidized Bed	Entrained Flow
Particle Size	10-50 mm	1.5-6 mm	1-100 μm
Operating T (K)	< 2000	1000-1400	1900-2000
Residence Time (s)	500-50,000	10-500	1-2
Coal Feed Rate (kg/hr)	< 40,000 (BYU heating plant was at 5000)	< 40,000	< 450,000
Advantages	Simple Low grinding costs	Low SO_x & NO_x Low slagging Multi-fuel Low corrosion	High efficiency High capacity
Disadvantages	Emissions, especially particulates Efficiency Low capacity	Feeding fuel Softening coal Low capacity Risk (not established)	High NO_x Fly ash capture Grinding costs

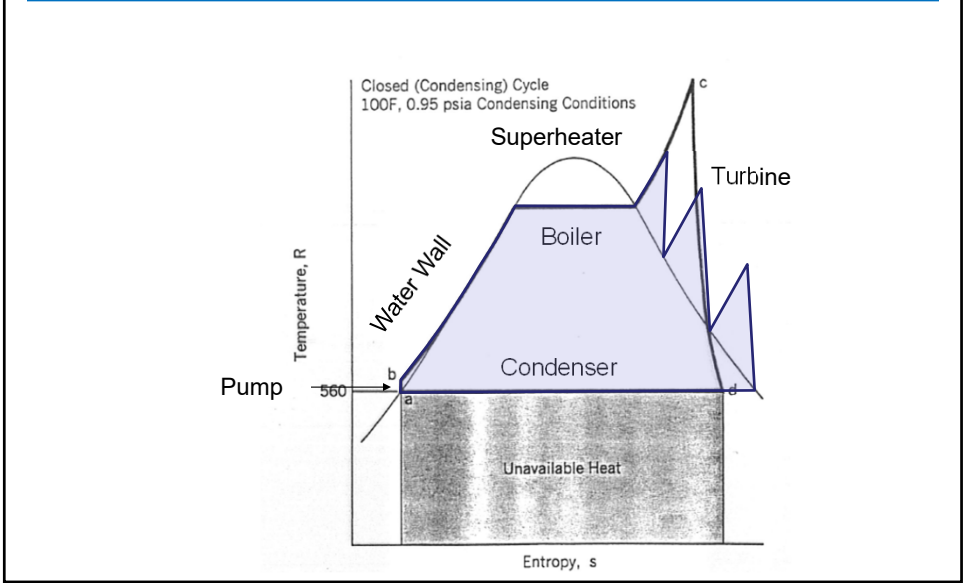
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From Steam, by Babcock & Wilcox

The diagram illustrates the internal structure of a 455 MW Radiant Boiler. Key components and flow paths include:

- Coal Bunker** and **Low NO_x Burners** at the top left, feeding into the **Furnace**.
- Platen Secondary Superheater** and **Secondary Superheater** located within the furnace area.
- Reheat Superheater** and **Convection Pass** in the upper right section.
- Primary Superheater** and **Economizer** in the middle right section.
- Secondary Air Duct** and **Air Heater** in the lower right section.
- Primary Air Duct** and **Tempering Air Duct** at the bottom, connected to **Pulverizers** and **Primary Air Fans**.
- Steam Drum** at the top left, with associated piping.
- From FD Fans** and **To ID Fan** connections at the bottom right.

Rankine Cycles



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Types of Boilers

- Subcritical (38% efficiency, new)
 - 2400 psi (steam pressure)
 - $T_{\text{steam}} = 1000^{\circ}\text{F}$
- Supercritical (42% efficiency, new)
 - 3500 psi
 - $T_{\text{steam}} = 1000^{\circ}\text{F}$
- Ultrasupercritical (44% efficiency, new)
 - 4400 psi
 - 1150°F

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Gasifiers

- Pretty much the same story as combustors
- Challenges:
 - Getting heat to where gasification happens
 - Slagging
 - Air separation unit required?
- Pressure?
 - Reduces size of gasifier
 - Adds complexity
 - Feeding
 - Disposing of ash
 - Lower volatiles

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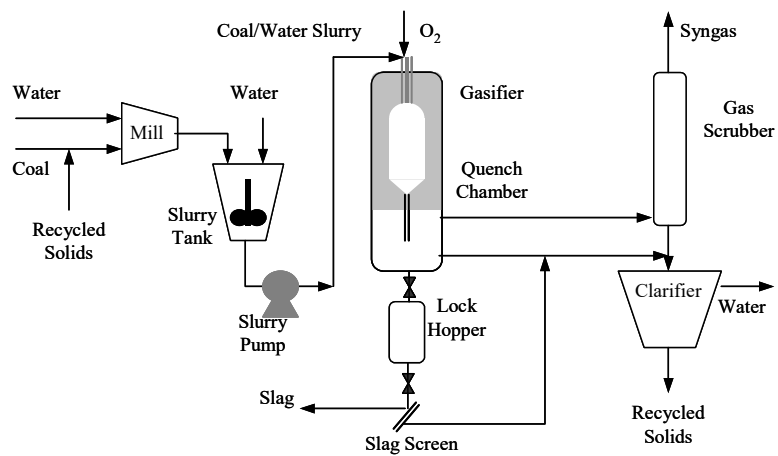
1b. Comparison of Gasifiers

Modified from Table 6.1 in Smoot & Smith, 1985

	Fixed Bed	Fluidized Bed	Entrained Flow
Particle Size	6-50 mm	0.5-2.5 mm	10-150 μm
Operating T (K)	1150-1300	600-1470	1150-2500
Residence Time (s)	1-3 hrs	20-150 min	0.4-12 s
Pressure (atm)	0.1-2	1-100	1-300
O ₂ /Coal ratio (mass)	0.14-0.81	0.25-0.97	0.28-1.17
CO+H ₂ (mol%)	39-66	2-80	35-91
CH ₄ (mol%)	2-15	3-68	0.1-17
High Heating Value (Btu/SCF)	250-320	300-800	115-550
Advantages	Established technology (Lurgi) Low thermal losses High turndown ratio	Multi-fuel, multi-size Moderate heat losses	Small, simple design High capacity per volume
Disadvantages	Low capacity	Softening coal Low capacity Risk (not established)	Down time due to wear of refractory and injectors

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GE Gasifier System



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2. Wall-Fired vs. Tangential

Tangential

- Lower NO_x due to large swirl zone
- More difficult to tune

Wall-Fired

- Less complex
- Easier to tune individual burners

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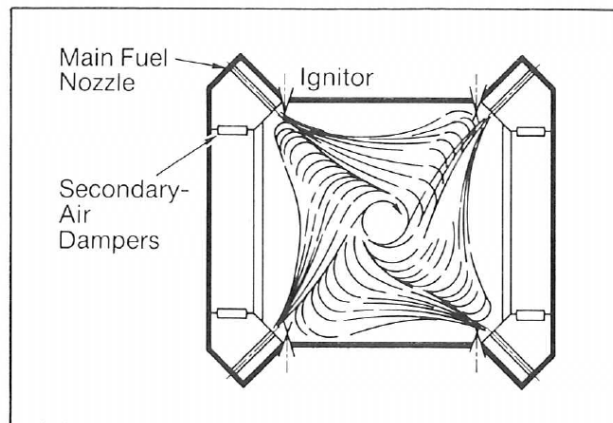


Fig. 3. Tangential firing pattern

From Combustion: Fossil Power Systems, by Combustion Engineering

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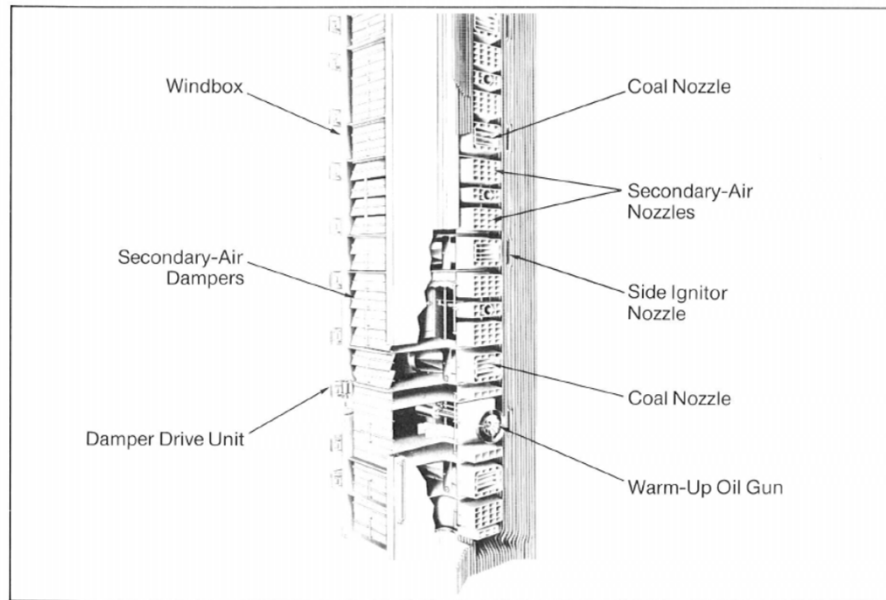


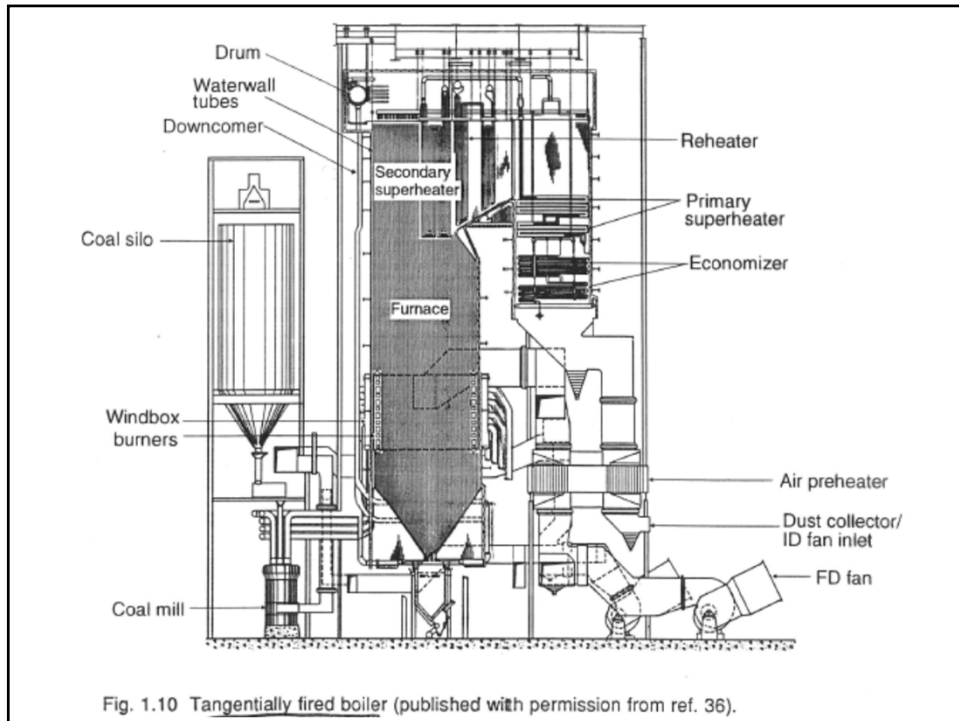
Fig. 4 Arrangement of corner windbox for tangential firing of coal

From Combustion: Fossil Power Systems, by Combustion Engineering

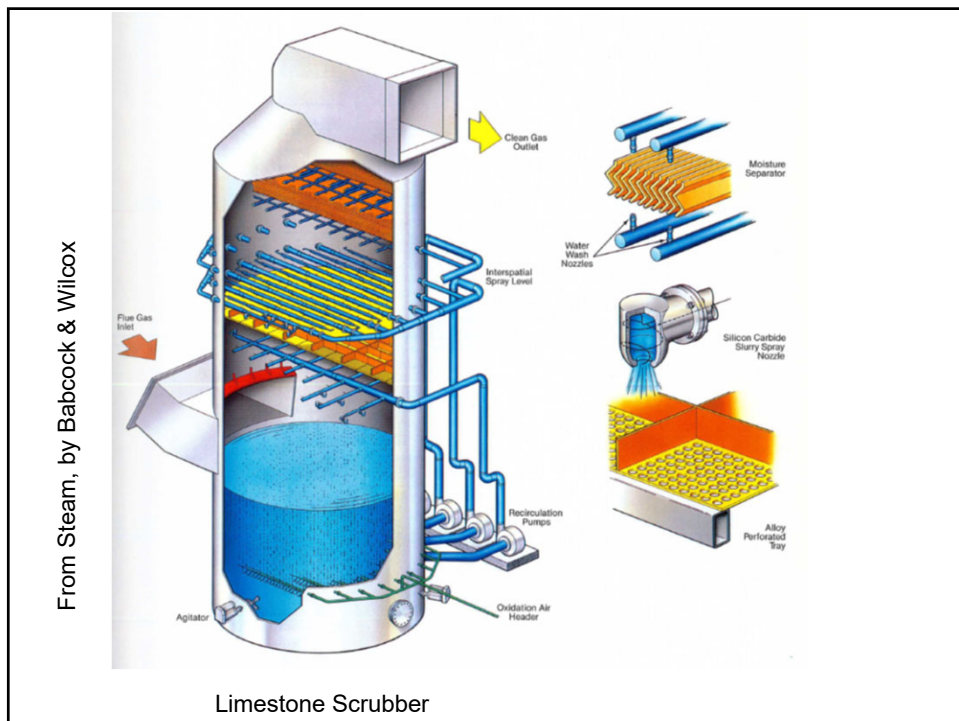
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3. Figures of Equipment

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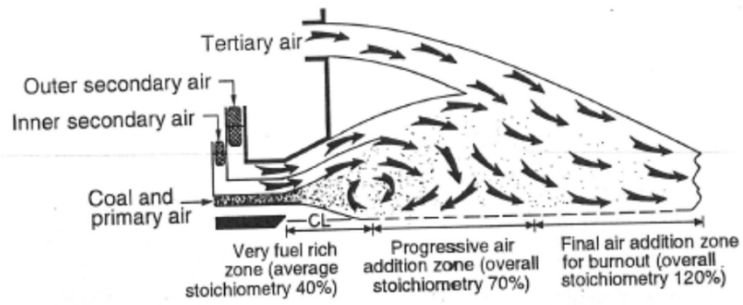


Fig. 1.12 Distributed mixing burner concept (published with permission from ref. 36).

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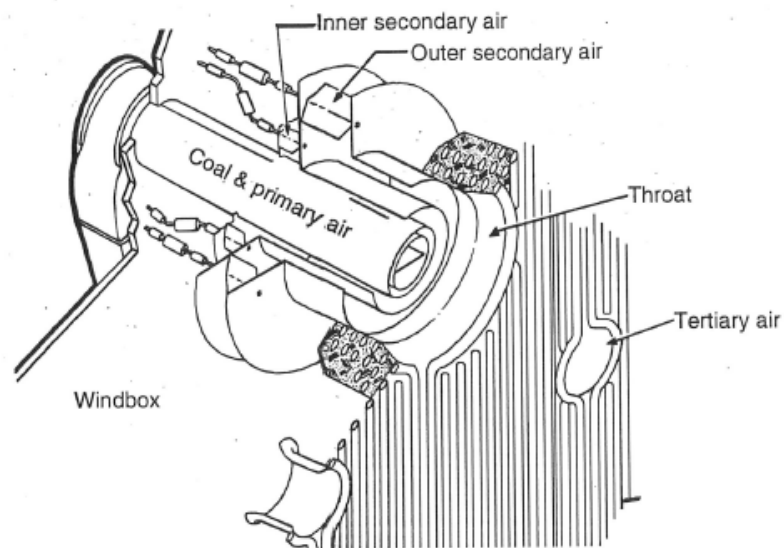
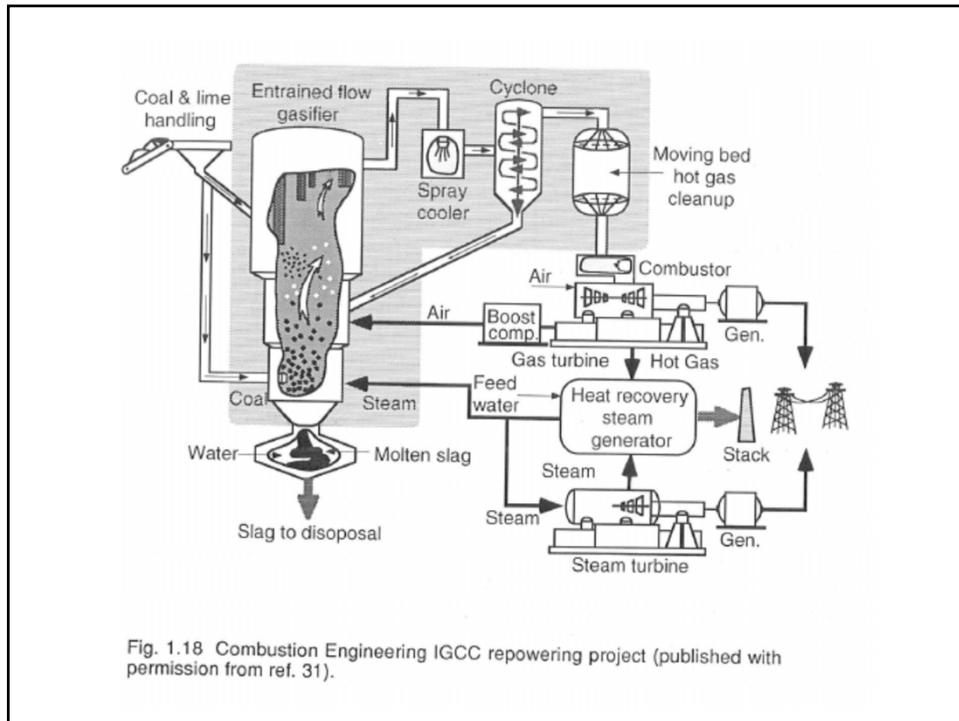
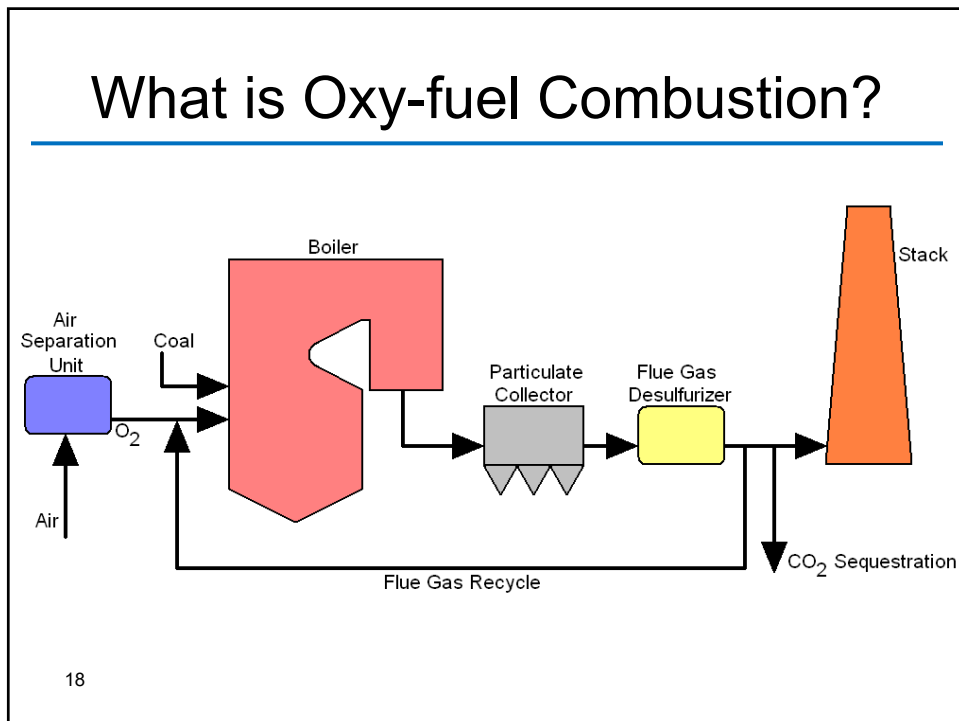


Fig. 1.13 Distributed mixing burner (published with permission from ref. 36).

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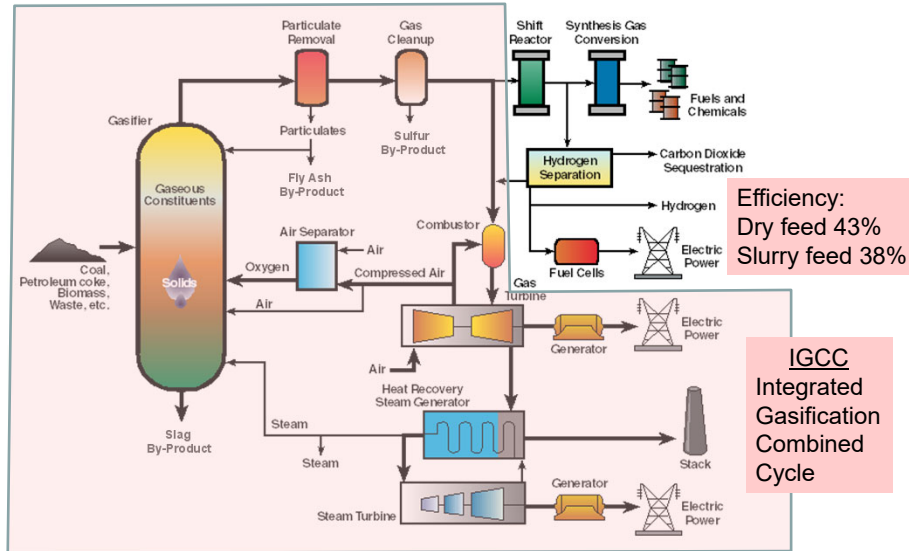


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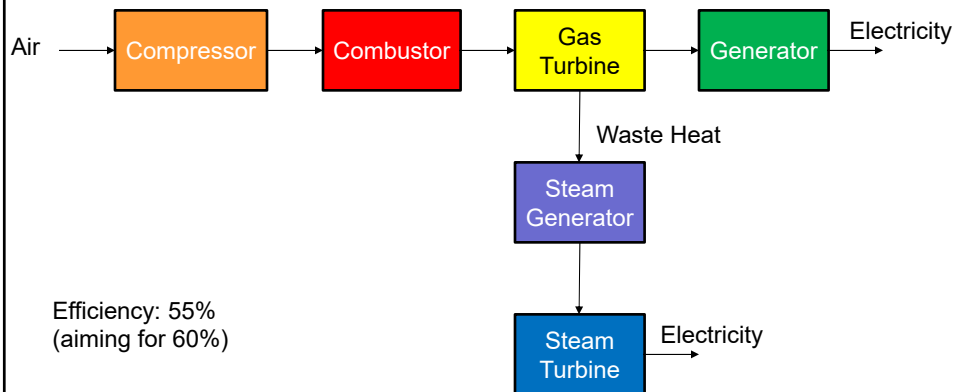
Gasification-Based Energy Production System Concepts



From a presentation by Gary Stiegel, DOE NETL, at the 2006 ACERC Conference

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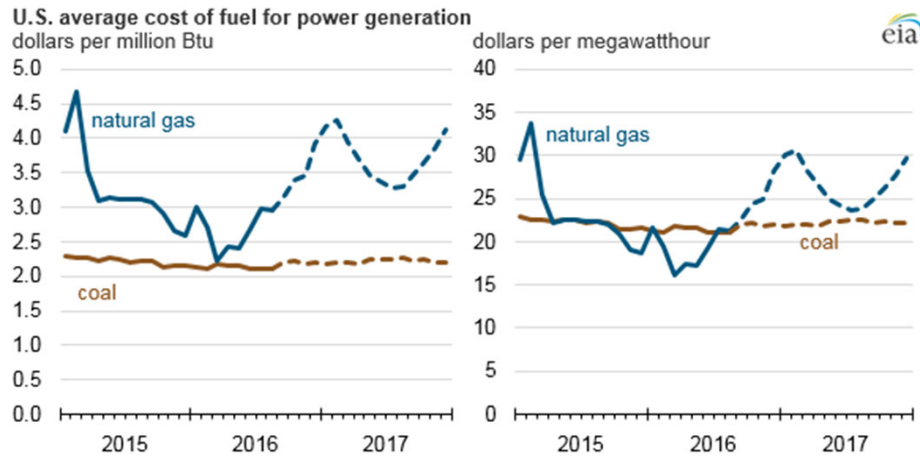
Natural Gas Combined Cycle (NGCC)



Efficiency: 55%
(aiming for 60%)

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Relative Costs



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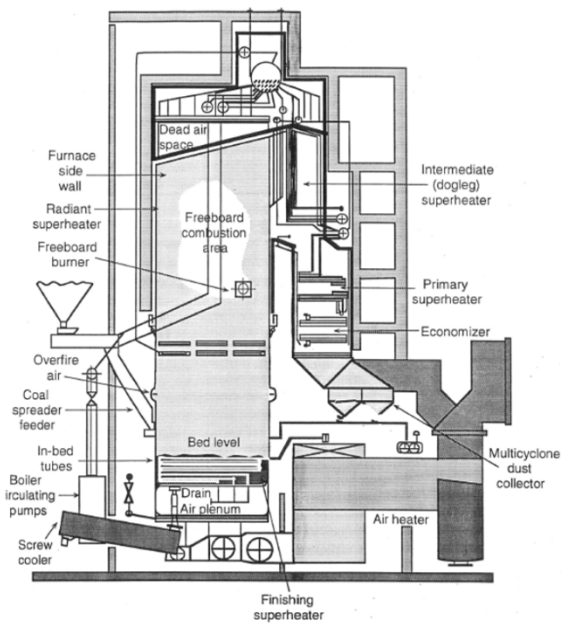
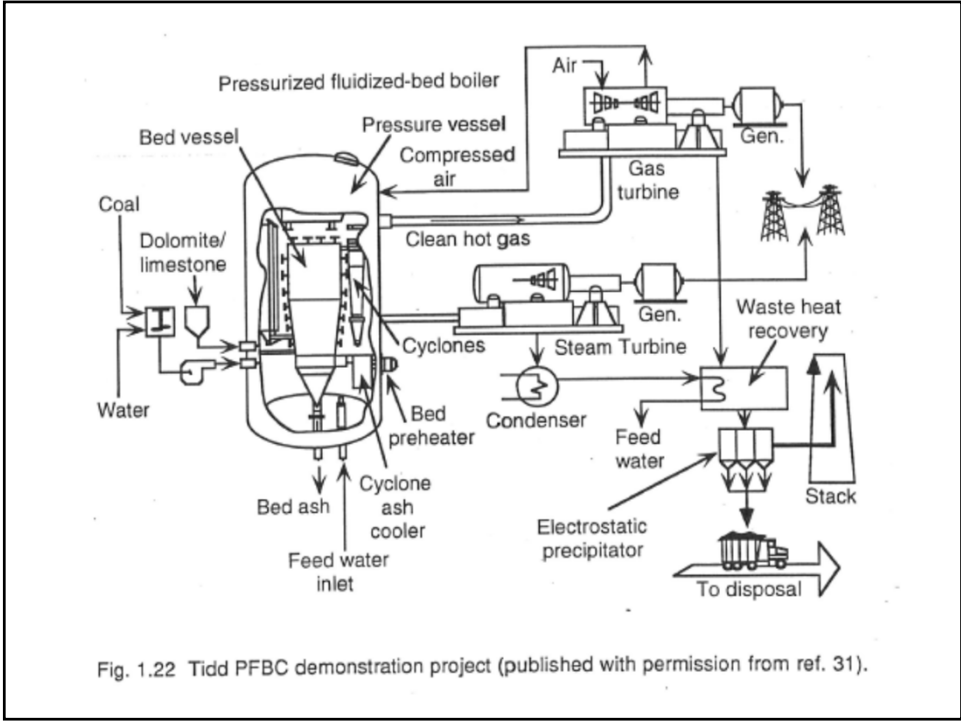
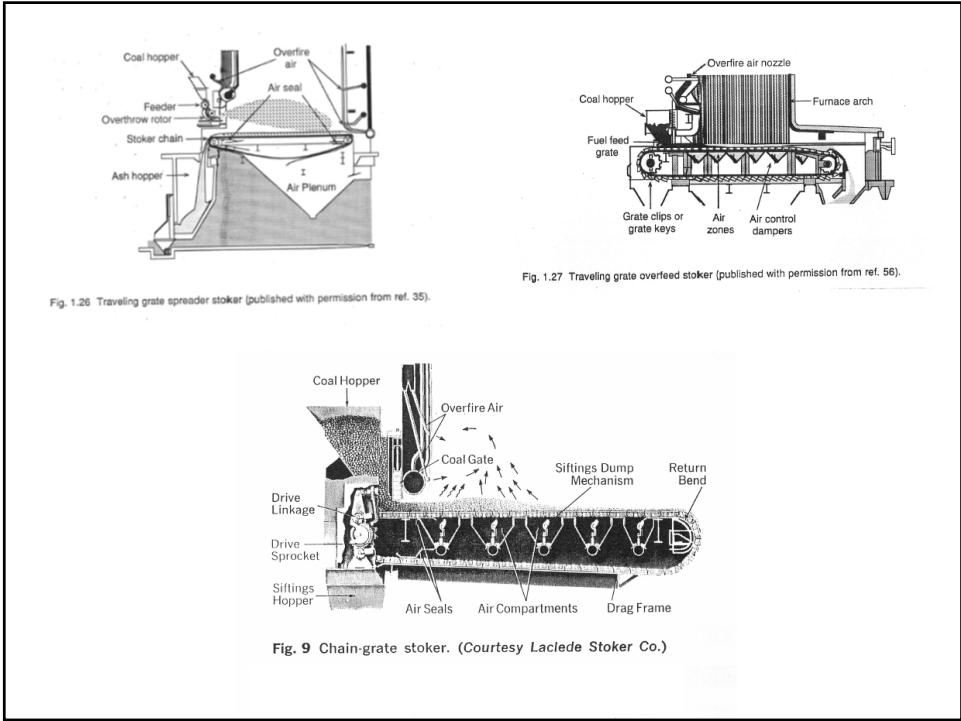


Fig. 1.20 Black Dog bubbling AFBC boiler (published with permission from ref. 50).

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Pulverizers

Medium Coal Feed Rate
(1.5 to 20 tons/hr)

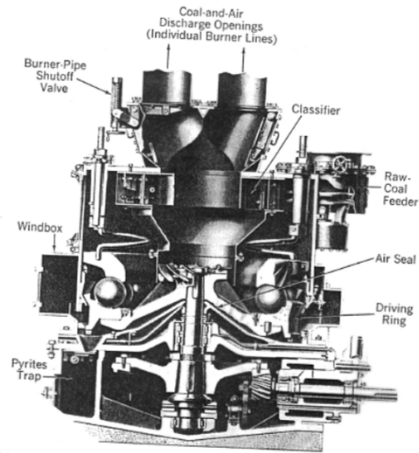


Fig. 7 B&W Type EL single-row ball-and-race pulverizer.

High Coal Feed Rate
(20 to 105 tons/hr)

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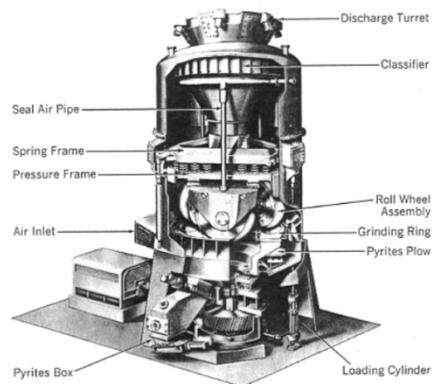
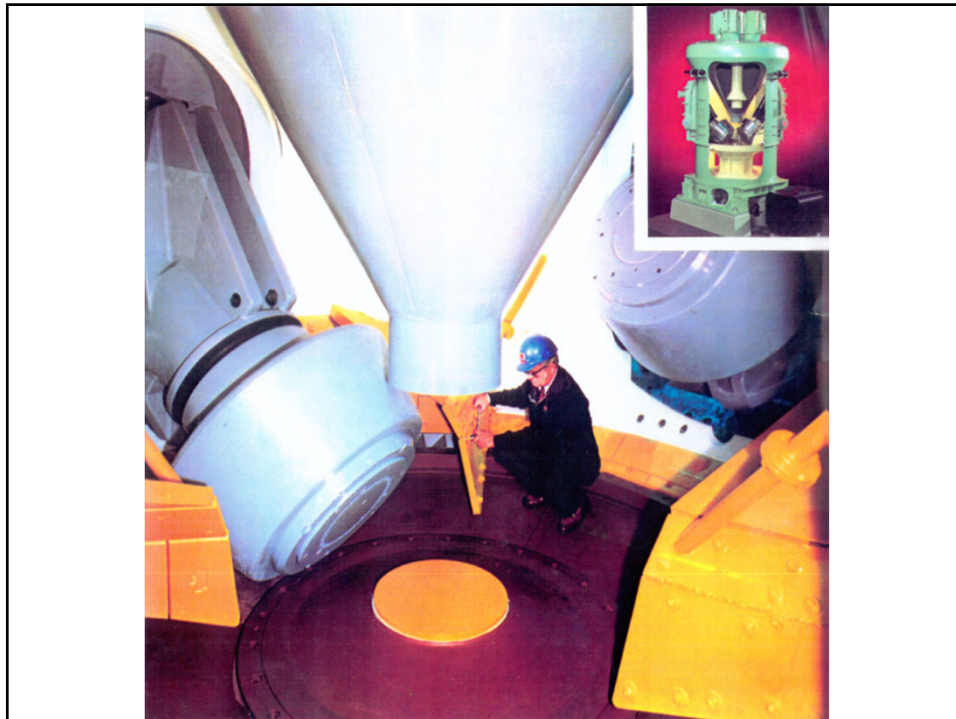
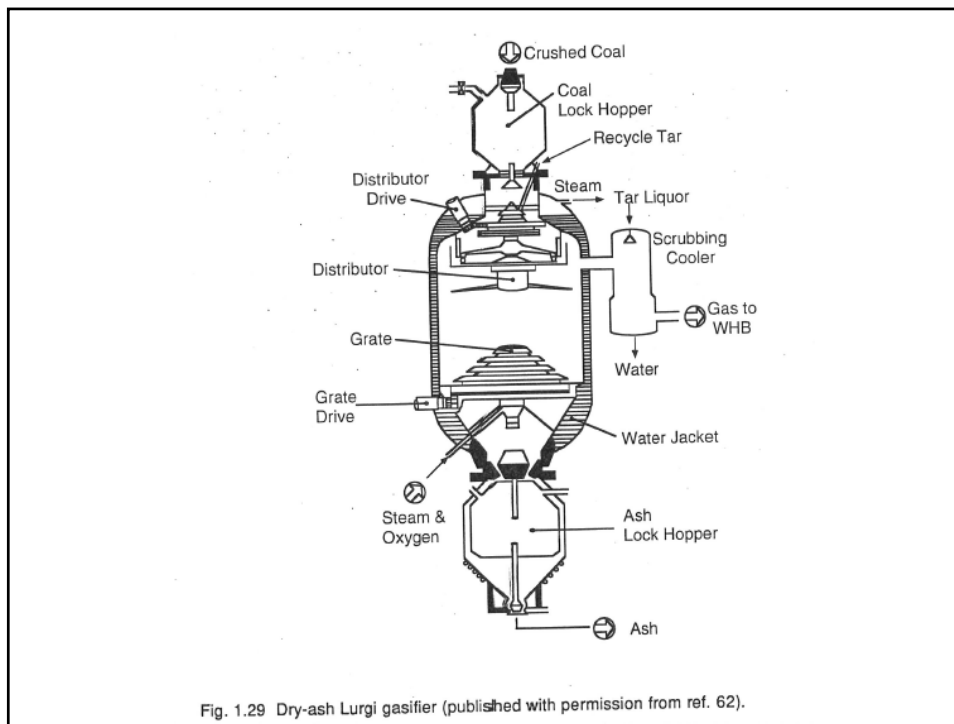


Fig. 8 Babcock & Wilcox Type MPS mill.

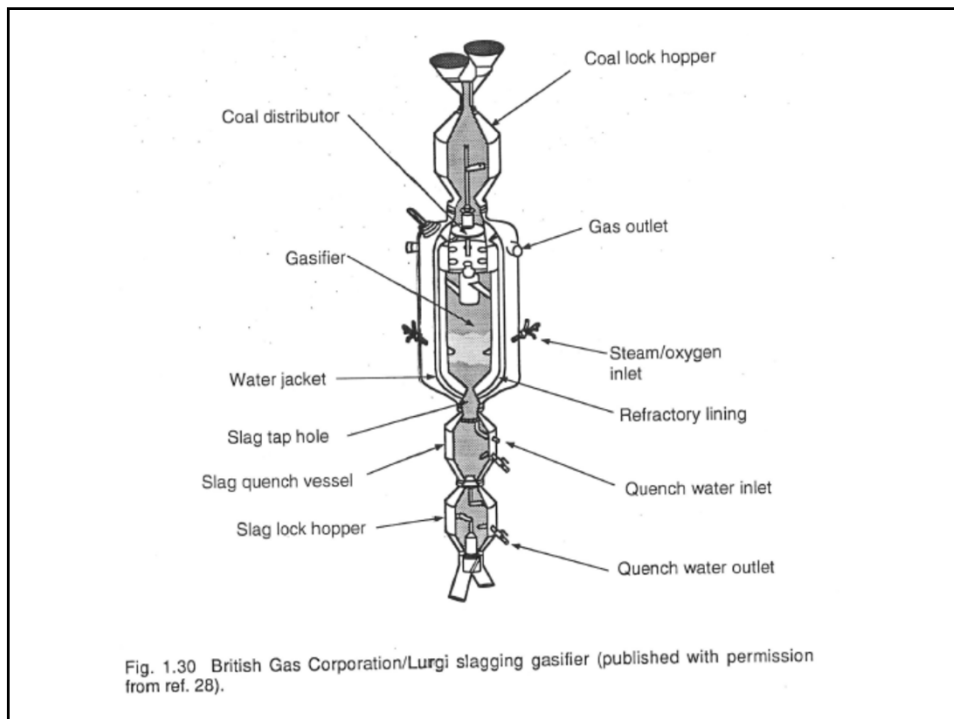
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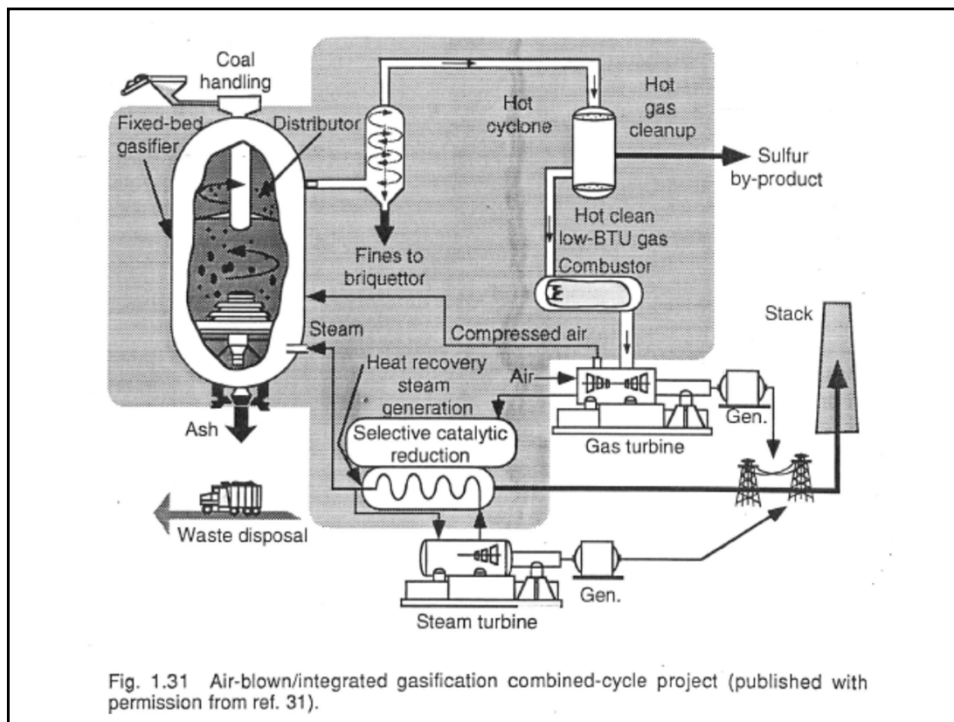
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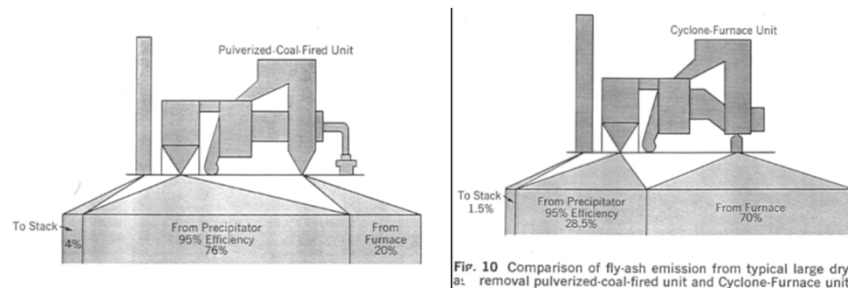


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4. Where Does The Ash Go?



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5. Co-firing Biomass

- Lower fuel costs
- More CO₂ friendly
- Changes deposit properties
 - Perhaps vaporization of Na, K, HCl
- Size of biomass?
- Supply of biomass
- Ash disposal regulations
- Risk
- Separate biomass handling system
 - Spontaneous ignition of biomass pile
- Lower heating value of biomass
- Possible increase in PM

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Interesting Stuff

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Heat Transfer

Mineral matter in coal and the thermal performance of large boilers

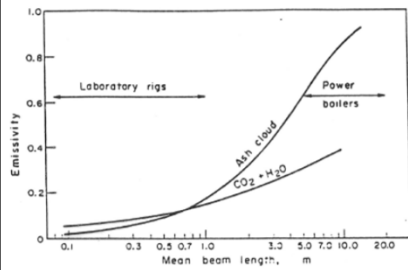


FIG. 3. Emissivity of p.f. combustion product components.

TABLE 11. Effect of ash absorption area on heat absorbed in furnace⁶⁰

Ash cloud absorption area (m ² /kg)	Mean particle absorption efficiency	Heat absorbed in furnace (MW)
58.4	0.7	362.5
41.7	0.5	338.9
10.4	0.125	271.8

from Wall et al., PECS, 5, 1-29 (1979)

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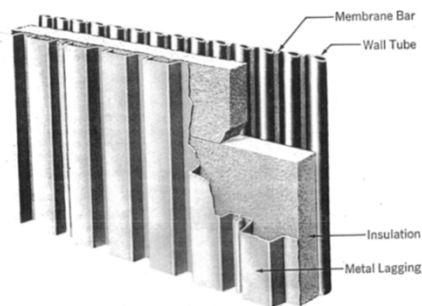


Fig. 2 Membrane wall construction.

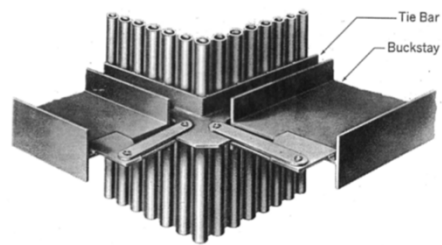


Fig. 6 Tie bar and buckstay arrangement at corner of furnace.

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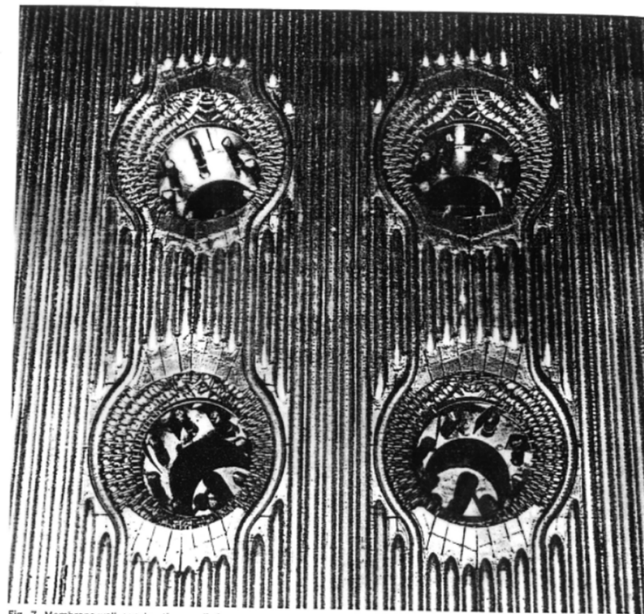
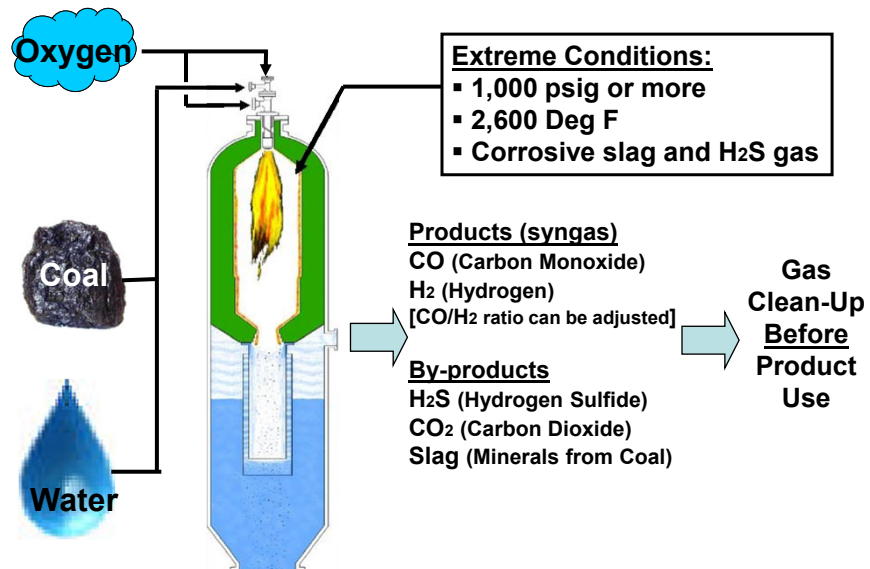


Fig. 7 Membrane-wall construction applied to a burner wall.

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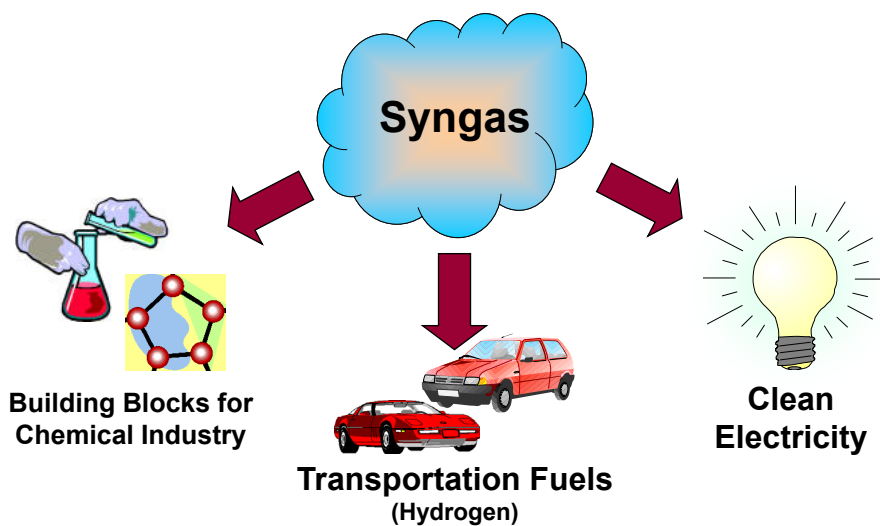
What is Gasification?



courtesy Gary Stiegel, DOE NETL, talk at ACERC conf. (2006)

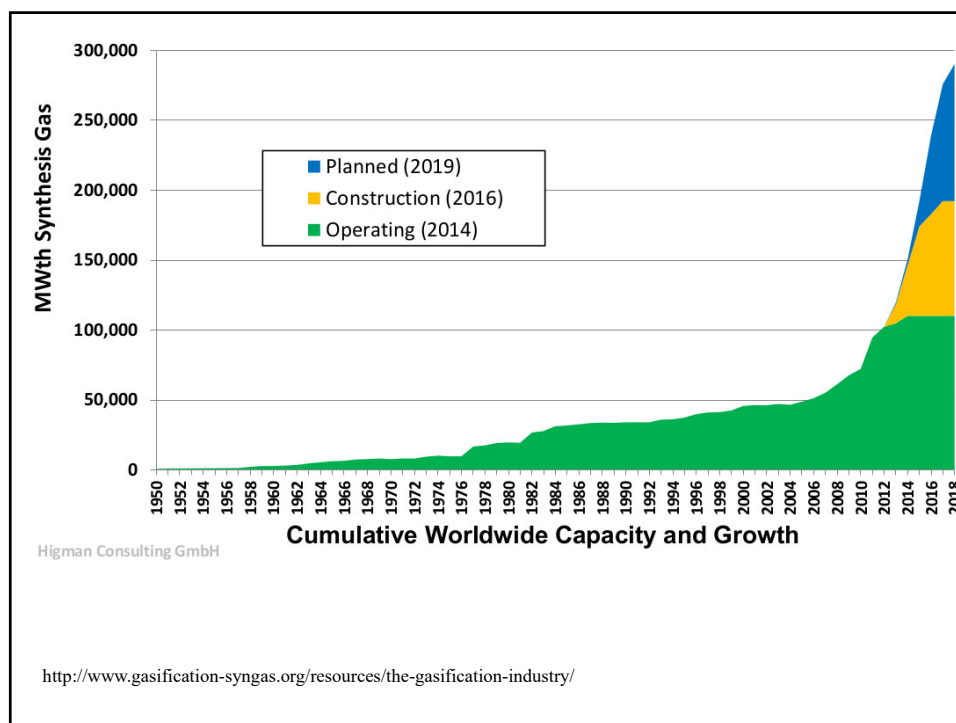
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So what can you do with CO and H₂ ?

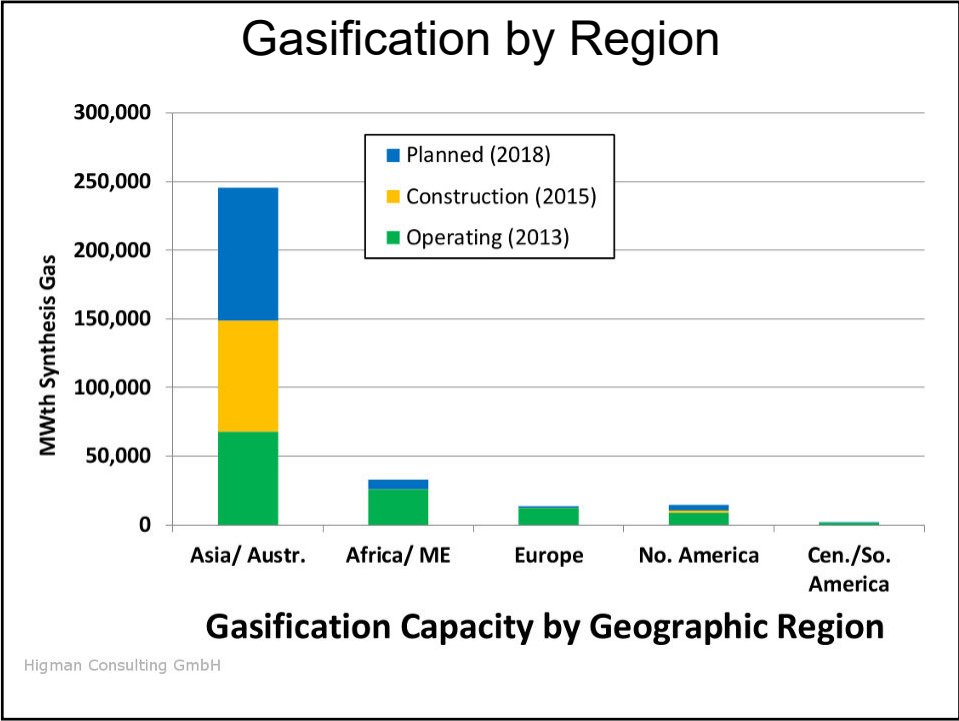


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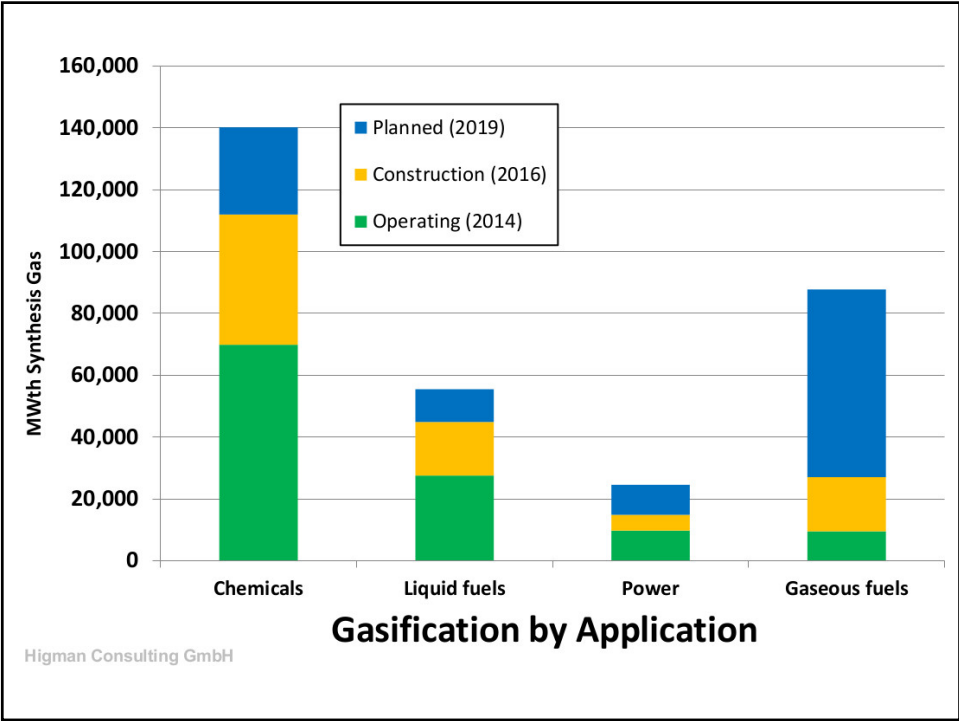
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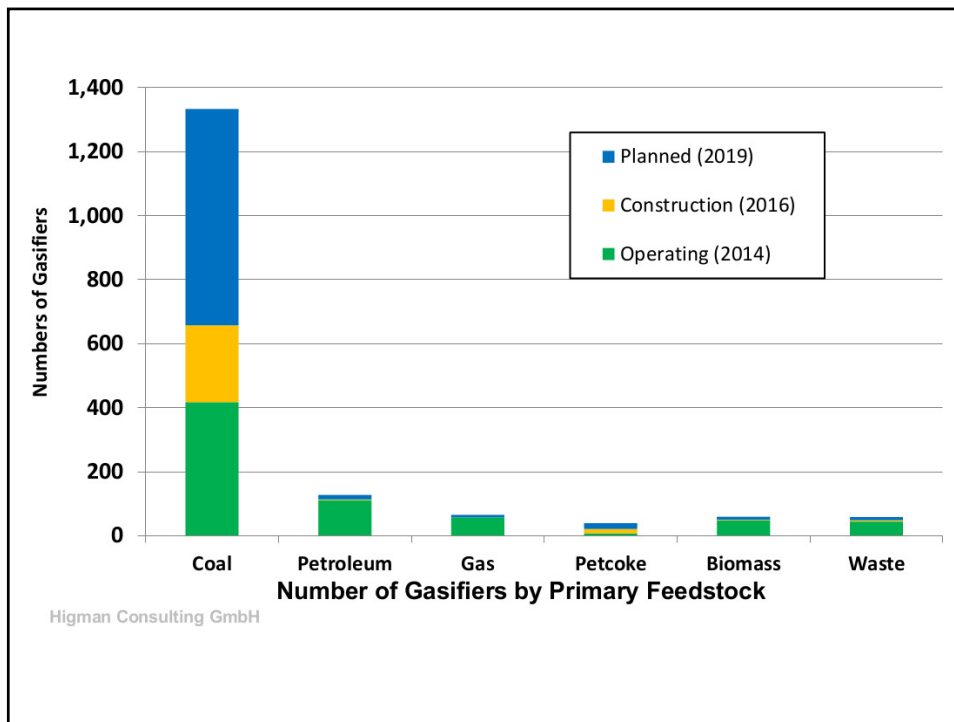
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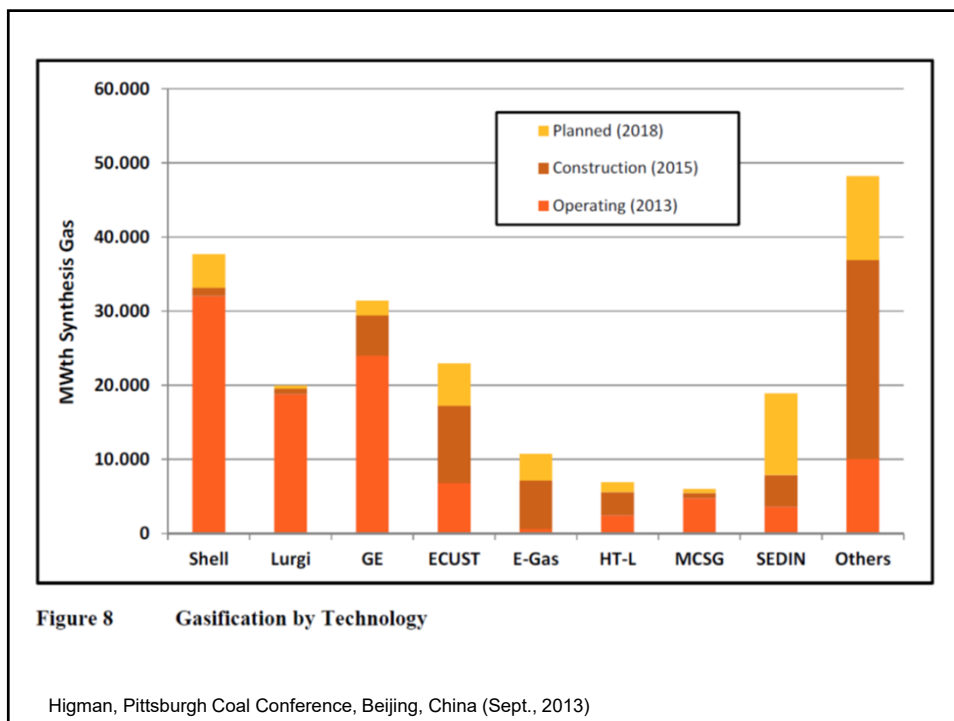
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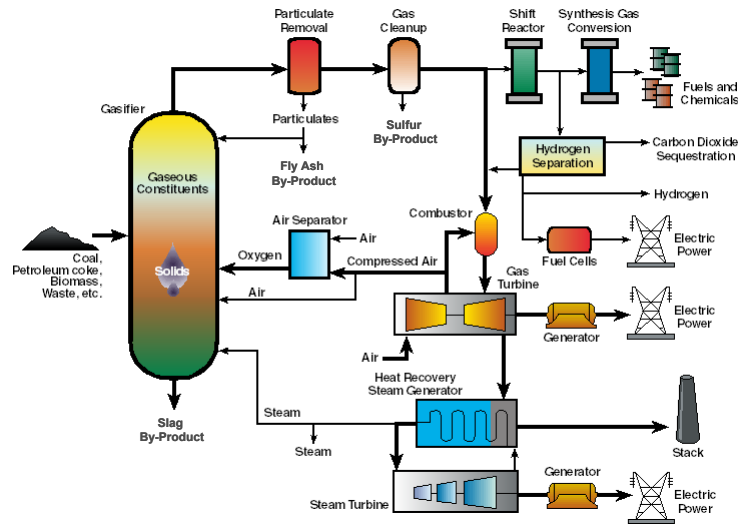


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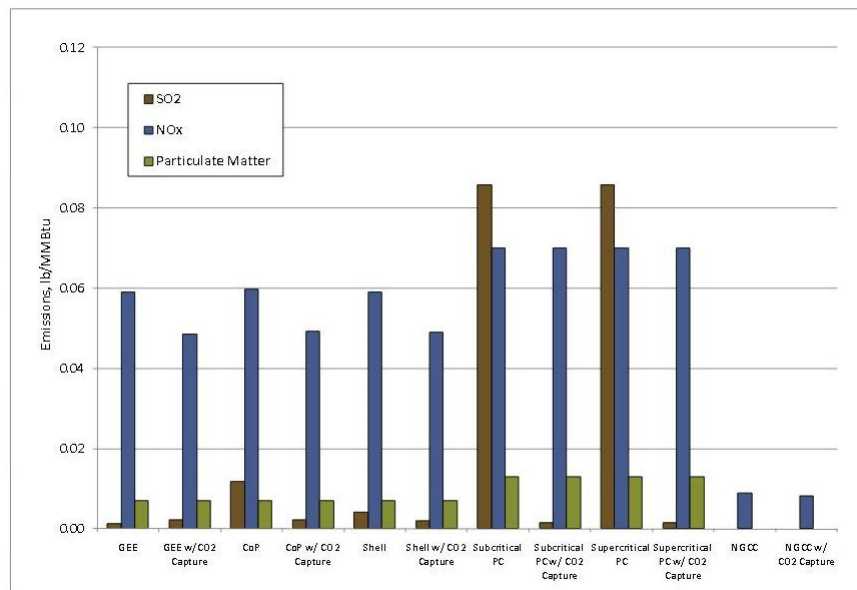
Gasification-Based Energy Production System Concepts



courtesy Gary Stiegel, talk at ACERC conf. (2006)

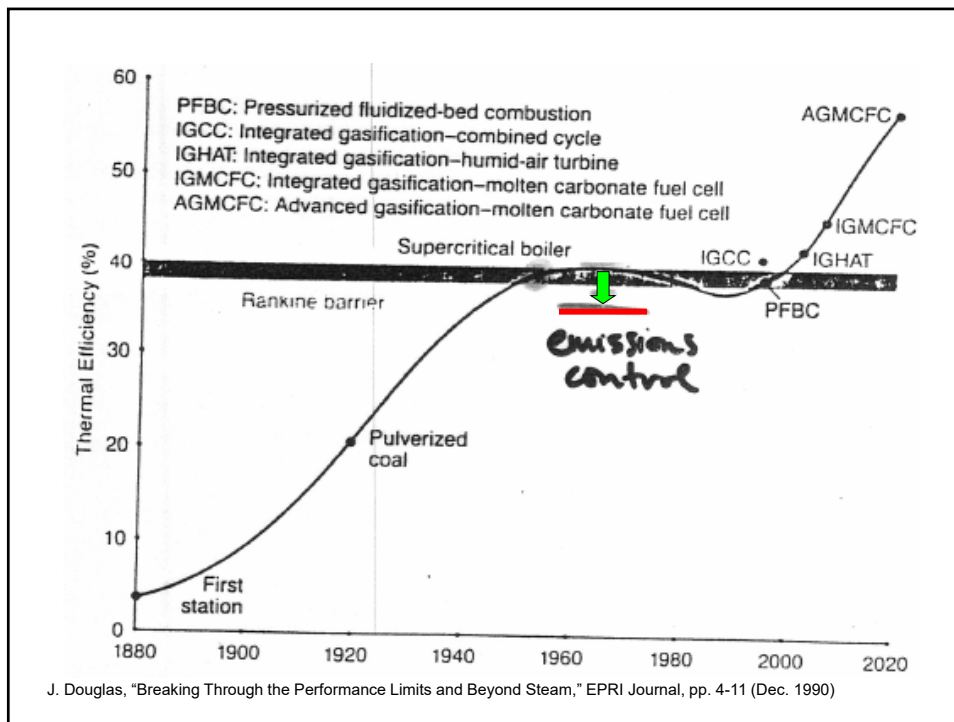
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Compare Emissions

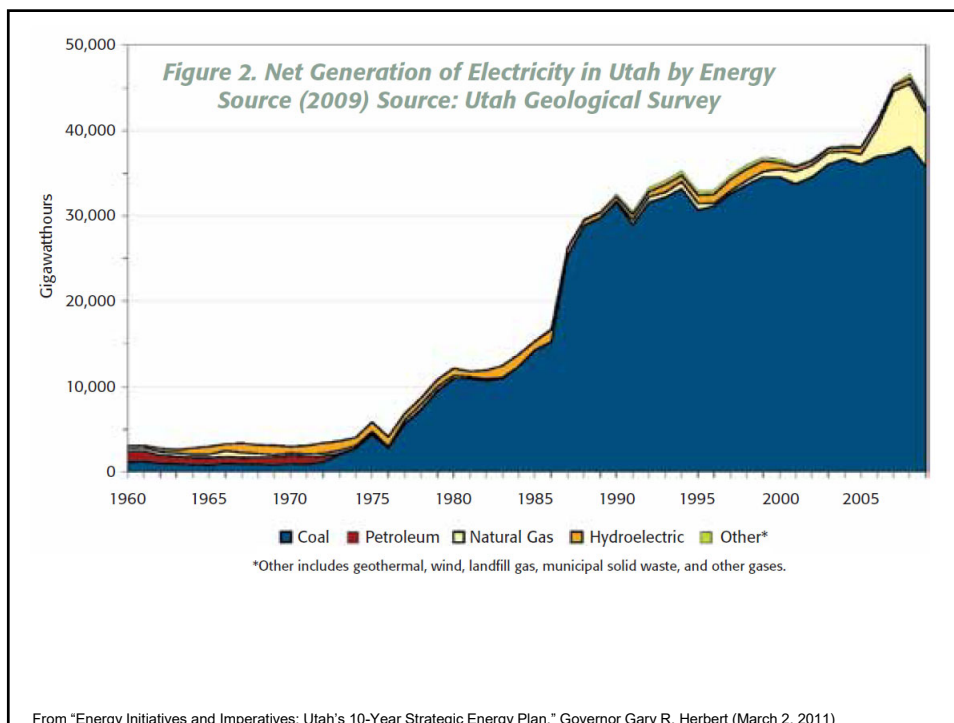


From Wikipedia

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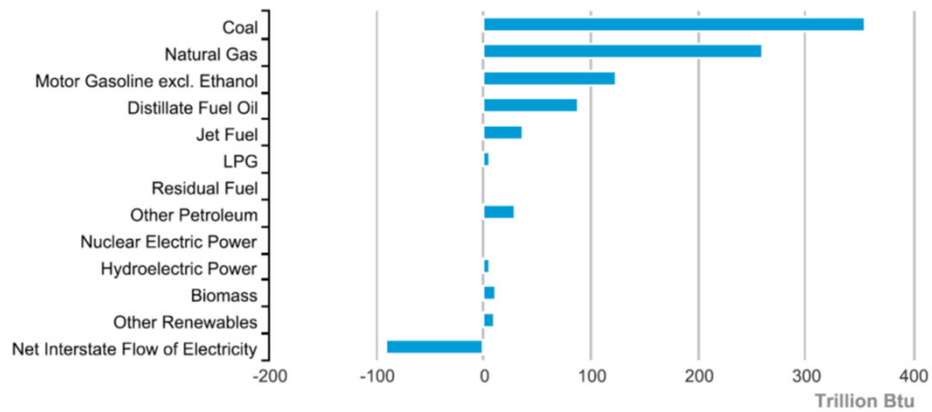


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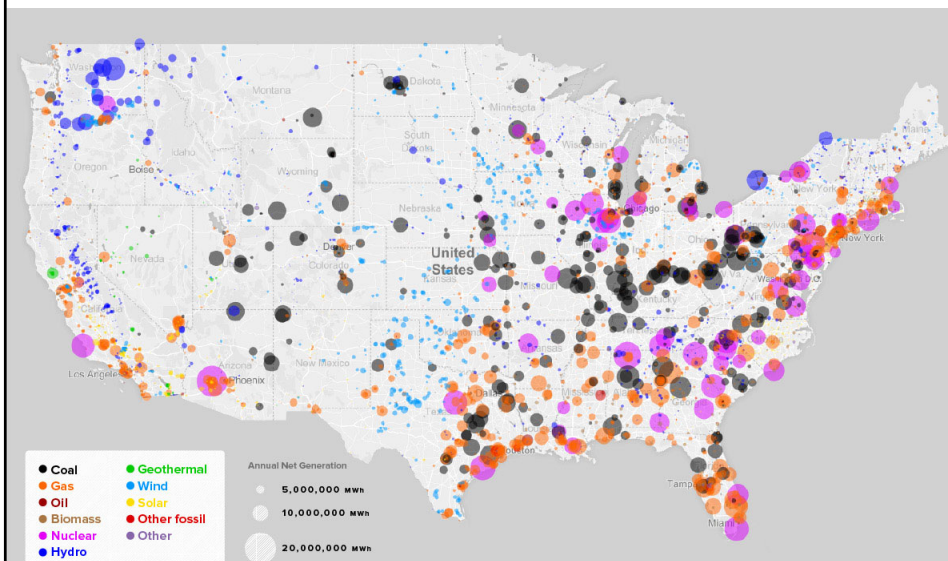
Utah Energy Consumption Estimates, 2013



eia Source: Energy Information Administration, State Energy Data System
<http://www.eia.gov/state/?sid=UT>

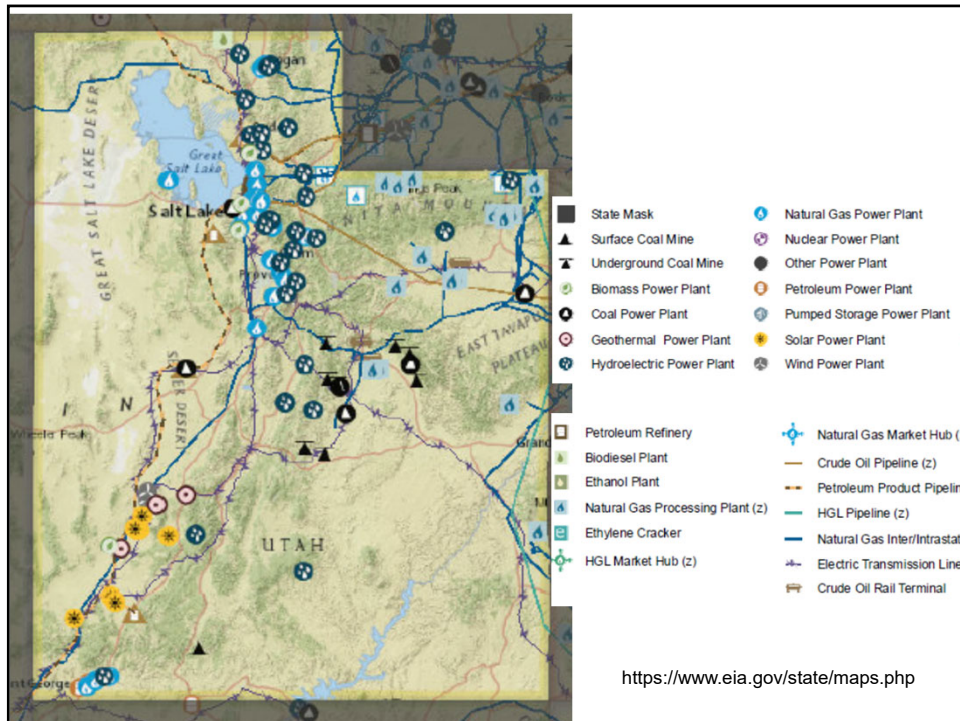
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U.S. Power Plants

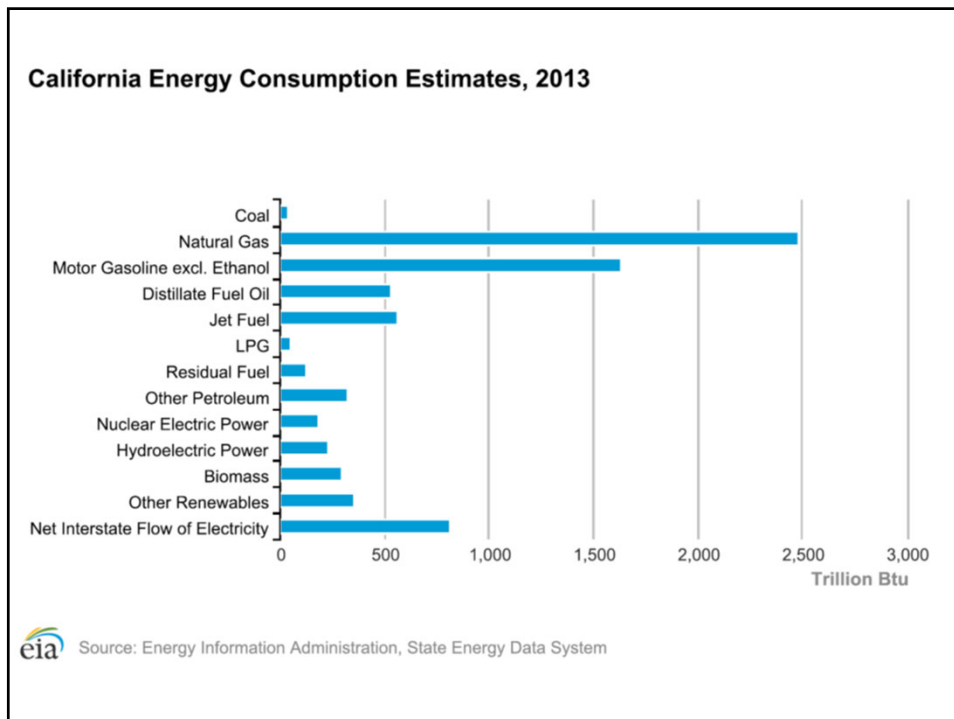


<https://www.visualcapitalist.com/mapped-every-power-plant-in-the-united-states/>

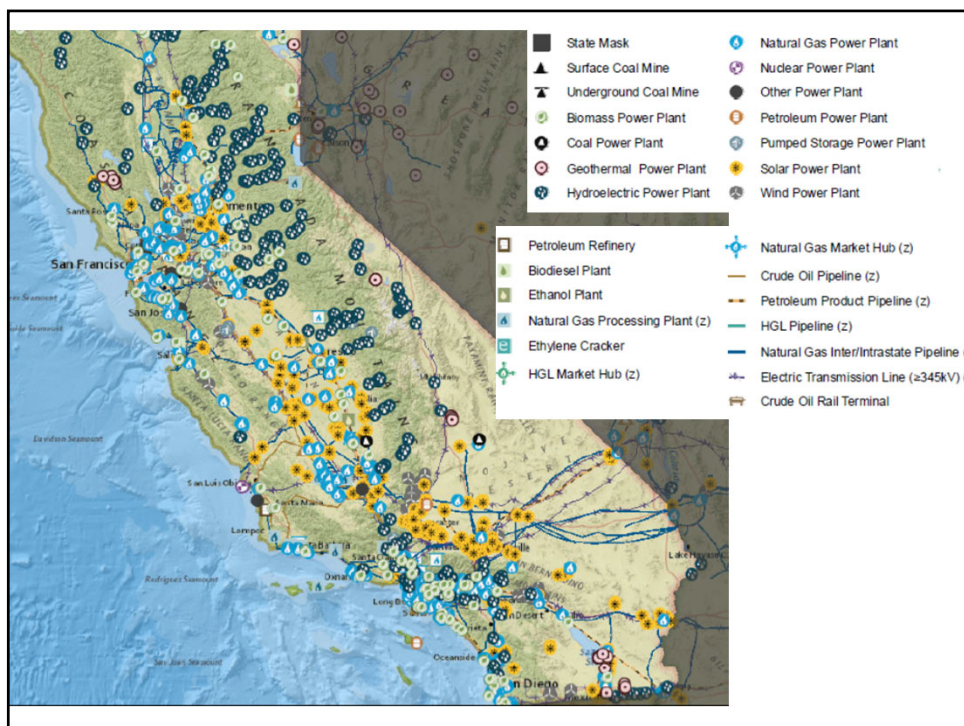
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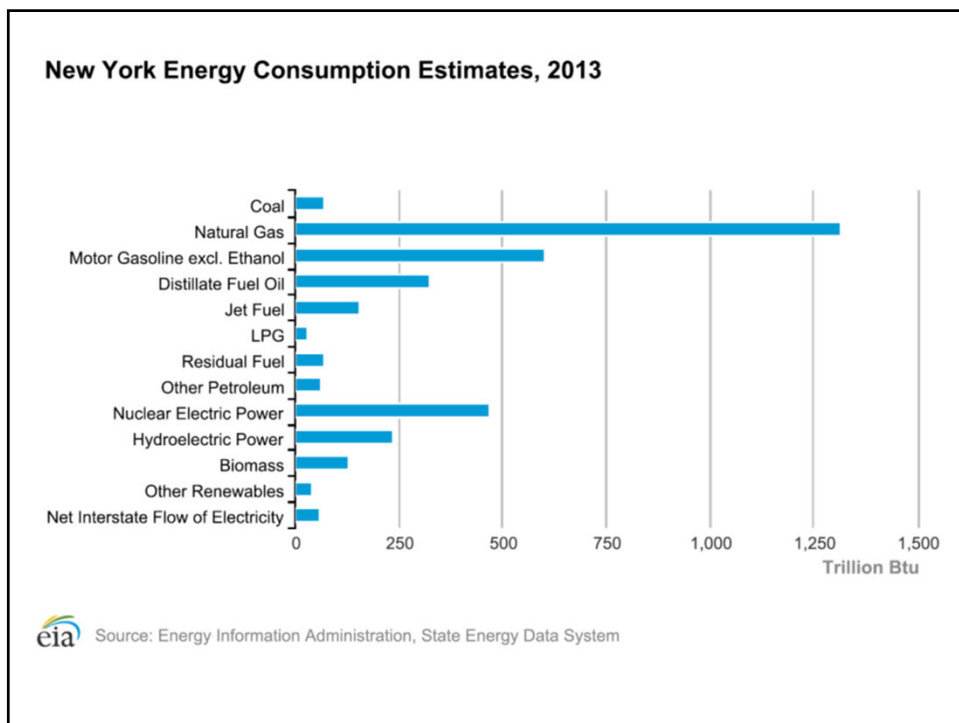
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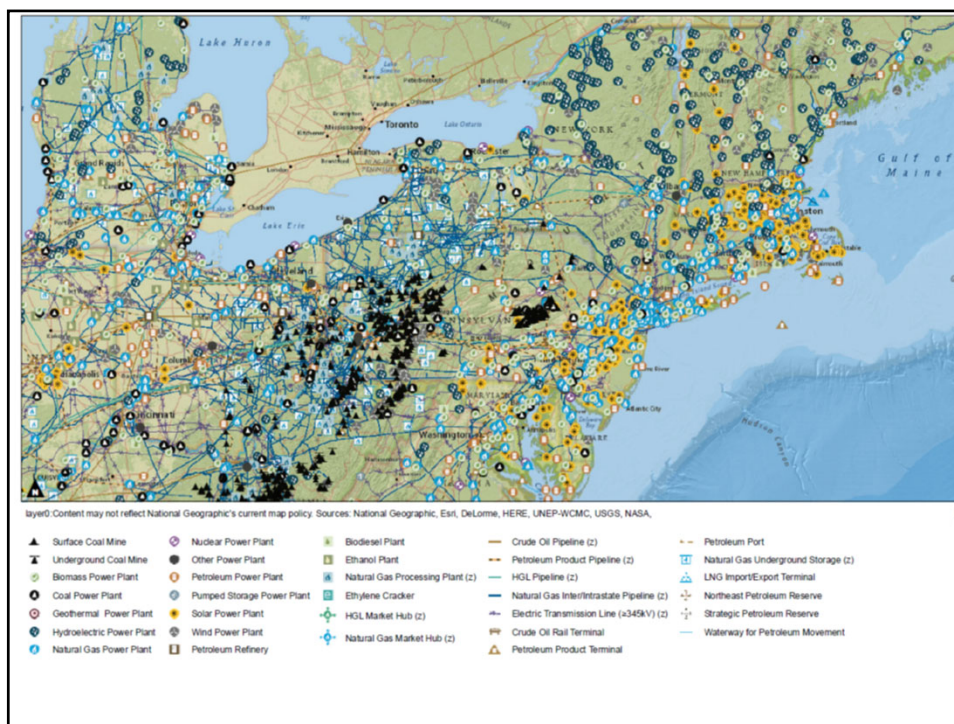
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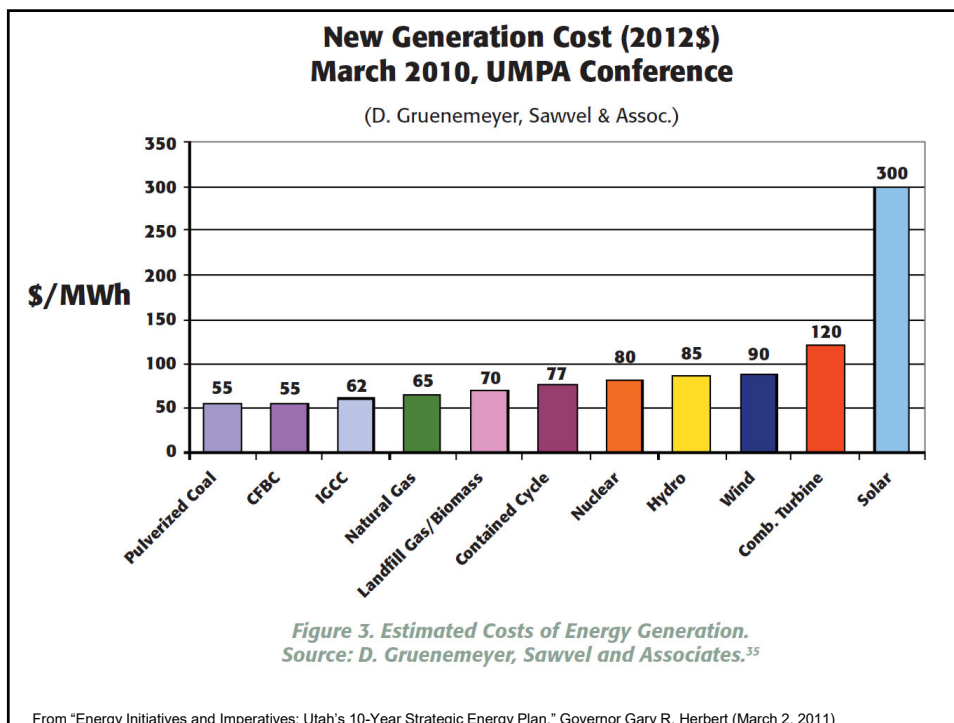
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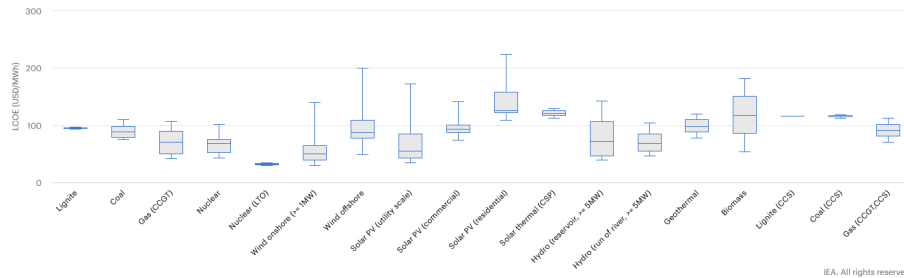


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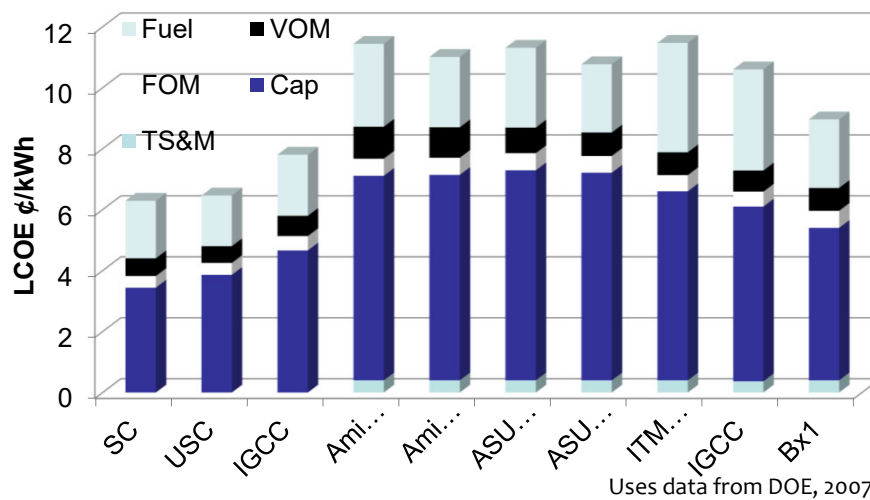
Levelized Cost of Electricity per MW-hr (IEA 2020)



<https://www.iea.org/reports/projected-costs-of-generating-electricity-2020>

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Levelized Cost of Power (with carbon capture and sequestration)



Uses data from DOE, 2007

Cases are supercritical (current, modern technology), ultrasupercritical (10 year out developing technology), integrated gasification combined cycle, and these technologies with amine-based absorption, cryogenic air-separation unit (ASU), ion transport membrane (ITM), and two new processes. Categories are fuel, variable operating & maintenance, fixed operating & maintenance, capital, and transportation, storage & monitoring.

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