Practical Combustion

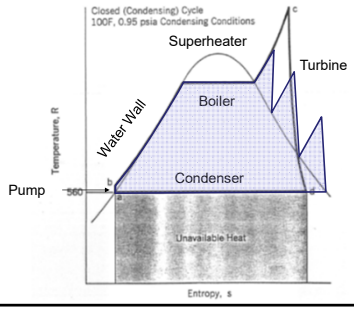
Class 15

1a. Comparison of Combustors

	Fixed Bed	Fluidized Bed	Entrained Flow
Particle Size	10-50 mm	1.5-6 mm	1-100 μm
Operating T (K)	< 2000	1000-1400	1900-2000
Residence Time (s)	500-50,000	10-500	1-2
Coal Feed Rate (kg/hr)	< 40,000 (BYU is at 5000)	< 40,000	< 450,000
Advantages	Simple Low grinding costs	Low SO_x & NO_x Low slagging Multi-fuel Low corrosion	High efficiency High capacity
Disadvantages	Emissions, especially particulates Efficiency Low capacity	Feeding fuel Softening coal Low capacity Risk (not established)	High NO_x Fly ash capture Grinding costs

Modified from Table 5.2 in Smoot & Smith, 1985

Rankine Cycles



Types of Boilers

- Subcritical (38% efficiency, new)
  - 2400 psi (steam pressure)
  - T_{steam} = 1000°F
- Supercritical (42% efficiency, new)
  - 3500 psi
  - T_{steam} = 1000°F
- Ultrasupercritical (44% efficiency, new)
  - 4400 psi
  - 1150°F

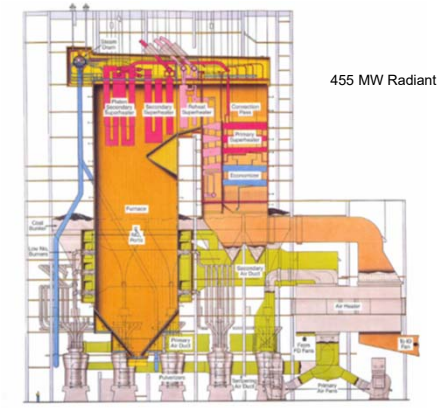
Gasifiers

- Pretty much the same story as combustors
- Challenges:
  - Getting heat to where gasification happens
  - Slagging
  - Air separation unit required?
- Pressure?
  - Reduces size of gasifier
  - Adds complexity
    - Feeding
    - Disposing of ash
    - Lower volatiles

1b. Comparison of Gasifiers

	Fixed Bed	Fluidized Bed	Entrained Flow
Particle Size	6-50 mm	0.5-2.5 mm	10-150 μm
Operating T (K)	1150-1300	600-1470	1150-2500
Residence Time (s)	1-3 hrs	20-150 min	0.4-12 s
Pressure (atm)	0.1-2	1-100	1-300
O_2/Coal ratio (mass)	0.14-0.81	0.25-0.97	0.28-1.17
CO+H_2 (mol%)	39-66	2-80	35-91
CH_4 (mol%)	2-15	3-68	0.1-17
High Heating Value (Btu/SCF)	250-320	300-800	115-550
Advantages	Established technology (Lurgi) Low thermal losses High turndown ratio	Multi-fuel, multi-size Moderate heat losses	Small, simple design High capacity per volume
Disadvantages	Low capacity	Softening coal Low capacity Risk (not established)	Down time due to wear of refractory and injectors

Modified from Table 6.1 in Smoot & Smith, 1985



455 MW Radiant Boiler

From Steam, by Babcock & Wilcox

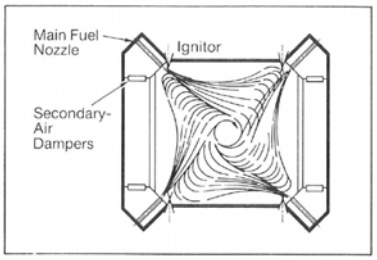


Fig. 3. Tangential firing pattern

From Combustion: Fossil Power Systems, by Combustion Engineering

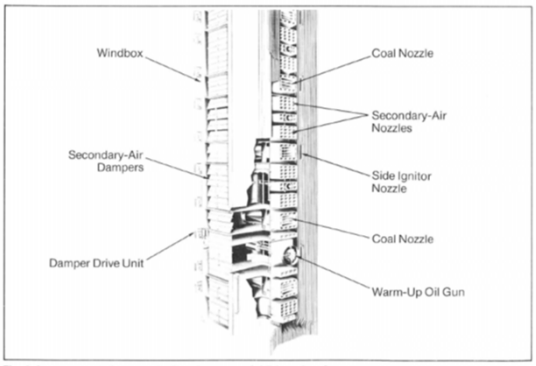


Fig. 4 Arrangement of corner windbox for tangential firing of coal

From Combustion: Fossil Power Systems, by Combustion Engineering

2. Wall-Fired vs. Tangential

Tangential

- Lower NO_x due to large swirl zone
- More difficult to tune

Wall-Fired

- Less complex
- Easier to tune individual burners

3. Figures of Equipment

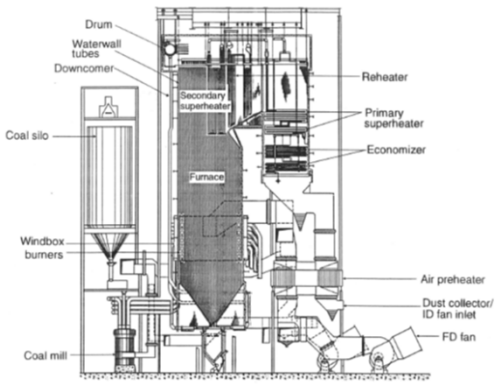
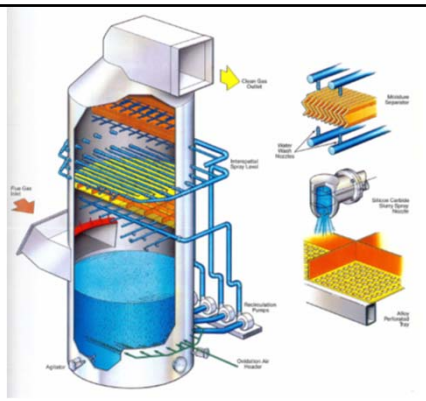


Fig. 1.10 Tangentially fired boiler (published with permission from ref. 36).

From Steam, by Babcock & Wilcox



Limestone Scrubber

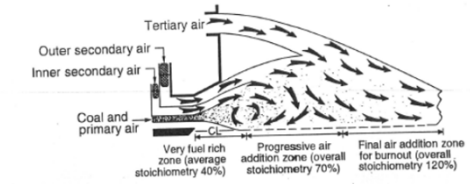


Fig. 1.12 istributed mixing burner concept (published with permission from ref. 36).

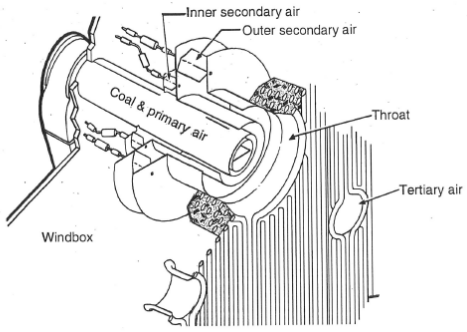


Fig. 1.13 Distributed mixing burner (published with permission from ref. 36).

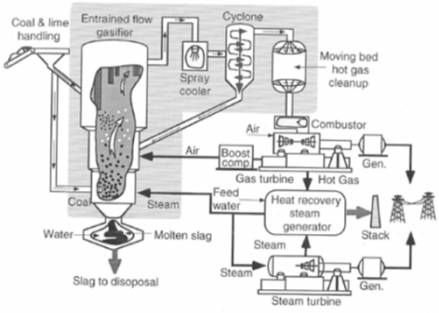
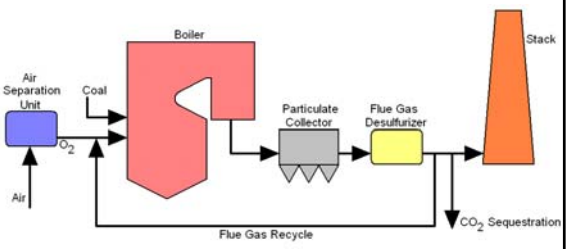


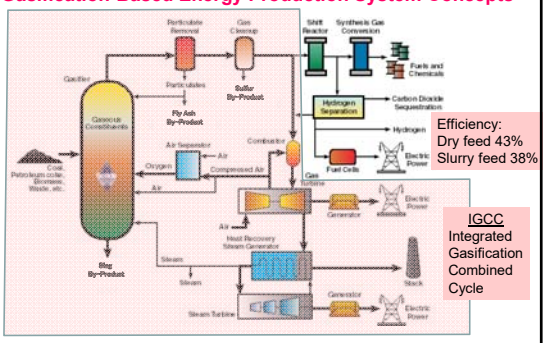
Fig. 1.18 Combustion Engineering IGCC repowering project (published with permission from ref. 31).

What is Oxy-fuel Combustion?



17

Gasification-Based Energy Production System Concepts

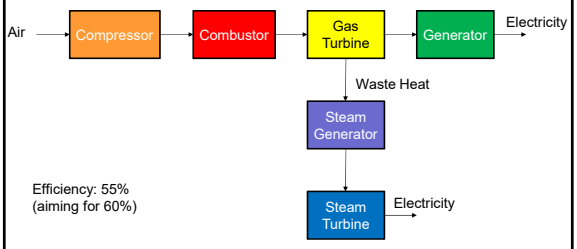


Efficiency:
Dry feed 43%
Slurry feed 38%

IGCC
Integrated Gasification Combined Cycle

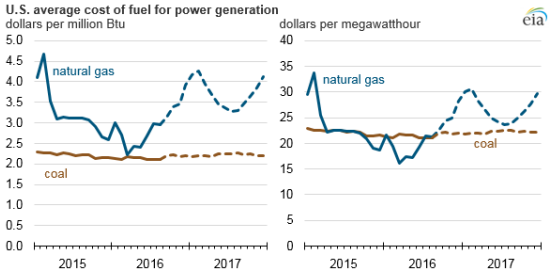
From a presentation by Gary Stiegel, DOE NETL, at the 2006 ACERC Conference

Natural Gas Combined Cycle
(NGCC)



Efficiency: 55%
(aiming for 60%)

Relative Costs



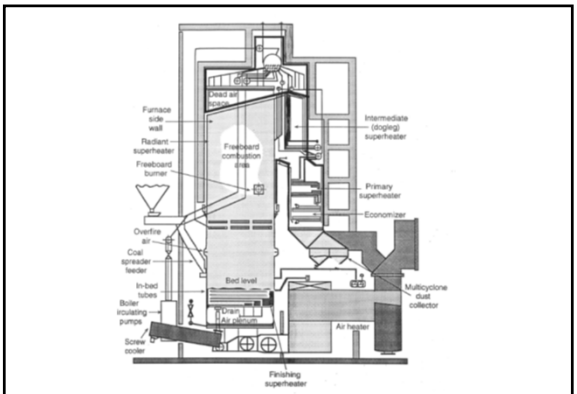


Fig. 1.20 Black Dog bubbling AFBC boiler (published with permission from ref. 50).

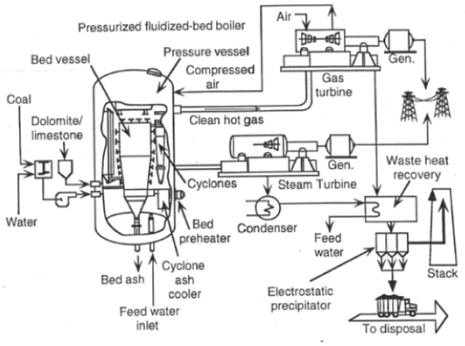


Fig. 1.22 Tidd PFBC demonstration project (published with permission from ref. 31).

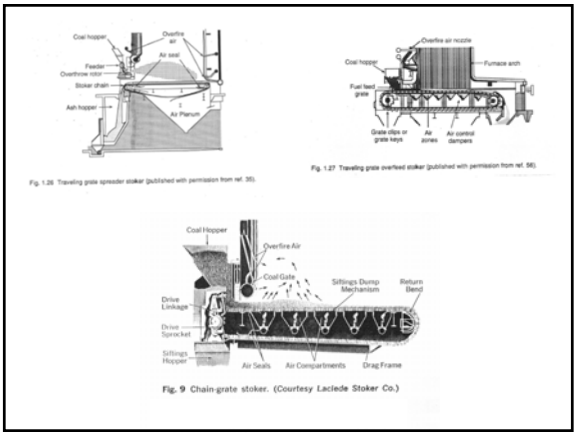


Fig. 9 Chain-grate stoker. (Courtesy Laclede Stoker Co.)

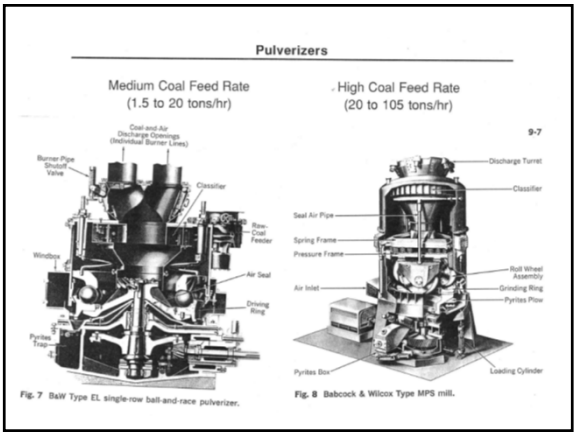


Fig. 7 B&W Type EL single-row ball-and-race pulverizer.

Fig. 8 Babcock & Wilcox Type MPS mill.

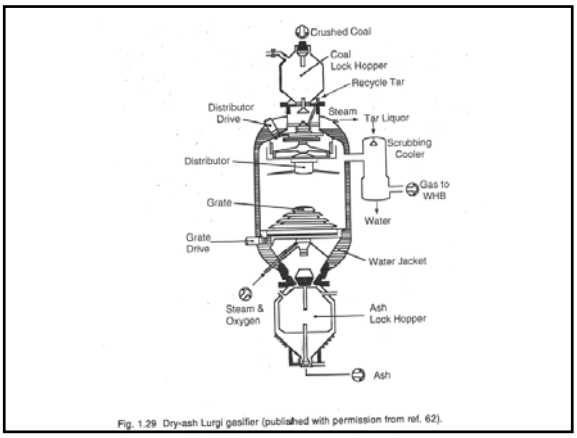


Fig. 1.29 Dry-ash Lurgi gasifier (published with permission from ref. 62).

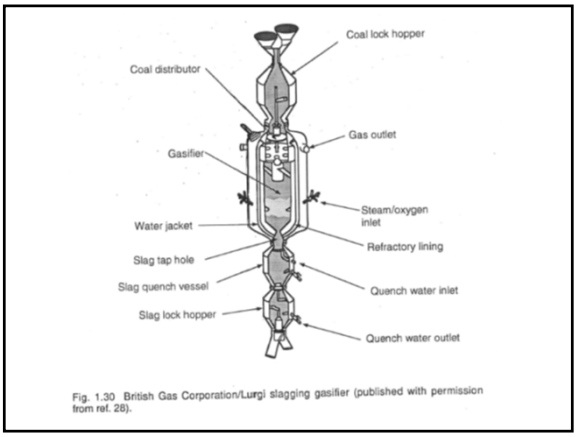


Fig. 1.30 British Gas Corporation/Lurgi slagging gasifier (published with permission from ref. 28).

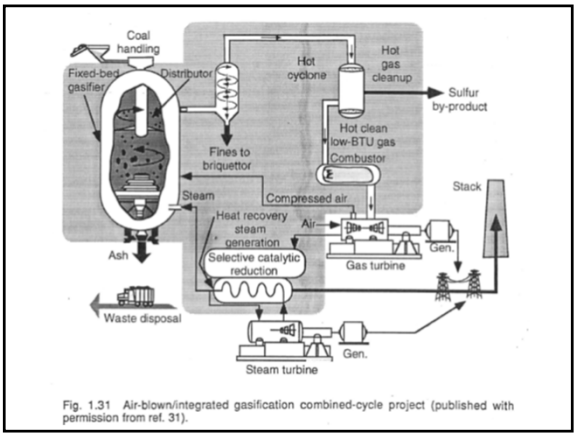


Fig. 1.31 Air-blown/integrated gasification combined-cycle project (published with permission from ref. 31).

4. Where Does The Ash Go?

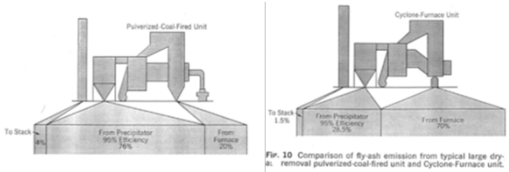


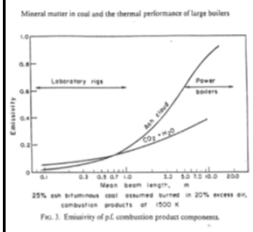
Fig. 10 Comparison of fly-ash emission from typical large dry-a removal pulverized-coal-fired unit and Cyclone-Furnace unit.

5. Co-firing Biomass

- Lower fuel costs
- More CO_2 friendly
- Changes deposit properties
  - Perhaps vaporization of Na, K, HCl
- Size of biomass?
- Supply of biomass
- Ash disposal regulations
- Risk
- Separate biomass handling system
  - Spontaneous ignition of biomass pile
- Lower heating value of biomass
- Possible increase in PM

Interesting Stuff

Heat Transfer



Mineral matter in coal and the thermal performance of large boilers

Fig. 3. Emissivity of p.f. combustion product components.

Table 11. Effect of ash absorption area on heat absorbed in furnace[a,b]

Ash cloud absorption area (m^2/kg)	Mean particle absorption efficiency	Heat absorbed in furnace (MW)
58.4	0.7	362.5
41.7	0.5	338.9
10.4	0.125	271.8

from Wall et al., PECS, 5, 1-29 (1979)

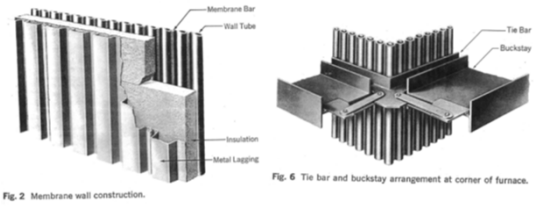


Fig. 2 Membrane wall construction.

Fig. 6 Tie bar and buckstay arrangement at corner of furnace.

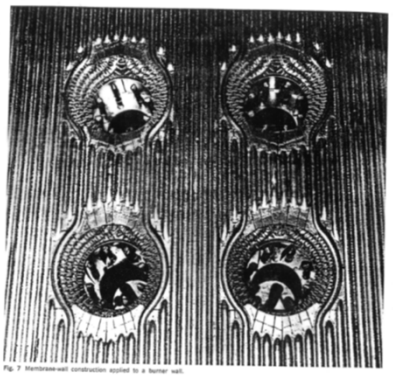
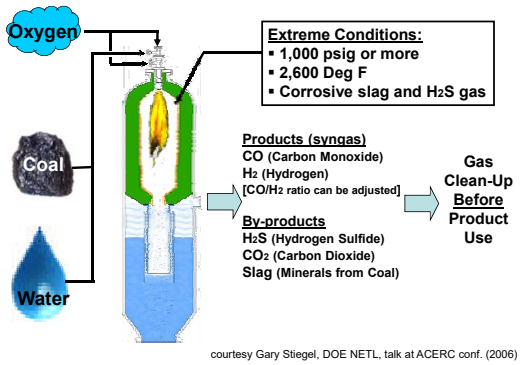


Fig. 7 Membrane-wall construction applied to a burner wall.

What is Gasification?



Extreme Conditions:
- 1,000 psig or more
- 2,600 Deg F
- Corrosive slag and H_2S gas

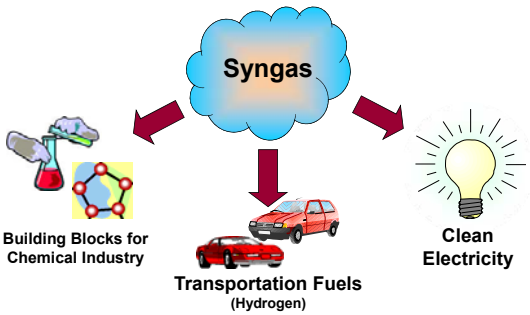
Products (syngas)
CO (Carbon Monoxide)
H_2 (Hydrogen)
[CO/H_2 ratio can be adjusted]

By-products
H_2S (Hydrogen Sulfide)
CO_2 (Carbon Dioxide)
Slag (Minerals from Coal)

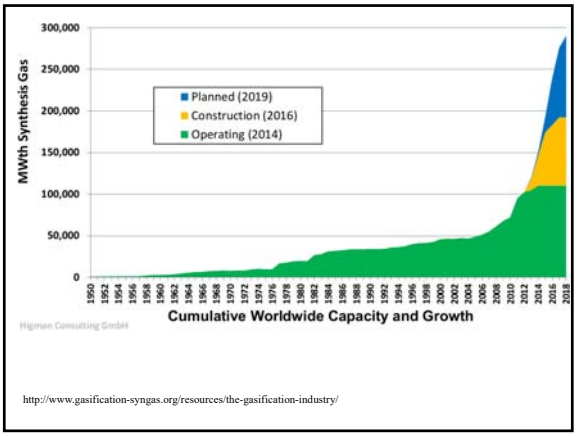
Gas Clean-Up Before Product Use

courtesy Gary Stiegel, DOE NETL, talk at ACERC conf. (2006)

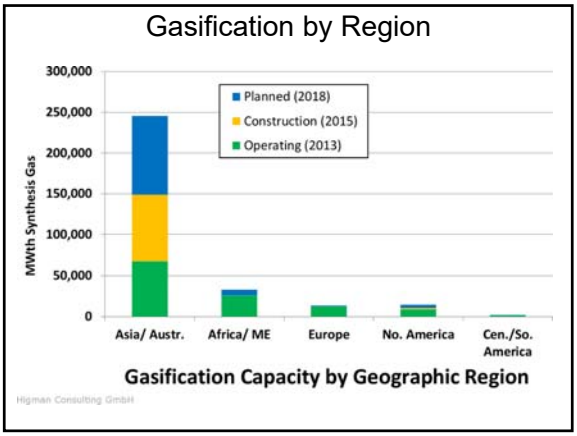
So what can you do with CO and H_2 ?

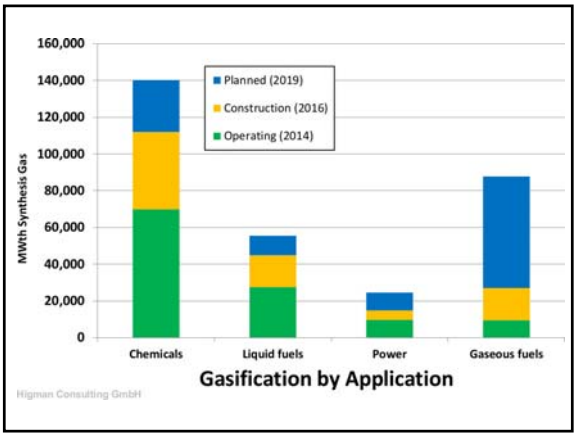


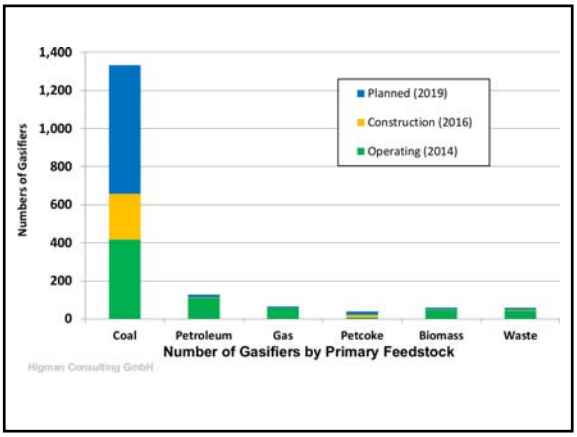
courtesy Gary Stiegel, talk at ACERC conf. (2006)



http://www.gasification-syngas.org/resources/the-gasification-industry/







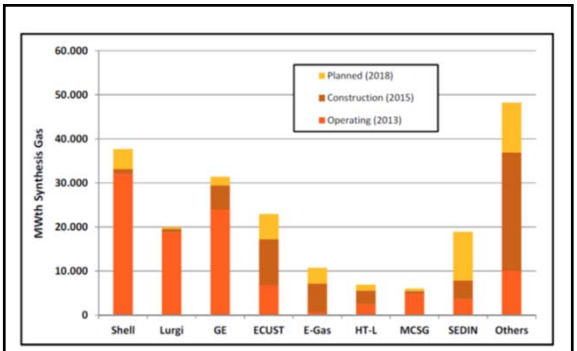
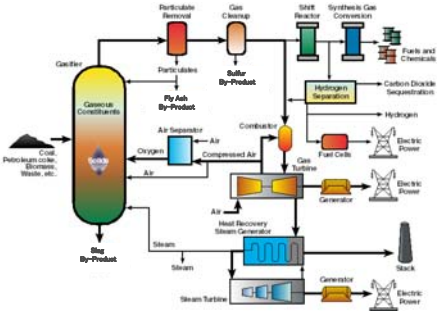


Figure 8 Gasification by Technology

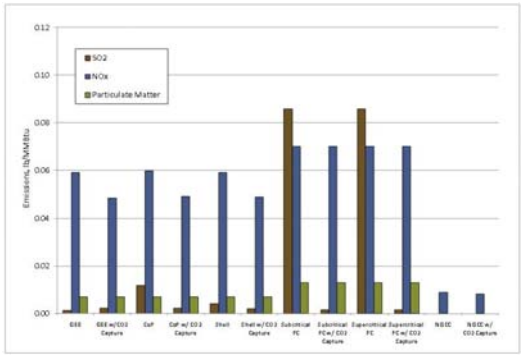
Higman, Pittsburgh Coal Conference, Beijing, China (Sept., 2013)

Gasification-Based Energy Production System Concepts

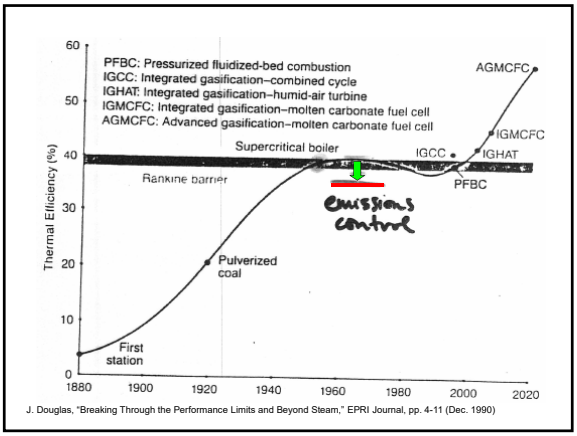


courtesy Gary Stiegel, talk at ACERC conf. (2006)

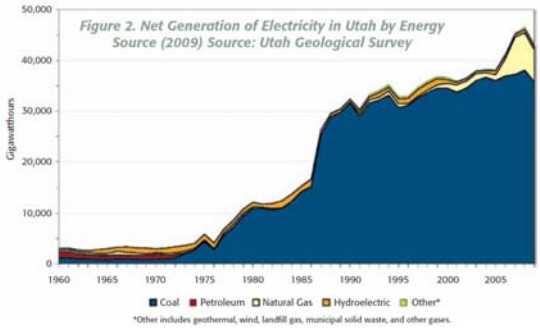
Compare Emissions



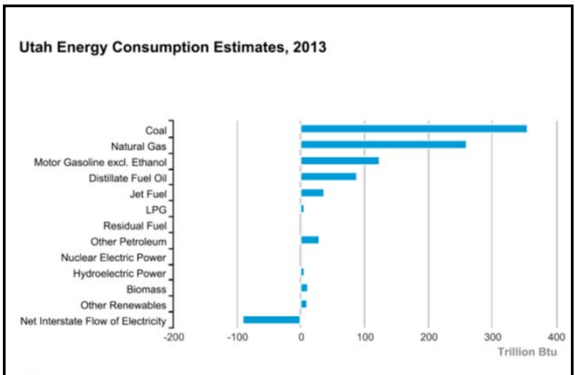
From Wikipedia



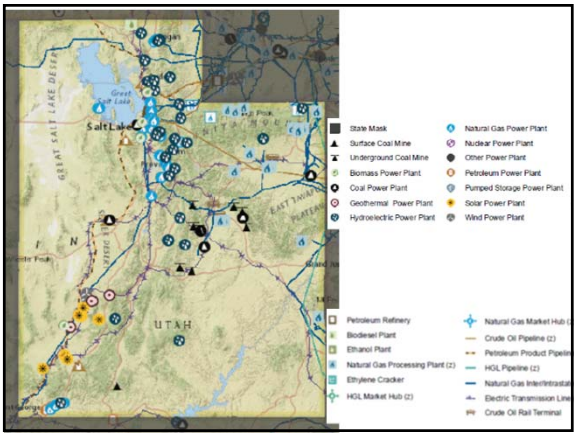
J. Douglas, "Breaking Through the Performance Limits and Beyond Steam," EPRI Journal, pp. 4-11 (Dec. 1990)

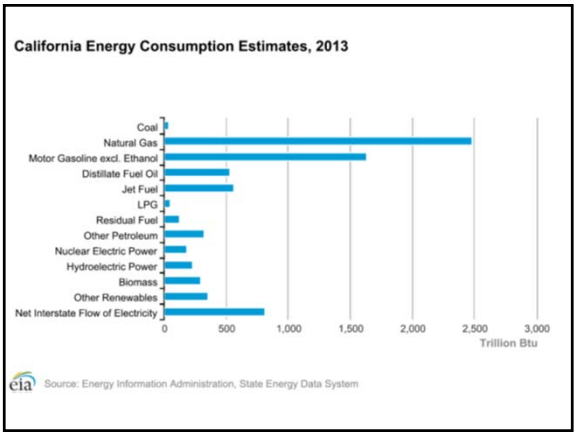


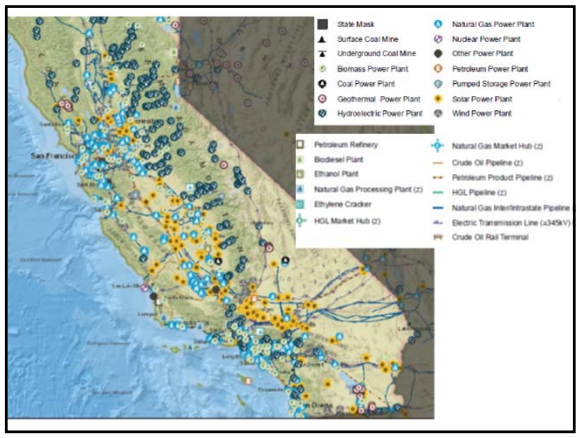
From "Energy Initiatives and Imperatives: Utah's 10-Year Strategic Energy Plan," Governor Gary R. Herbert (March 2, 2011)

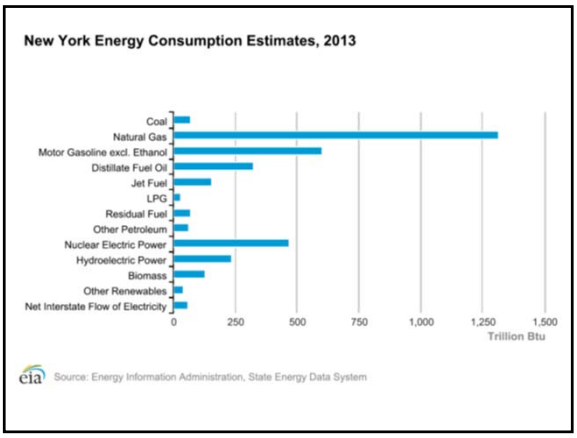


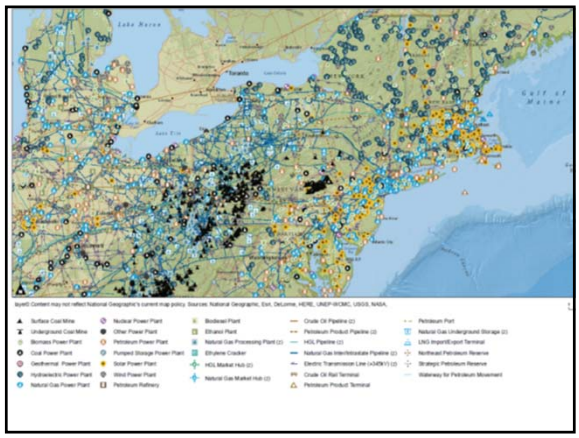
http://www.eia.gov/state/?sid=UT

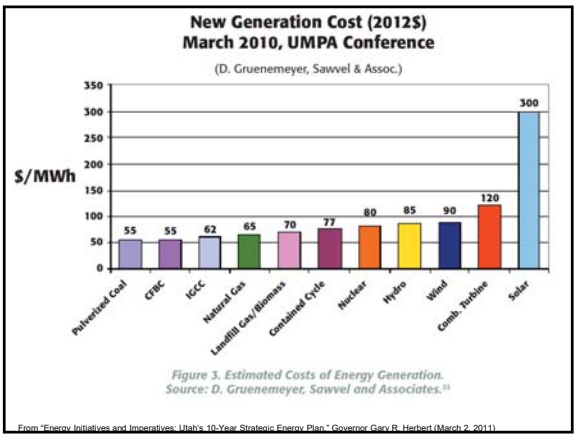












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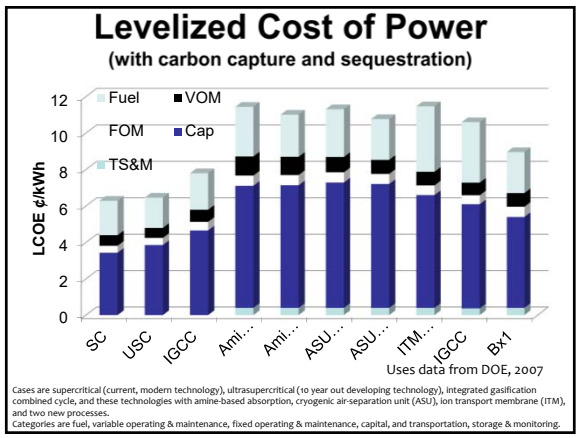

Cases are supercritical (current, modern technology), ultrasupercritical (10 year out developing technology), integrated gasification combined cycle, and these technologies with amine-based absorption, cryogenic air-separation unit (ASU), Ion transport membrane (ITM), and two new processes.
Categories are fuel, variable operating & maintenance, fixed operating & maintenance, capital, and transportation, storage & monitoring.