## Homework 6

Ch En 374 – Fluid Mechanics

Due date: 25 Oct. 2019

## **Survey Question**

Please report how long it took you to complete this assignment (in hours) in the "Notes" section when you turn your assignment in on Learning Suite.

## **Practice Problems**

- 1. [Lecture 17 Dynamics II: Navier-Stokes]. For each equation, write the name of the equation, any relevant restrictions to when it applies, and what each term in the equation represents physically.
  - (a)  $\rho \frac{D \boldsymbol{v}}{D t} = \rho \boldsymbol{g} + \nabla \cdot \boldsymbol{\sigma}$
  - (b)  $\boldsymbol{\tau} = 2\mu\boldsymbol{\Gamma}$ (c)  $\rho\left(\frac{\partial \boldsymbol{v}}{\partial t} + \boldsymbol{v}\cdot\nabla\boldsymbol{v}\right) = \rho\boldsymbol{g} - \nabla P + \mu\nabla^2\boldsymbol{v}$
  - (d) Additionally, consider an airplane flying through the sky at a constant velocity, U. Discuss the velocity boundary conditions on the air adjacent to the surface of the airplane from the perspective of an observer moving with the airplane.
- 2. [Lecture 18 Unidirectional Flow]. In a Couette viscometer the liquid to be studied fills the annular space between two cylinders, as shown in the figure to the right. The inner and outer radii are  $\kappa R$  and R, respectively. The viscosity is determined by measuring the torque required to keep the inner cylinder stationary when the outer one is rotated at a constant angular velocity  $\omega$ . The cylinders are long enough that the end effects associated with the top and bottom can be neglected and it can be assumed that v and  $\mathcal{P}$  are independent of z as well as of  $\theta$ . Show that a unidirectional velocity field with  $v_{\theta} = v_{\theta}(r)$  is consistent with continuity and determine  $v_{\theta}(r)$ .



3. [Lecture 19 – Non-Newtonian Pipe Flow]. In class, we showed that a power-law fluid flowing in a pipe has a velocity profile

$$v_z(r) = \frac{n}{n+1} \left(\frac{R^{n+1} \left|\Delta \mathcal{P}\right|}{2mL}\right)^{1/n} \left[1 - \left(\frac{r}{R}\right)^{(n+1)/n}\right] \tag{1}$$

where R is the pipe radius, m and n are coefficients in the power-law constitutive model, L is the pipe length, and  $|\Delta \mathcal{P}|$  is the magnitude of the pressure drop.

(a) Calculate the average velocity U.

- (b) Calculate the wall shear stress  $\tau_w$  in terms of U, R, m and n. We have seen this expression before! We used it in HW 3 problem 2 to find n and m from a set of pressure drop data.
- (c) Combine the expressions you get from (a) and (b) to find the friction factor of a powerlaw fluid in terms of the average velocity U, R, m, n and the density  $\rho$ .
- (d) Using the expression for the friction factor you found in part (a) and the fact that  $f = 16/\text{Re}_{\text{PL}}$  for laminar flow of a power-law fluid, find an expression for Re<sub>PL</sub>.

## **Challenge Problems**

- 4. In this problem we are going to explore the velocity field of a power-law fluid flowing in a pipe.
  - (a) Make Eq. 1 from problem 3 dimensionless using R as the length scale and U as the velocity scale.
  - (b) Use Python to plot the 1D dimensionless velocity field  $v_z/U$  versus r/R for n = 0.2, 1.0 and 5.0. Does the profile become more sharply peaked in the middle or more blunt as n increases?
- 5. Suppose that an open container of radius R is filled with liquid to an initial height  $h_0$ . It is then rotated at a constant angular velocity  $\omega$  as shown in the figure to the right. After an initial transient, the liquid rotates as if it were a rigid body. Assuming that the air pressure is constant at  $P_0$ and that the surface tension and viscous stresses are negligible, determine the liquid pressure P(r, z). Hint: Because it is a rigid body, we know that the velocity of the fluid is unidirectional with velocity  $v_{\theta}(r) = \omega r$ .



6. Consider pressure-driven flow in an annular channel. The inner and outer radii are the same as the figure from problem 2, but now both cylinders are stationary and there is a mean fluid velocity U in the z direction (into the page). The conduit length is L. Solve for  $v_z(r)$  in terms of the pressure drop. It is convenient to lump the viscosity and pressure together as  $B = |\Delta \mathcal{P}| / (\mu L)$  and write the final result in terms of a dimensionless radial coordinate  $\eta = r/R$ .

**Bonus Problem** (no points). Derive the Navier-Stokes equation in Cylindrical coordinates by making a momentum balance on the cylindrical shell shown on the left. *If you bring me the solution, I will buy you a King-Size Candy Bar of your choice.* 

