

Lecture 10 - Solving 1D Transport Equations

I. Motivation and Overview

A. Motivation

* Transport equations are (in general) non-linear PDEs.

They are hard to solve. We'd like to simplify them as much as possible.

* Why not just solve the whole non-linear PDE on a computer?

* We can and do sometimes. That isn't easy either.

Before ≈ 1990 , not really feasible. Before ≈ 2005 , not convenient (Matlab, comsol).

- Analytical solutions provide insight. "ABC's" of transport.
- Analytical solutions can be used to check numerical solutions on computer
- Analytical solutions are faster to compute.
- Analytical solutions teach us more. More to learn from.

Analytical
Solution

Numerical
Solution



Faster
More Insight
More Qualitative
More approximations
Limited methods

Slower
More accurate, Quantitative
More can be solved
Fewer approximations
Compare to experiment

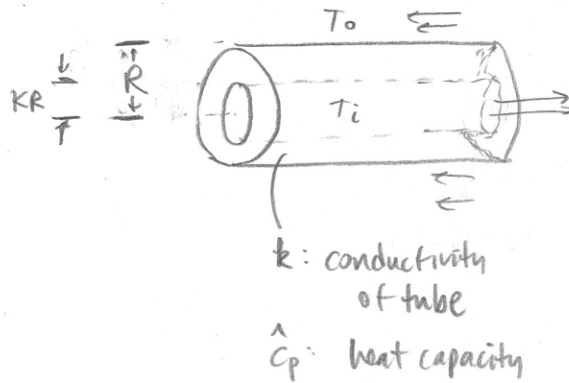
* In real life, we do both! If an analytical solution exists, it helps a lot! Both have their place.

B. Steps to solutions

1. Draw a picture. ID geometry.
ID balance equation & boundary conditions
2. Write balance equation in right coordinate system.
Simplify equation until it is one-dimensional.
3. Solve the math problem
4. Check physical interpretation. what does it mean?
Does it make sense?

II. Examples

A. Heat conduction in a tube wall



- Tube. $OD = R$
 $ID = KR$

- Fluid flowing very fast.
 $T_{inner} = T_i$
 $T_{outer} = T_o$ } Boundary conditions
 $T(r=R, \theta, z) = T_o$
 $T(r=KR, \theta, z) = T_i$

* Find temperature distribution in wall. Could use
find heat flux (but we don't have time).

* Balance Equation: Energy equation in cylindrical coordinates

$$\rho \hat{c}_p \frac{DT}{Dt} = k \nabla^2 T + H_v \quad (\text{p. 37, table 2-3})$$

$$\rho \hat{c}_p \left[\frac{\partial T}{\partial t} + v_r \frac{\partial T}{\partial r} + \frac{v_\theta}{r} \frac{\partial T}{\partial \theta} + v_z \frac{\partial T}{\partial z} \right] = k \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 T}{\partial \theta^2} + \frac{\partial^2 T}{\partial z^2} \right] + H_v$$

- steady : $T \neq T(t)$, $\frac{\partial T}{\partial t} = 0$
- one-dimensional : $T = T(r)$ $\frac{\partial T}{\partial \theta} = \frac{\partial T}{\partial z} = 0$
- solid wall : $v_r = v_\theta = v_z = 0$
- No heat generation : $H_v = 0$

$\Rightarrow$ only underlined terms survive

$$\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) = 0$$

* Solve math problem:

$$\frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) = 0 \quad T(R) = T_o \quad T(KR) = T_i$$

- Separable, linear, ^{2nd order} homogeneous ODE with Dirichlet BC's.

$$r \frac{\partial T}{\partial r} = C_1 \Rightarrow \frac{\partial T}{\partial r} = \frac{C_1}{r} \Rightarrow T = C_1 \ln r + C_2$$

- solve for BC's:

$$T(R) = C_1 \ln R + C_2 = T_o \quad (1)$$

$$T(KR) = C_1 \ln KR + C_2 = T_i \quad (2)$$

$$(1) - (2) = C_1 \ln(R/KR) = T_o - T_i$$

$$C_1 = \frac{T_o - T_i}{-\ln(K)} = \frac{T_i - T_o}{\ln K}$$

$$(1) : (T_i - T_o) \frac{\ln R}{\ln K} + C_2 = T_o$$

$$C_2 = T_o - \frac{\ln R}{\ln K} (T_i - T_o)$$

$$T(r) = \frac{T_i - T_o}{\ln K} \ln r - \frac{\ln R}{\ln K} (T_i - T_o) + T_o$$

$$T(r) = T_o + \frac{(T_i - T_o)}{\ln K} \ln \left(\frac{r}{R} \right)$$

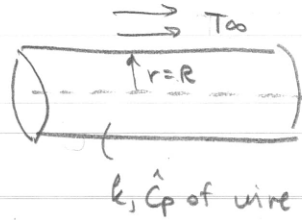
* get q_r by

$$q_r = -k \frac{\partial T}{\partial r} \Big|_{r=R}$$

* Does this make sense? look at python plot.

B. Electrically Heated wire

(Ex. 3.2-5)



- wire diameter: R
- Fluid flowing w/
heat transfer coeff, h .
- Heating rate due to electrical
heating: H_v .

• Boundary conditions?

- Symmetry at $r=0$

$$\left. \frac{dT}{dr} \right|_{r=0} = 0$$

- Newton's Law of cooling / convection at $r=R$

$$-k \left. \frac{dT}{dr} \right|_{r=R} = h [T(R) - T_{\infty}]$$

* Balance equation: Energy equation in cylindrical coords.
(same as before)

$$\rho \hat{C}_p \frac{DT}{Dt} = k \nabla^2 T + H_v$$

$$\rho \hat{C}_p \left[\frac{\partial T}{\partial t} + u_r \frac{\partial T}{\partial r} + \frac{v_{\theta}}{r} \frac{\partial T}{\partial \theta} + v_z \frac{\partial T}{\partial z} \right] = k \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 T}{\partial \theta^2} + \frac{\partial^2 T}{\partial z^2} \right] + H_v$$

↑
only surviving terms

- steady, one-dimensional ($T = T(r)$), solid wire
 $\left(\frac{\partial T}{\partial t} = 0 \right)$ $(T \neq T(z) \neq T(\theta))$ $(v = 0)$

$$\frac{k}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) + H_v = 0$$

* Solve Math problem

$$\frac{k}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) + H_v = 0$$

$$\left. \frac{\partial T}{\partial r} \right|_{r=0} = 0$$

$$\left. \frac{\partial T}{\partial r} \right|_{r=R} = -\frac{h}{k} [T(R) - T_{\infty}]$$

- Separable, linear, 2nd order, non-homogeneous ODE with Robin condition. (Harder problem, a bit.)

$$\frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) = -r \frac{H_v}{k}$$

$$r \frac{\partial T}{\partial r} = -\frac{r^2}{2} \frac{H_v}{k} + C_1 \Rightarrow \frac{\partial T}{\partial r} = -\frac{r}{2} \frac{H_v}{k} + \frac{C_1}{r}$$

$$T = -\frac{r^2}{4} \frac{H_v}{k} + C_1 \ln r + C_2$$

(*) Same general solution, but w/ particular solution due to H_v .

- Apply BC's to find C_1, C_2

BC1: $\frac{dT}{dr} \Big|_{r=0} = 0 \quad \lim_{r \rightarrow 0} \frac{dT}{dr} = \frac{C_1}{r} \rightarrow \infty, C_1 = 0$

$$\frac{dT}{dr} \Big|_{r=R} = -\frac{H_v R}{2k}$$

plug into BC2

$$T(r=R) = -\frac{R^2}{4k} \frac{H_v}{k} + C_2$$

BC2: $\frac{\partial T}{\partial r} \Big|_{r=R} = -\frac{h}{k} [T(R) - T_\infty]$

$$-\frac{H_v R}{2k} = -\frac{h}{k} \left[-\frac{H_v R^2}{4k} + C_2 - T_\infty \right] \quad \leftarrow \text{Solve for } C_2$$

$$+\frac{H_v R}{2h} = -\frac{H_v R^2}{4k} + C_2 - T_\infty$$

$$C_2 = T_\infty + \frac{H_v R^2}{4k} + \frac{H_v R}{2h}$$

$$T = -\frac{H_v r^2}{4k} + \frac{H_v R^2}{4k} + \frac{H_v R}{2h} + T_\infty$$

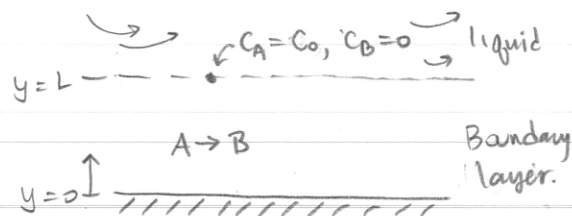
$$T = T_\infty + \frac{H_v R}{2h} + \frac{H_v R^2}{4k} \left(1 - \frac{r^2}{R^2} \right)$$

Temp. at surface

Temp distribution from center to wire edge.

* Does it make sense? See plot!

C. Irreversible Homogeneous Reaction in a liquid (Ex. 3.2-1)



- Consider close to the boundary in a liquid. (boundary layer)

- Homogeneous reaction: $A \rightarrow B$

- Pseudo binary solution
 - $R_{v,A} = -kC_A$
 - $R_{v,B} = kC_A$

$$C_A, C_B \ll C_S$$

- L set by external fluid flow problem, given

- $v \approx 0$ in B.L.

- Boundary conditions:

$$C_A(y=L) = C_0, \quad C_B(y=L) = 0$$

$$\begin{aligned} \vec{J}_A \cdot \vec{n} |_{y=0} &= 0, \quad \vec{J}_B \cdot \vec{n} |_{y=0} = 0 \\ \Downarrow \quad \frac{dC_A}{dy} |_{y=0} &= 0, \quad \frac{dC_B}{dy} |_{y=0} = 0 \end{aligned}$$

* Balance Equations: Pseudo binary species mass balance in Cartesian coordinates

$$\textcircled{*} \quad \frac{DC_A}{Dt} = D_A \nabla^2 C_A + R_{v,A} \quad \leftarrow \text{let's just solve } C_A$$

$$\frac{DC_B}{Dt} = D_B \nabla^2 C_B + R_{v,B}$$

- time
- need C_A to find C_B b/c of reaction.

(Table 2-4)
$$\frac{\partial C_A}{\partial t} + v_x \frac{\partial C_A}{\partial x} + v_y \frac{\partial C_A}{\partial y} + v_z \frac{\partial C_A}{\partial z} = D_A \left[\frac{\partial^2 C_A}{\partial x^2} + \frac{\partial^2 C_A}{\partial y^2} + \frac{\partial^2 C_A}{\partial z^2} \right] - kC_A$$

• steady: $\frac{\partial C_A}{\partial t} = 0$

• stagnant: $u_x = u_y = u_z = 0$

- one-dimensional:

$$C_A \neq C_A(x) \neq C_A(z)$$

$\Rightarrow$ only underlined terms survive

$\textcircled{*}$ Careful with velocities in mass transfer problems. See supp. notes. Diffusive flux can cause bulk flow:

$$\sum_i \underline{N_i} = C \underline{v}$$

* Solve math problem:

$$D_A \frac{\partial^2 C_A}{\partial y^2} - k C_A = 0 \quad C_A(y=L) = C_0$$

$$\frac{dC_A}{dy}(y=0) = 0$$

- 2nd order, linear, constant coefficient ODE
w/ 1 Dirichlet / 1 Neumann condition.

$$\frac{\partial^2 C_A}{\partial y^2} - \frac{k}{D_A} C_A = 0$$

$$\text{Let } C_A = C e^{ry} \rightarrow r^2 - \frac{k}{D_A} = 0 \rightarrow r = \pm \sqrt{\frac{k}{D_A}}$$

$$\text{Let } \lambda = \sqrt{\frac{D_A}{k}} \rightarrow r = \pm 1/\lambda \quad (\lambda \text{ is a length, } k \text{ is } 1/\text{time})$$

$$C_A = C_1 \sinh(y/\lambda) + C_2 \cosh(y/\lambda)$$

- Solve for constants

$$C_A(L) = C_1 \sinh(L/\lambda) + C_2 \cosh(L/\lambda) = C_0$$

$$\frac{dC_A}{dy}(y=0) = \frac{C_1}{\lambda} \underbrace{\cosh(0)}_1 + \frac{C_2}{\lambda} \underbrace{\sinh(0)}_0 = 0$$

$$C_1 = 0, \text{ so}$$

$$C_2 = C_0 / \cosh(L/\lambda)$$

$$\boxed{C_A(y) = C_0 \frac{\cosh(y/\lambda)}{\cosh(L/\lambda)}, \quad \lambda = \sqrt{\frac{D_A}{k}}}$$

* Does this make sense? See python plot.