

## Chapter 6 Controller Design Using *Design Tools*

### Defining Good Process Test Data

- The process should be at steady state before data collection starts
- The test dynamics should clearly dominate the process noise
- The disturbances should be quiet during the dynamic test
- The model fit should visually approximate the data
- (The first data point should equal the initial steady state value)

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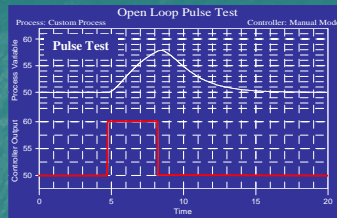
## Dynamic Testing

- **Limitations of the Step Test**
  - It moves the process away from the desired operating level for too long causing significant off-spec production
  - Generates data on only one side of initial steady state
- **Limitations of All Open Loop Tests**
  - Open loop tests require operating personnel to put a loop in manual "just" to generate dynamic process data
  - Popular open loop tests include: step, pulse, doublet, PRBS

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## Pulse Test

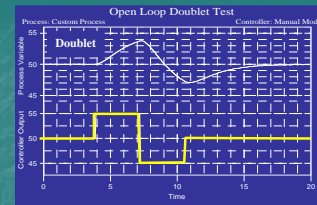


- Pulse test is two step tests performed in rapid succession
- *Desirable*: starts from and returns to an initial steady state
- *Undesirable*: data generated on one side of this steady state (which presumably is design level of operation)

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## Doublet Testing



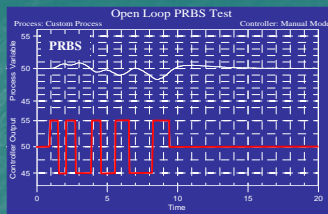
- A doublet, two pulses in opposite directions, is desirable:
  - returns quickly to the design level of operation
  - produces data both above and below the design level
  - relatively small deviation from the initial steady state

*Doublet is preferred by many practitioners*

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## PRBS Testing



- Pseudo-random binary sequence (PRBS) tests are a sequence of controller output pulses that are
  - uniform in amplitude
  - alternating in direction
  - random in duration

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## PRBS Testing

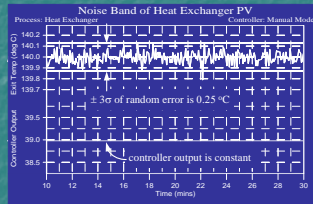
- *Desirable*:
  - start and return to the design level of operation
  - produces data both above and below the design level
  - produces the smallest maximum deviation from the initial steady state of all open loop tests
- A proper PRBS design requires specifying:
  - controller output initial value
  - controller output pulse amplitude
  - average duration of each pulse
  - standard deviation of the random change in pulse duration around this average
  - length of the experiment itself
- If you perform the experiment a number of times in a search of a "best" test, stick with the quick and practical doublet test

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## Noise Band and Signal to Noise Ratio

- To obtain good data for tuning, the controller output must force the process variable to move at least 10 times the *noise band* (signal to noise ratio  $\geq 10$ )



- Here, controller output should be moved far and fast enough to cause the measured exit temperature to move at least 2.5 °C
- Noise band includes measurement noise *and* process noise

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## Automated Controller Design Using *Design Tools*

| Time | Controller Output | Process Variable |
|------|-------------------|------------------|
| 0.00 | 70.0              | 4.00             |
| 0.15 | 70.0              | 4.01             |
| 0.30 | 80.0              | 3.99             |
| 0.45 | 80.0              | 4.03             |
| 0.60 | 80.0              | 4.09             |
| 0.75 | 80.0              | 4.17             |

process must be at steady state when data collection begins

first PV value must equal the true initial steady state

- Design Tools* fits dynamic models to process data in text files with (at least) three columns:

- a time stamp
- manipulated variable data (usually controller output)
- measured process variable data

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## Automated Controller Design Using *Design Tools*

### Step 1:

- Find model parameters that minimize sum of squared errors:

$$SSE = \sum_{i=1}^N [\text{Measured Data}_i - \text{Model Data}_i]^2$$

- The smaller the SSE, the better the model describes the data
- To obtain a meaningful model:
  - process must be at steady state before data collection begins
  - the first point in the file must equal this steady state value
- If these are not true, the model will be of little use

### Step 2:

- Uses the FOPDT model parameters in correlations to compute initial controller tuning values

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## Example Fit of Heat Exchanger Doublet Test

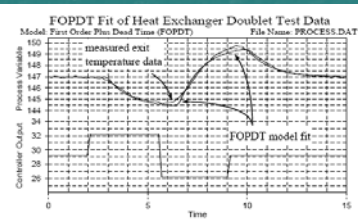


Figure 6.6 - *Design Tools* fit of heat exchanger doublet test data using a FOPDT model

Fit results in values for  $K_p$ ,  $\tau_p$ , and  $\theta_p$

$$\tau_p \frac{dy}{dt} + y = K_p u(t - \theta_p)$$

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## Controller Design Using **Closed Loop Data**

- Operations may not open an existing loop for controller design, so closed loop dynamic testing required
- In theory, closed loop testing can produce data that reflects the character of the controller as well as that of the process
- In practice this rarely is a problem
- For closed loop studies, dynamic data is generated by stepping, pulsing or otherwise perturbing the set point
- The controller must be tuned aggressive enough so that the changing controller output forces the measured process variable to move more than ten times the noise band

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## Do Not Model Disturbance Driven Data! (for controller design)

- A controller uses the FOPDT model to understand how its output signal affects the measured process variable
- So test data must contain measured process variable dynamics that have been forced by the controller output
- Disturbance events that occur during data collection will degrade accuracy and hence usefulness of the FOPDT model

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## Comparison of Manual vs. Automated Fits

|                                    | ← Open Loop Data →                 |                             | Closed Loop Data |
|------------------------------------|------------------------------------|-----------------------------|------------------|
|                                    | Graphical Analysis<br>Of Step Test | Design Tools<br>Doublet Fit |                  |
| Process Gain, $K_p$ (%/°C)         | -0.86                              | -0.90                       | -0.86            |
| Time Constant, $\tau_p$ (min)      | 1.0                                | 1.1                         | 1.2              |
| Dead Time, $\theta_p$ (min)        | 0.3                                | 0.9                         | 1.0              |
| Sum of Squared Errors (SSE)        | 44.1                               | 3.2                         | 5.4              |
| ITAE Controller Gain, $K_c$ (%/°C) | -2.1                               | -0.7                        | -0.7             |

Table 6.7 – Comparing FOPDT models for heat exchanger

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## FOPDT Fit of Underdamped Process

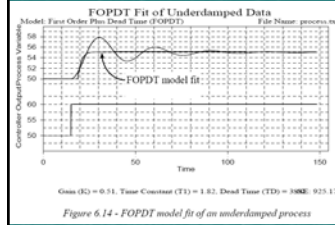


Figure 6.14 - FOPDT model fit of an underdamped process

- Fit looks bad
  - No oscillations predicted
- FOPDT parameters used in correlations to get tuning parameters
  - Good control parameters!
- Reason:
  - Time delay modeled
  - Initial time response modeled
    - Direction of response as well
  - Gain (ultimate response to controller output) modeled

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## Inverse Response

The measured process variable first moves in one direction before it ultimately responds to steady state in the opposite direction

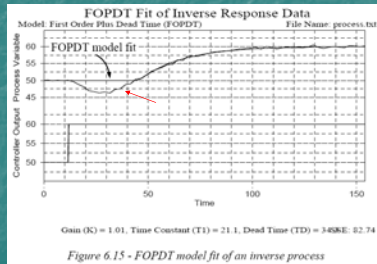


Figure 6.15 - FOPDT model fit of an inverse process

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Sometimes teenagers act this way (or spouses)!

**Let's Do It in Control Station!**