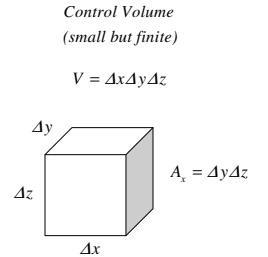
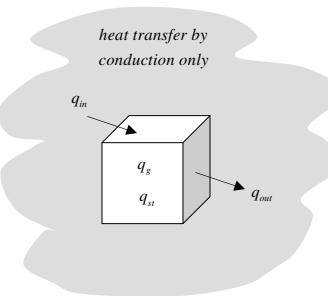
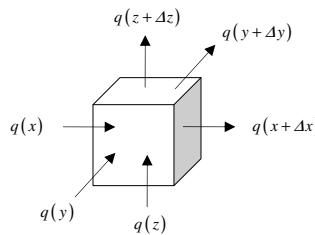
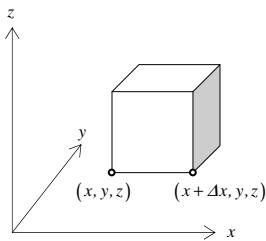


## 2.3 THE HEAT EQUATION

Derivation of the Heat Equation in the Cartesian coordinates (finite control volume approach)

Consider a Control Volume  
in the stagnant continuous medium



$$\text{Energy Balance: } q_{in} - q_{out} + q_g = q_{st}$$

$$q(x) - q(x + \Delta x) + q(y) - q(y + \Delta y) + q(z) - q(z + \Delta z) + q_g = q_{st}$$

$$\begin{aligned} q_x &= q''_x \cdot A_x = q''_x \cdot \Delta y \cdot \Delta z \\ q_y &= q''_y \cdot A_y = q''_y \cdot \Delta x \cdot \Delta z \\ q_z &= q''_z \cdot A_z = q''_z \cdot \Delta x \cdot \Delta y \end{aligned} \quad \left[ q''(x) - q''(x + \Delta x) \right] \Delta y \Delta z + \left[ q''(y) - q''(y + \Delta y) \right] \Delta x \Delta z + \left[ q''(z) - q''(z + \Delta z) \right] \Delta x \Delta y + \dot{q} \Delta x \Delta y \Delta z = \rho c_p \frac{\partial T}{\partial t} \Delta x \Delta y \Delta z$$

$$\text{divide equation by } \Delta x \Delta y \Delta z \quad - \frac{q''(x + \Delta x) - q''(x)}{\Delta x} - \frac{q''(y + \Delta y) - q''(y)}{\Delta y} - \frac{q''(z + \Delta z) - q''(z)}{\Delta z} + \dot{q} = \rho c_p \frac{\partial T}{\partial t}$$

take a limit when

$$\Delta x \rightarrow 0$$

$$\Delta y \rightarrow 0$$

$$\Delta z \rightarrow 0$$

$$-\frac{\partial q''_x}{\partial x} - \frac{\partial q''_y}{\partial y} - \frac{\partial q''_z}{\partial z} + \dot{q} = \rho c_p \frac{\partial T}{\partial t}$$

apply Fourier's Law:

$$q''_x = -k \frac{\partial T}{\partial x}$$

$$q''_y = -k \frac{\partial T}{\partial y}$$

$$q''_z = -k \frac{\partial T}{\partial z}$$

$$\boxed{\frac{\partial}{\partial x} \left( k \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left( k \frac{\partial T}{\partial y} \right) + \frac{\partial}{\partial z} \left( k \frac{\partial T}{\partial z} \right) + \dot{q} = \rho c_p \frac{\partial T}{\partial t}}$$

In general,  $k$  is a tensor with components:

$$k_x(T)$$

$$k_y(T)$$

$$k_z(T)$$

depending on temperature

assume:  
 $k = \text{const}$

$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} + \frac{\dot{q}}{k} = \frac{\rho c_p}{k} \frac{\partial T}{\partial t}$$

introduce:  
 $\alpha = \frac{k}{\rho c_p}$

$$\boxed{\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} + \frac{\dot{q}}{k} = \frac{1}{\alpha} \frac{\partial T}{\partial t}}$$

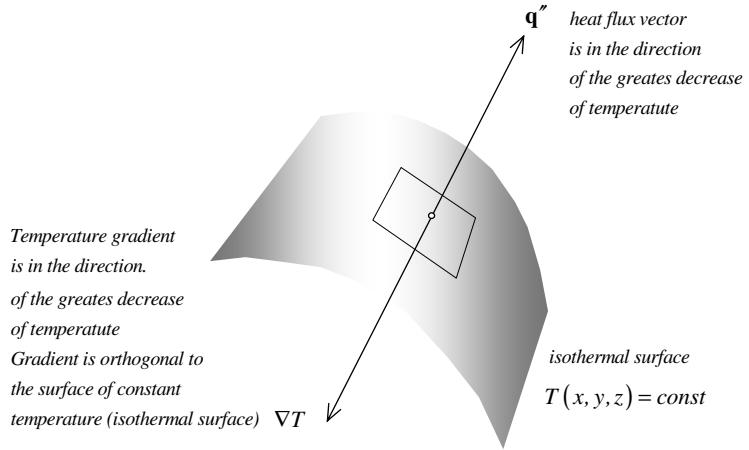
The Heat Equation

$$T(x), \dot{q}(x)$$

2.1

## FOURIER'S LAW

$$\mathbf{q}'' = -k \nabla T$$



**The Heat Equation - Derivation** Consider a point in the system defined by a position vector  $\mathbf{r} \in D \subset \mathbb{R}^3$ . Let  $V$  be an arbitrary small control volume containing the point  $\mathbf{r}$ .

Conservation of energy principle for control volume  $V$ :

$$\begin{bmatrix} \text{rate of} \\ \text{net heat flow} \\ \text{through the} \\ \text{boundary } S \end{bmatrix} + \begin{bmatrix} \text{rate of heat} \\ \text{generation} \\ \text{in volume } V \end{bmatrix} = \begin{bmatrix} \text{rate of heat} \\ \text{storage} \\ \text{in volume } V \end{bmatrix}$$

$$-\int_S \mathbf{q}(\mathbf{r}, t) \cdot \mathbf{n} dS + \int_V g(\mathbf{r}, t) dV = \int_V \rho c_p \frac{\partial T(\mathbf{r}, t)}{\partial t} dV$$

Apply the divergence theorem and combine the terms:

$$\int_V \left[ -\nabla \cdot \mathbf{q}(\mathbf{r}, t) + g(\mathbf{r}, t) - \rho c_p \frac{\partial T(\mathbf{r}, t)}{\partial t} \right] dV = 0$$

Because  $V$  is an arbitrary control volume, in the limit when  $V \rightarrow 0$ :

$$-\nabla \cdot \mathbf{q}(\mathbf{r}, t) + g(\mathbf{r}, t) - \rho c_p \frac{\partial T(\mathbf{r}, t)}{\partial t} = 0$$

Apply the Fourier Law:

$$\nabla \cdot [k(\mathbf{r}) \nabla T(\mathbf{r}, t)] + g(\mathbf{r}, t) = \rho c_p(\mathbf{r}) \frac{\partial T(\mathbf{r}, t)}{\partial t}$$

If  $k, \rho, c_p$  are constant, then

$$\nabla^2 T(\mathbf{r}, t) + \frac{g(\mathbf{r}, t)}{k} = \frac{1}{\alpha} \frac{\partial T(\mathbf{r}, t)}{\partial t}$$

2.3

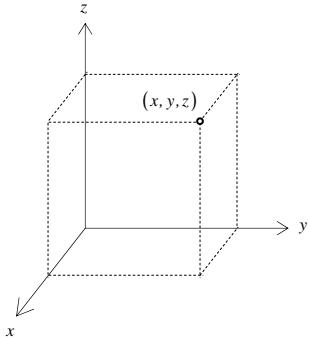
### THE HEAT DIFFUSION EQUATION

**in uniform medium:**  $k, \rho, c_p$ , and  $\alpha$  are constants

Vector form

$$\nabla^2 T(\mathbf{r}, t) + \frac{g(\mathbf{r}, t)}{k} = \frac{I}{\alpha} \frac{\partial T(\mathbf{r}, t)}{\partial t}$$

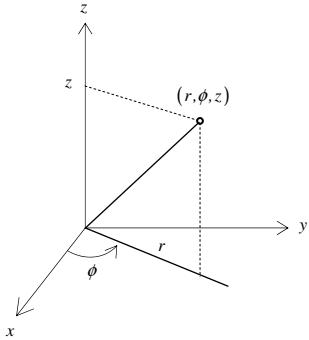
Cartesian coordinates



$$\nabla T = \left\langle \frac{\partial T}{\partial x}, \frac{\partial T}{\partial y}, \frac{\partial T}{\partial z} \right\rangle$$

$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} + \frac{\dot{q}}{k} = \frac{I}{\alpha} \frac{\partial T}{\partial t} \quad (2.21)$$

Cylindrical coordinates

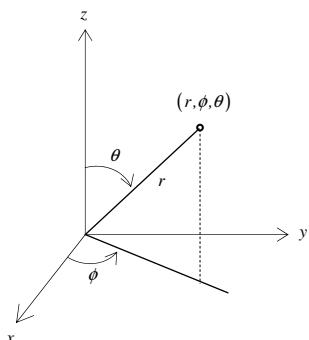


$$\nabla T = \left\langle \frac{\partial T}{\partial r}, \frac{1}{r} \frac{\partial T}{\partial \phi}, \frac{\partial T}{\partial z} \right\rangle$$

$$\frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial T}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 T}{\partial \phi^2} + \frac{\partial^2 T}{\partial z^2} + \frac{\dot{q}}{k} = \frac{I}{\alpha} \frac{\partial T}{\partial t} \quad (2.26)$$

$$r \frac{\partial T}{\partial r} + \frac{\partial^2 T}{\partial r^2} + \frac{1}{r^2} \frac{\partial^2 T}{\partial \phi^2} + \frac{\partial^2 T}{\partial z^2} + \frac{\dot{q}}{k} = \frac{I}{\alpha} \frac{\partial T}{\partial t}$$

Spherical coordinates



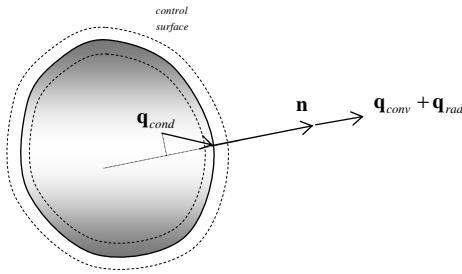
$$\nabla T = \left\langle \frac{\partial T}{\partial r}, \frac{1}{r \sin \theta} \frac{\partial T}{\partial \phi}, \frac{1}{r \sin \theta} \frac{\partial T}{\partial \theta} \right\rangle$$

$$\frac{1}{r^2} \frac{\partial}{\partial r} \left( r^2 \frac{\partial T}{\partial r} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 T}{\partial \phi^2} + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left( \sin \theta \frac{\partial T}{\partial \theta} \right) + \frac{\dot{q}}{k} = \frac{I}{\alpha} \frac{\partial T}{\partial t} \quad (2.29)$$

$$\frac{2}{r} \frac{\partial T}{\partial r} + \frac{\partial^2 T}{\partial r^2} + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 T}{\partial \phi^2} + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left( \sin \theta \frac{\partial T}{\partial \theta} \right) + \frac{\dot{q}}{k} = \frac{I}{\alpha} \frac{\partial T}{\partial t}$$

## Derivation of the Boundary Condition

Energy balance for Control Surface:



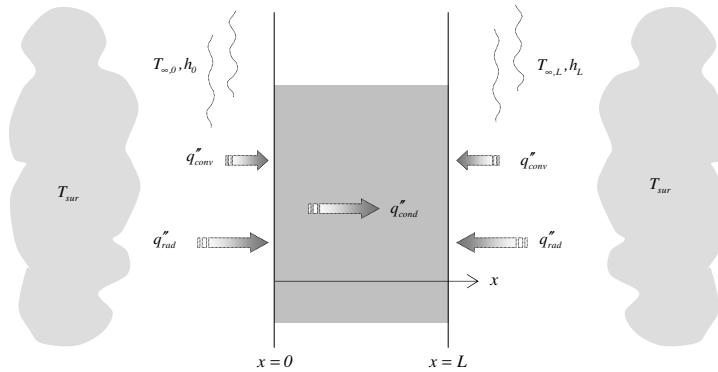
$$\mathbf{q}_{cond}(\mathbf{r}, t) \cdot \mathbf{n}|_S = h[T(\mathbf{r}, t)|_S - T_\infty] + \varepsilon\sigma[T^4(\mathbf{r}, t)|_S - T_{sur}^4]$$

2.4

## BOUNDARY CONDITIONS

### in 1-D Cartesian Coordinates

Consider the boundaries  $x=0$  and  $x=L$  exposed to convective and radiative environment



Energy Balance:

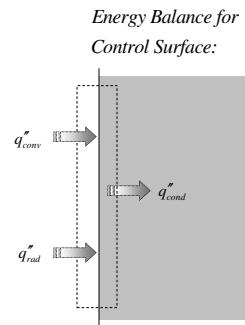
$$q''_{cond} = q''_{conv} + q''_{rad}$$

$$\left[ -k \frac{dT}{dx} \right]_{x=0} = h[T_\infty - T(0)] + \varepsilon\sigma[T_{sur}^4 - T^4(0)]$$

non-linear boundary condition

$$\left[ -k \frac{dT}{dx} + hT \right]_{x=0} = hT_\infty$$

linear convective boundary condition with  
 $h = h_{conv} + h_{rad}$  effective convective coefficient  
when it is assumed that  $T_{sur} = T_\infty$



Linearization of the boundary conditions:

$$\begin{aligned} \varepsilon\sigma[T_{sur}^4 - T^4(0)] &= \varepsilon\sigma[T_{sur}^2 + T^2(0)][T_{sur} + T(0)][T_{sur} - T(0)] \\ &= h_{rad}[T_{sur} - T(0)] \end{aligned}$$

$$h_{rad} = \varepsilon\sigma[T_{sur}^2 + T^2(0)][T_{sur} + T(0)]$$

$$\text{if } \frac{|T - T_{sur}|}{T_{sur}} \ll 1 \quad \text{then} \quad h_{rad} \approx 4\varepsilon\sigma T_{sur}^3$$

<p><i>Dirichlet</i></p> <p><b>I</b></p>	$[T]_{x=0} = T_{s,0}$	$[T]_{x=L} = T_{s,L}$	<p>prescribed temperature at the boundary  <i>(thermostated boundary with the surface temperature <math>T_s = T_\infty</math> when <math>h \gg k</math>)</i></p>
<p><i>Neumann</i></p> <p><b>II</b></p>	$\left[ -k \frac{dT}{dx} \right]_{x=0} = q''_{s,0}$	$\left[ k \frac{dT}{dx} \right]_{x=L} = q''_{s,L}$	<p>prescribed heat flux at the boundary  <math>\left[ \frac{dT}{dx} \right]_{x=0} = 0</math> <i>insulated boundary</i></p>
<p><i>Robin</i></p> <p><b>III</b></p>	$\left[ -k \frac{dT}{dx} + h_0 T \right]_{x=0} = h_0 T_{\infty,0}$	$\left[ k \frac{dT}{dx} + h_L T \right]_{x=L} = h_L T_{\infty,L}$	<p>convective boundary condition</p>

## INITIAL CONDITION

$$T(x, y, z, 0) = T_0(x, y, z)$$

for all interior points of the domain  $(x, y, z) \in D$